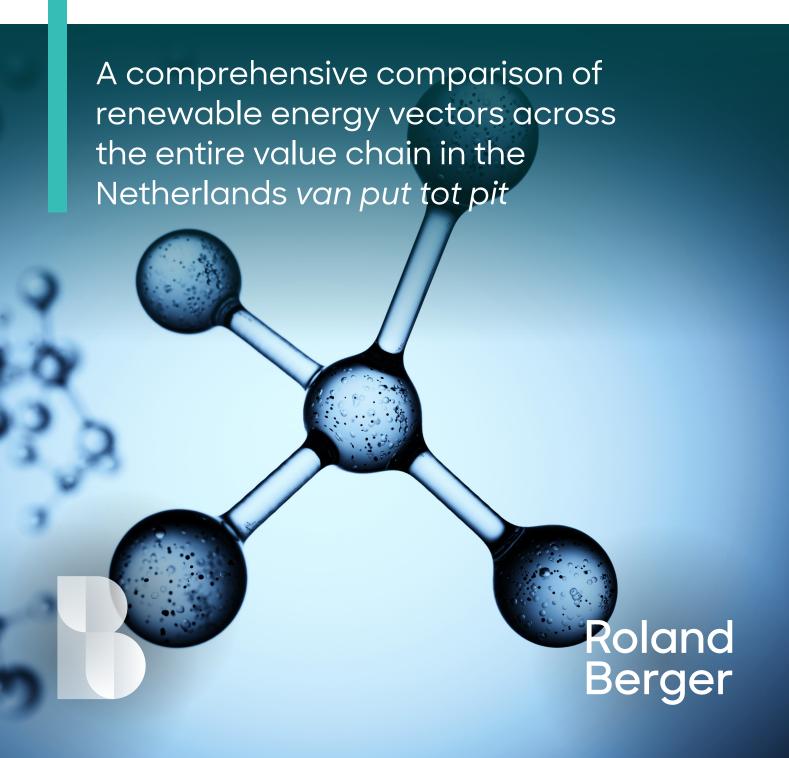


# Feasibility and potential of e-methane in the future energy mix



#### **Foreword**

he energy transition is both a necessity and an opportunity as the Netherlands strives to meet its ambitious climate goals. In this transition, exploring diverse renewable energy vectors is essential to ensuring a reliable, sustainable, and cost-effective energy system.

E-methane, a renewable vector produced using renewable hydrogen and captured CO<sub>2</sub>, is one such option that warrants careful consideration.

This report, Feasibility and potential of e-methane in the future energy mix, examines e-methane's potential role in the Netherlands' energy landscape, comparing it to other renewable vectors across the entire value chain van put tot pit. Commissioned by Gasunie and GasTerra, it has been independently prepared by Roland Berger BV ("Roland Berger") based on publicly available data, ensuring a transparent and objective assessment.

The insights in this report contribute to the ongoing dialogue on the future of energy in the Netherlands, providing relevant perspectives for policymakers, industry stakeholders, and market players. They are also applicable to other regions that share a similar reliance on natural gas and are likely to require substantial imports to meet their future renewable energy needs. A separate appendix details the assumptions and data sources used in this study.

## **Executive** summary

enewable energy vectors will play a critical role in the energy transition, especially in sectors that are difficult to electrify. Multiple renewable energy vectors exist, and a comprehensive comparison across the entire value chain, tailored to specific enduse cases, is essential to assess their potential and identify the most viable options for specific end-use cases. The goal of this study is to evaluate the feasibility and potential of e-methane, compared to the other renewable energy vectors biomethane, hydrogen, LOHC, ammonia and methanol, within the future energy mix of the Netherlands. The analysis includes the cost-competitiveness of these vectors across the entire value chain, from production to transportation, transmission, storage, distribution and end-use in the Netherlands. Additionally, non-financial factors such as technological maturity, environmental impact, safety characteristics and land-use efficiency are also considered.

E-methane is a renewable energy vector with a carbon neutral cycle synthesized by combining CO<sub>2</sub> captured from a point source or the air via DAC with renewable hydrogen. When combined with carbon capture and storage of the CO<sub>2</sub> released during the combustion, e-methane produced with biogenic CO<sub>2</sub> or DAC can even achieve negative emissions. While e-methane is expected to become more widely available and cost-competitive in long term, it will still be more expensive than CO<sub>2</sub> compensated natural gas and will require more cohesive regulation to scale up.

When comparing renewable energy vectors, e-methane produced from DAC has slightly higher production costs compared to ammonia and LOHC, as e-methane requires CO<sub>2</sub> in addition to renewable hydrogen. E-methane produced from biogenic CO<sub>2</sub> has lower production costs than CO<sub>2</sub> from DAC, but biogenic CO<sub>2</sub> availability is expected to be limited in the long term. In terms of transportation, pipelines are the most cost-competitive option for shorter distances, provided sufficient volumes are transported. For medium to longer distances, shipping becomes more cost-competitive. E-methane's landed cost at port is competitive with other renewable energy vectors when delivered in their end-use state. For hydrogen-specific applications, ammonia and liquid hydrogen offer the lowest landed cost.

Five key use cases where e-methane could play a role were selected for further analysis: iron and steel production, process heat for the five large industrial clusters in the Netherlands, process heat for the dispersed industrial cluster 6, central dispatchable electricity production and decentral heating. These use cases were selected based on their feasibility for e-methane and their projected demand in the Netherlands. Together, they are forecasted to represent more than 70% of the total Dutch e-methane demand. Among these, e-methane emerges as a cost-competitive vector in the long term - towards 2040 and beyond - for enduse cases with high downstream costs, specifically decentral heating, industrial process

heat for cluster 6 and central dispatchable electricity production. These use cases demand extensive pipeline networks for distribution or significant seasonal storage. E-methane's cost advantage stems from its ability to serve as a "drop-in" replacement for natural gas, effectively leveraging existing natural gas infrastructure, such as transmission, seasonal storage, distribution and end-use conversion, unlike hydrogen, which requires costly modifications to the current system. E-methane's cost-competitiveness is further bolstered by its lower CAPEX intensity, the technological maturity of its downstream processes, its positive emissions impact, its safety advantages and its efficiency in land use and logistics.

Initially, e-methane could be produced using biogenic CO<sub>2</sub>. However, due to feedstock limitations, large-scale adoption will depend on DAC for CO<sub>2</sub> sourcing. While DAC presents significant potential, uncertainties around its costs pose challenges for the long-term cost-competitiveness of e-methane.

Ultimately, e-methane is a promising renewable energy vector for specific use cases with high downstream costs in the Netherlands and similar regions, where established natural gas infrastructure can be leveraged for renewable energy distribution. Its efficiency in terms of capital and operational costs, emissions, safety, land use and transportation makes it a viable vector in the renewable energy mix. Given the capital-intensive nature of the energy transition, adopting e-methane conserves financial and human resources, minimizes delays and enhances societal value, enabling a more resource-efficient transition. However, to realize the full potential of e-methane, it will be essential to advance technological maturity through R&D and demonstration projects, reduce renewable hydrogen production costs and scale DAC solutions to ensure economic viability. Additionally prioritizing high-impact end-use cases and implementing supportive regulatory frameworks will be key to driving e-methane adoption and integration into the future energy mix.

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Renewable energy vectors are critical to the energy transition, especially in sectors that are difficult to electrify. To identify the most viable renewable energy vectors for a net-zero future, a comprehensive comparison at the value chain level is essential. This study aims to evaluate e-methane in comparison to other renewable energy vectors across the entire value chain - from production to transportation, transmission, distribution, storage and end-use - considering both financial and non-financial factors

#### 15 2 E-methane, potentially attractive renewable energy vector

E-methane is a renewable energy vector which can serve as a "drop-in" vector, leveraging the existing natural gas infrastructure and thus minimizing transition costs. When produced using biogenic CO<sub>2</sub> or DAC and combined with CCS at end-use, it will enable negative emissions. While e-methane is expected to become more widely available and cost-competitive in the future, it will still be more expensive than CO<sub>2</sub> compensated natural gas and will require more cohesive regulation to scale up

#### 21 3 End-use cases key in determining viability of renewable energy vector

By 2040, the Netherlands' projected demand for renewable energy vectors will be 137 TWh. Five key use cases are particularly promising for e-methane adoption based on feasibility and projected demand of e-methane. For each use case, considerations in different parts of value chain have been defined for both e-methane and hydrogen

#### 29 4 Key assumptions and boundary conditions

The study aims to provide a relative comparison of financial and non-financial parameters between energy vectors, rather than forecast absolute numbers. Standardized assumptions across energy vectors have been made to ensure a fair and consistent basis for comparison. The analysis assumes a mature, large-scale system with positive technological advancements and an optimized global supply chain by 2040

#### 5 E-methane *van put tot pit:* a financially viable renewable energy vector

E-methane's landed costs are competitive with other renewable energy vectors when delivered in their end-use state. For hydrogen-specific applications, ammonia and liquid hydrogen offer the lowest landed cost. E-methane is cost-competitive for specific end-use cases with high downstream costs, such as decentral heating, industrial process heat for cluster 6 and central dispatchable electricity production. Large-scale e-methane production will increasingly rely on DAC to ensure stable CO2 supplies. Consequently, DAC costs will critically determine e-methane's cost-competitiveness relative to hydrogen

#### 44 6 Comparing e-methane with other energy vectors on criteria beyond cost

Given the capital-intensive nature of the energy transition, the adoption of e-methane allows for the reuse of existing infrastructure, conserving financial and human resources while minimizing delays. With lower upfront costs, e-methane enhances societal value and enables a more resource-efficient energy transition. Its viability is further bolstered by its positive emissions impact, safety advantages and efficiency in land use and logistics

#### 54 7 Conclusions & recommendations

E-methane is a feasible and promising renewable energy vector for specific use cases with high downstream costs in the future energy mix of the Netherlands, but its full potential can only be realized with advancement and cost reduction of technologies for renewable hydrogen production, e-methane synthesis and direct air capture

# The need for renewable energy vectors

Renewable energy vectors are critical to the energy transition, especially in sectors that are difficult to electrify. To identify the most viable renewable energy vectors for a net-zero future, a comprehensive comparison at the value chain level is essential. This study aims to evaluate e-methane in comparison to other renewable energy vectors across the entire value chain - from production to transportation, transmission, distribution, storage and end-use - considering both financial and non-financial factors

he need to address global warming and its impact has led to global initiatives to achieve net-zero greenhouse gas emissions (GHG) or climate neutrality. These plans are rooted in the recognition that human activity, particularly the burning of fossil fuels, has significantly increased the concentration of GHGs in the atmosphere and changed the Earth's climate. To mitigate their impact and limit global temperature rise, the European Union, like many other governing bodies, has set an ambitious goal to achieve climate neutrality by 2050, in line with the Paris Agreement's aim to limit the temperature increase to 1.5 °C above pre-industrial levels.

As part of the EU's net-zero strategy, the Netherlands has committed to substantial GHG emission reductions: 55% by 2030 compared to 1990 and net-zero by 20501. These targets reflect a commitment to transitioning to a sustainable and resilient energy system.

#### In the energy transition, as much of the energy consumption as possible should be electrified while sustainable energy vectors will play a vital role in sectors where electrification is not feasible

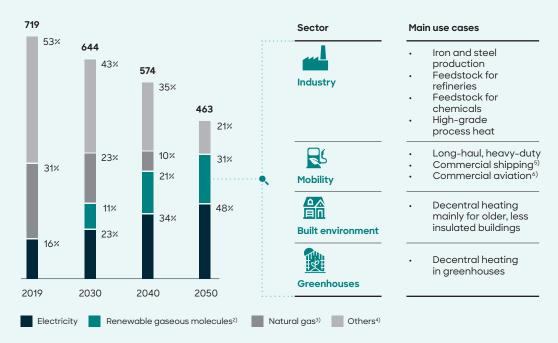
The energy transition relies on multiple levers, with electrifying as much energy consumption as possible being a key priority. Due to their higher efficiency, electric technologies reduce overall energy demand compared to fossil-based systems. For example, electric vehicles and heat pumps are more energy-efficient than conventional combustion technologies. Furthermore, GHG emissions can be minimized by powering electrification through low-emission sources such as solar, wind, geothermal, nuclear and hydropower.

In addition to electrification, energy efficiency measures - such as insulating buildings to reduce heating requirements - are crucial for further lowering energy use. While an increasing number of processes are becoming viable for electrification, it is still likely that no more than 50-60% of the Dutch final energy demand will be electrified by 2050. Sectors like heavy industry, aviation and shipping will not be fully electrified efficiently or economically before 2050. Industrial processes such as chemicals production or iron and steel manufacturing often require high-temperature process heat, which cannot be efficiently supplied by electricity. Certain fossil fuels, such as natural gas, are also used as feedstocks to produce key materials and substances, such as plastics, which require carbon atoms. Such industries and sectors need non-fossil, near-to-total net-zero alternatives if they are to decarbonize.

These so-called sustainable energy vectors such as renewable gaseous molecules (which include renewable hydrogen and its derivates and biomethane), synthetic fuels and biofuels are expected to play an increasingly vital role in replacing fossil fuels and supporting the transition to a net-zero future. The Integrated Infrastructure Outlook 2030-2050 (II3050), which forecasts future energy demand in the Netherlands for different sectors, was used as a starting point for projecting how the share of renewable energy vectors will develop in the Netherlands' future energy mix. ▶ A

<sup>1</sup> The Dutch Climate Law

#### A Renewable gaseous molecules are expected to play an increasingly important role in decarbonizing non-electrifiable sectors [TWh]<sup>1)</sup>



1) Only final energy demand is shown, meaning for example that electricity produced from renewable gaseous molecules (i.e. hydrogen and biomethane) will show as electricity demand. Demand forecasts are taken from the II3050 report, using the EU's International Ambition (IA) scenario for 2030 and the International Trading (INT) scenarios for 2040 and 2050, which are most comparable; 2) Hydrogen (derivatives) and biomethane; 3) Includes imported natural gas; 4) Includes other energy sources such as heat and oil which could also be (partially) delivered by sustainable energy vectors; 5) Excludes international shipping; 6) Excludes international aviation

Source: II3050

#### Sustainable energy vectors will likely form a significant part of the imports needed to meet the Dutch energy demand

The Netherlands has traditionally relied on domestic natural gas, largely from the Groningen gas field². However, with the decline of natural gas production, imports have increased in recent years. To meet GHG reduction targets, the Netherlands aims to boost domestic renewable energy production, primarily from solar and wind. According to the II3050 report, the Netherlands will have around 120 GW in renewable electricity production capacity by 2040: 70 GW from solar PV, 35 GW from offshore wind and 15 GW from onshore wind. In addition, electrolysis capacity for hydrogen production is forecasted at 15 GW³. But even if these forecasts are realized, it will not meet total energy demand in 2040.

Energy imports will therefore be necessary. Most of these imports are expected to come in the form of sustainable energy vectors from regions that are expected to produce a surplus of energy such as the Middle East and North Africa (MENA), the US and southern and northern Europe.

<sup>2 2030-2050</sup> Integrated Infrastructure Outlook, Netbeheer Nederland, 2023

<sup>3</sup> Based on the International Trading (INT) scenario

#### Sustainable energy vectors can be classified into low-carbon and renewable vectors. This study focuses specifically on renewable energy vectors

Sustainable energy vectors can be categorized into low-carbon vectors, derived from fossil sources with carbon mitigating technologies such as carbon capture, and renewable vectors, derived from renewable energy<sup>4</sup> sources such as solar, wind or biomass. For example, blue hydrogen is a low-carbon vector, which can be produced through autothermal reforming of natural gas combined with carbon capture and storage (CCS). These sustainable energy vectors will not only supply energy for sectors that cannot be electrified but also serve as renewable feedstocks for certain industrial processes, such as refining and chemicals production.

Low-carbon vectors are likely to play a key role in the short to medium term due to their costcompetitiveness compared to renewable energy vectors. However, the focus of this study is on renewable energy vectors, as they are expected to be critical in reducing dependency on finite fossil resources and achieving net-zero emissions in the long term.



Renewable energy vectors can be distinguished based on whether their origin was organic or synthetic. > B

Organic renewable energy vectors are derived from organic matter, such as plants or animal waste, which mainly consists of carbon and hydrogen atoms. These carbon atoms come from atmospheric carbon dioxide (CO<sub>2</sub>) absorbed by plants and converted into organic matter. From this matter, gaseous vectors like biomethane (CH<sub>4</sub>) and liquid vectors like biomethanol (CH<sub>3</sub>OH) can be produced.

When organic renewable energy vectors are combusted, CO2 is released back into the atmosphere. This CO2 is considered part of the short carbon cycle, having been recently absorbed by organisms, and is thus considered net-zero emissions. In contrast,

combusting fossil fuels releases CO₂ from the long carbon cycle: that CO2 was absorbed from the atmosphere millions of years ago, and its release contributes to current atmospheric buildup of CO2.

Synthetic energy vectors are chemically produced, starting with renewable electricity. This electricity can split water into hydrogen and oxygen via electrolysis to produce renewable hydrogen, which can either be used directly or converted into other synthetic renewable energy vectors to increase energy density and facilitate transportation or meet specific end-use requirements.

Examples of such hydrogen carriers include liquid organic hydrogen carriers (LOHC), ammonia (NH3) and methanol (CH<sub>3</sub>OH). LOHC can absorb and release

<sup>4</sup> For the purposes of this study, within renewable energy, renewable electricity is defined as electricity generated from solar, wind, hydropower, geothermal or nuclear systems. Although nuclear energy is not classified as renewable in the EU, its carbon emissions are very low. Nuclear can thus be used for production of renewable energy vectors if the average emission intensity of the electricity grid is <18 g  $\rm CO_2e/MJ$ 

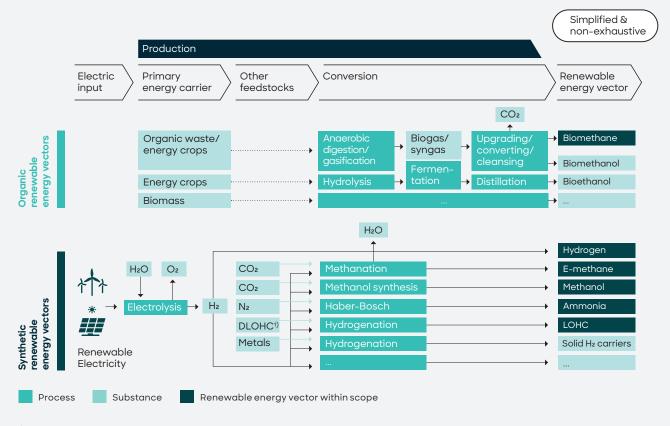
hydrogen, making it transportable like oil. Ammonia, produced from hydrogen and nitrogen via the Haber-Bosch process, liquefies at -33 °C, making it easier to transport than in gaseous form. After transport, ammonia can be potentially reconverted into hydrogen by ammonia cracking or can be directly used as feedstock for fertilizers or fuel for applications such as shipping and electricity. Methanol, produced either organically or synthetically, can also be transported as a liquid (under room temperatures) and later reconverted to hydrogen or used directly as chemical feedstock or fuel for applications such as shipping. Hydrogen can also be converted into solid hydrogen carriers such as sodium boron hydride, iron hydride and magnesium hydride. These solid hydrogen carriers are being further explored in initiatives such as

the Iron Power alliance. However, this and other solid hydrogen carriers are considered out of scope for the purpose of this study due to the relatively lower technological maturity compared to other hydrogen carriers.

Like methanol, renewable methane (CH4) can be produced either organically or synthetically. Methane from an organic source is called biomethane, while synthetic methane is also known as e-methane.

E-methane is produced through methanation of hydrogen produced through electrolysis and CO2. The notable aspect of renewable methane is that it is chemically close to natural gas, allowing the use of existing natural gas infrastructure and equipment for its transportation, storage and end-use. Additionally, renewable methane can be reconverted back to hydrogen if needed.

#### B Organic renewable energy vectors are produced from biomass, whereas synthetic renewable energy vectors are produced from renewable hydrogen



1) Dehydrogenated liquid organic hydrogen carrier

 $Source: European \, commission, Desk \, research$ 

#### Within renewable energy vectors, this study takes a close look at e-methane and compares it to renewable hydrogen (derivatives) from beginning to end of the value chain considering both financial and non-financial factors

Over the years, numerous studies - e.g. from leading organizations International Energy Agency (IEA) and International Renewable Energy Agency (IRENA) - have compared renewable hydrogen and its derivatives, focusing primarily on the initial stages of the value chain: from production to long-distance transportation and reconversion. The costs and challenges in the latter stages of the value chain, including storage, distribution and enduse conversion, are rarely considered. Yet local investments in these downstream stages will be essential to ensure the scalability and viability of renewable energy vectors. They are not just operationally significant, they will drive the overall cost-effectiveness, reliability and integration of the vectors into the economy.

Moreover, most existing studies tend to focus on a single aspect of comparison, such as financial metrics, GHG emissions intensity, or technological maturity. While these analyses are valuable, they do not offer the integrated perspective necessary for informed decisionmaking. Thus, a comprehensive comparison of energy vectors across the entire value chain (van put tot pit) is required.

This study seeks to address these gaps by evaluating both the financial and non-financial feasibility of e-methane and comparing it to renewable hydrogen and its derivatives from beginning to end of the value chain. Despite its potential advantages in the latter value chain stages of transportation, storage and end-use conversion, e-methane has rarely been the subject of renewable energy vector studies. Only recently have Agora<sup>5</sup> and Frontier<sup>6</sup> compared e-methane with renewable hydrogen and its derivatives, but these studies focused only on the initial value chain steps. A recently published multi-criteria analysis (MCA)<sup>7</sup> of hydrogen carriers in the Netherlands does include e-methane for comparison throughout the value chain but provides only a high-level cost estimate that is largely based on the HyDelta report8.

This comprehensive assessment of e-methane and other vectors thus incorporates financial factors, GHG emissions, technology readiness levels (TRL) and safety considerations, and does so across the entire value chain. By examining all these dimensions, this study offers a nuanced evaluation that will enable stakeholders to identify the most suitable renewable energy carrier for specific situations.

It is important to note that multiple renewable energy vectors likely will coexist in the future. However, each vector requires local infrastructure, ranging from import and storage facilities to transportation networks and end-use conversion equipment. Given the investment costs and spatial requirements, developing full infrastructure for each renewable energy vector

<sup>5</sup> Hydrogen import options for Germany, 2023

Comparative analysis of import costs of synthetic methane to Germany, 2024

Comparison of hydrogen carriers - Multi-criteria analysis of supply chains in the Netherlands, 2024

Value Chain Analysis - Hydrogen value chain literature review, 2021; Risks, uncertainty and collaboration in the hydrogen-based value chain - Technical analysis of hydrogen supply chains, 2023

likely is uneconomical and given the required man-power likely is unfeasible. Consequently, choices must be made based on use cases of the vectors in all aspects of the value chain.

#### The goal of this study is to evaluate the feasibility and potential of e-methane within the future energy mix of the **Netherlands**

This study aims to investigate the potential of e-methane alongside other renewable energy vectors biomethane, hydrogen, LOHC, ammonia and methanol. Using 2040 as the reference year, this study therefore provides a long-term perspective, extending towards 2040 and beyond, on the future energy mix in the Netherlands in terms of:

- Demand for renewable energy vectors through the lens of various use cases in the
- The cost-competitiveness<sup>9</sup> of renewable energy vectors across the entire value chain
- Additional factors such as technological maturity, environmental impact, safety characteristics and land-use efficiency

The study is structured as follows: Chapter 2 introduces the e-methane energy vector and the status of its development. Chapter 3 identifies the key use cases that are potentially attractive for e-methane. Chapter 4 outlines the boundary conditions and key input assumptions used in the study. Chapter 5 compares the cost of e-methane to other energy vectors for identified use cases. Chapter 6 evaluates the energy vectors on non-financial parameters such as emissions, safety and land use. Chapter 7 presents the conclusions and recommendations of the study.

Cost-competitiveness only includes actual costs and excludes government subsidies or other financial schemes



A typical value chain for renewable energy vectors imported into the Netherlands begins with production. This involves producing the primary energy carrier, such as biomass or renewable hydrogen, and converting it into the renewable energy vector. > C

The next step is long-distance transportation, where the renewable energy vector is first prepared for transportation - either compressed for pipelines or liquefied for vessels - and then transported. Shipping also includes storage at both the production and

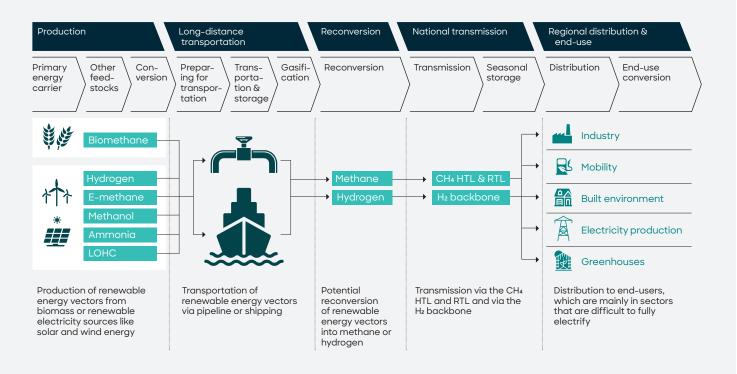
import locations, followed by gasification at the import location if the vector was liquefied.

The third step involves the potential reconversion of the renewable energy vector into hydrogen, depending on the end-use. For instance, oil refining requires hydrogen, necessitating reconversion. Conversely, in fertilizer production, ammonia is needed, so reconversion is unnecessary if the renewable energy vector is ammonia.

After potential reconversion, the renewable energy vector enters the national transmission network, which may include seasonal storage. The Netherlands has an extensive transmission and storage network for methane, which includes main (HTL) and regional (RTL) transmission pipelines. There are also plans to develop a hydrogen backbone by 2030<sup>10</sup>, including sufficient storage capacity to operate the system. This would require repurposing part of the existing HTL and RTL from methane to hydrogen, including the necessary adjustments. The transmission methods for other vectors like ammonia and methanol are still being determined.

Finally, the renewable energy vectors are distributed to end-users. The final step varies greatly depending on the use case. While for e-methane, most existing end-use equipment for natural gas can likely be used as-is, additional investments are likely required to adapt the equipment to be suitable for other energy vectors like hydrogen.

The value chain for renewable energy vectors includes production, transportation, reconversion, national transmission, regional distribution and end-use



<sup>10</sup> Hynetwork roll-out plan (https://www.hynetwork.nl/ en/about-hynetwork/the-roll-out-plan)

# E-methane, potentially attractive renewable energy vector

E-methane is a renewable energy vector which can serve as a "drop-in" vector, leveraging the existing natural gas infrastructure and thus minimizing transition costs. When produced using biogenic CO<sub>2</sub> or DAC and combined with CCS at end-use, it will enable negative emissions. While e-methane is expected to become more widely available and cost-competitive in the future, it will still be more expensive than CO<sub>2</sub> compensated natural gas and will require more cohesive regulation to scale up



he Netherlands' transition to net zero involves substantial changes in the energy mix. Natural gas, which comprises about one-third of the country's energy supply<sup>11</sup>, primarily consists of methane (85-90%) alongside smaller quantities of hydrocarbons like ethane and propane, as well as traces of non-hydrocarbon gases such as CO2 and nitrogen. The exact makeup of natural gas can vary depending on its source, including conventional reservoirs, shale formations or coal seams.

#### E-methane can serve as a "drop-in" vector, leveraging the existing natural gas infrastructure and thus minimizing transition costs

An option for decarbonizing the Dutch energy supply is e-methane, a renewable gas created by combining renewable hydrogen with GHG-neutral CO<sub>2</sub>. E-methane can be synthesized to meet the specific compositions of L-gas and H-gas<sup>12</sup> utilized in the Netherlands, making it nearly identical to natural gas in terms of combustion properties, calorific value and behavior within pipeline systems. This alignment enables e-methane to serve as a "drop-in" replacement, effectively leveraging the existing natural gas infrastructure - such as LNG terminals, vessels, storage facilities, pipelines and end-use equipment. By doing so, it has the potential to minimize additional downstream investments needed during the energy transition. While e-methane's production costs will be higher than hydrogen due to the additional conversion step, its ability to minimize infrastructure changes may offset these costs. This allows for a less disruptive and therefore possibly less costly shift from fossil fuels to renewable energy vectors - while still meeting the aims of the Paris Agreement.

#### E-methane is a renewable energy vector with a carbon neutral cycle, as the CO<sub>2</sub> emitted during combustion equals the CO<sub>2</sub> captured during its production

E-methane is synthesized by combining CO<sub>2</sub> captured from biogenic point sources or from the air via direct air capture (DAC) with renewable hydrogen produced via electrolysis<sup>13</sup>. When combusted, e-methane releases the same amount of CO2 which was previously captured during its production - thus effectively resulting in a carbon neutral cycle with no net increase in CO2 emissions to the atmosphere. In combination with CCS of the CO2 released during combustion, even negative emissions can be achieved. E-methane can also be created with CO2 captured from the combustion of fossil fuels. In this case, the fossil source from which the CO₂ is captured is considered the CO₂ emitter.

#### The Sabatier method remains the only commercialized synthesis method for e-methane - for now

E-methane can be produced via several methods, including Sabatier methanation, hybrid methanation, direct methanation and biological methanation. Currently, the Sabatier pro-

<sup>12</sup> L-gas refers to low-calorific gas (from the Groningen gas field) and H-gas refers to high-calorific gas (from most

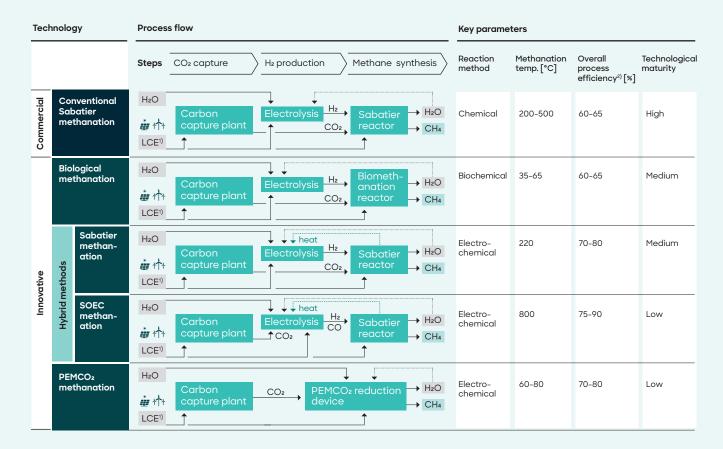
<sup>13</sup> The RED II Delegated Act restricts the eligibility of CO₂ captured from industrial activities until 2041 (or 2036 for CO₂ from electricity production) for RFNBO, meaning that only CO2 captured through DAC or from biogenic sources can be used for e-methane production after 2040 if used as RFNBO

cess is the only commercially viable method. It involves a chemical reaction between hydrogen and CO<sub>2</sub> over a nickel catalyst at 200–500 °C, achieving an overall process efficiency of both electrolysis and methanation of about 65%. D

Emerging technologies such as biological methanation leverage microorganisms to catalyze the reaction between hydrogen and CO<sub>2</sub> at low temperatures, achieving efficiencies of up to 65%. Hybrid methods improve efficiency by utilizing heat from the exothermic reaction to support hydrogen production. Examples include conventional Sabatier methanation integrated with hydrogen electrolysis and solid oxide electrolyzer cell (SOEC) methanation. In SOEC methanation, water and CO<sub>2</sub> are co-electrolyzed to produce hydrogen and carbon monoxide (CO), which are subsequently converted to methane, potentially achieving efficiencies of up to 90%. Direct methanation combines water electrolysis and CO<sub>2</sub> reduction in a single step using proton–exchange membrane (PEM) electrolysis, achieving efficiencies of up to 80%. These emerging methods represent promising advancements in the efficiency and scalability of e-methane production in the future.

#### There are five main methods to synthesize e-methane, but Sabatier is the only commercialized method

Simplified & non-exhaustive



1) Low carbon energy; 2) Figure comprises efficiency of electrolysis and methane synthesis

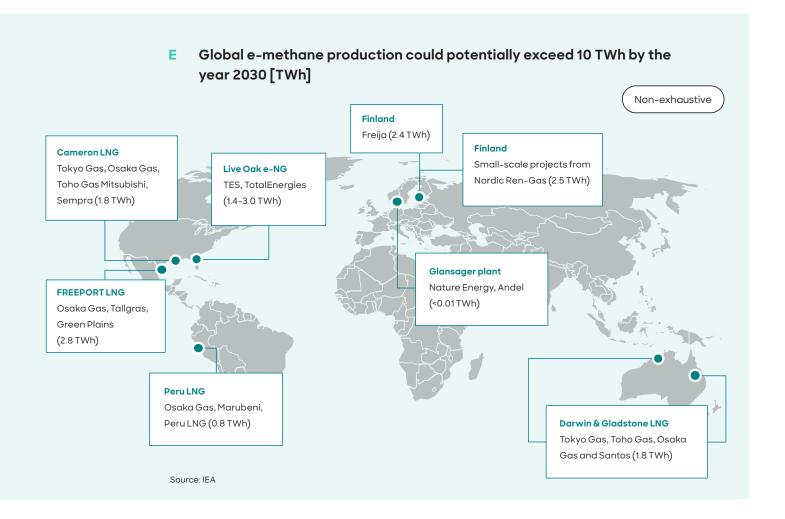
Source: Japan Gas Association, IEA, Store & Go, DENA

Despite the potential of these newer methods to improve efficiency, they are not yet commercially available, making Sabatier methanation the most viable production method for e-methane today. It is therefore the reference production method in this study.

#### E-methane is gaining momentum, with global production expected to exceed 10 TWh by 2030

The IEA projects global e-methane production could exceed 10 TWh by 203014, contingent on securing investments in ongoing projects. ▶ E These projects are in regions with abundant and low-priced renewable electricity, primarily the US, Australia and the Nordics, with over 50% of supply expected from the US. Japan positions itself as a leader in e-methane development, aiming to source 1% of city gas from e-methane by 2030 and 90% by 2050, with major investments in large-scale production abroad, including in Cameroon and the US. In Europe, TES is planning to build an e-methane import hub in Germany<sup>15</sup>, while Ren-Gas leads small-scale projects in Finland targeting 2.5 TWh. The sector is also gaining momentum with the formation of the global e-NG16 coalition, which includes several industry leaders17.

<sup>17</sup> https://www.eng-coalition.org/



<sup>14</sup> E-methane - a new gas for a net-zero future, IEA

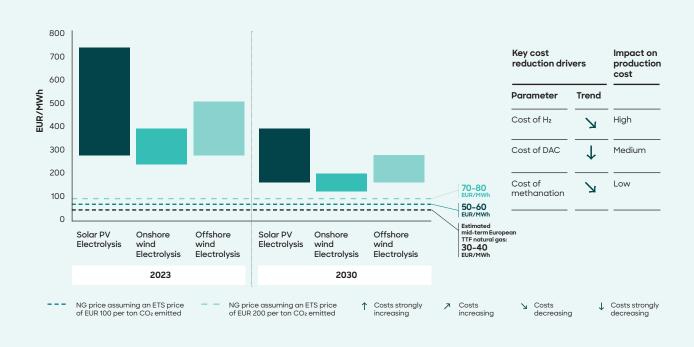
<sup>15</sup> TES is planning to build an LNG import terminal in Germany with the aim to later import e-methane produced in US

<sup>16</sup> E-natural gas is synonymous with e-methane

#### E-methane production costs are expected to drop by 2030, though not below the cost of natural gas

Based on IEA calculations, current e-methane production costs are in the range of 250-700 EUR/MWh. This is largely driven by the cost of renewable hydrogen and the GHG-neutral COz. By 2030, e-methane production costs are expected to drop to 150-300 EUR/MWh due to reductions in the costs of renewable hydrogen and carbon capture, improved methanation efficiency and economies of scale. > F However, even at these lower costs e-methane production costs remain several times that of natural gas, which is expected to be priced at EUR 50-80 EUR/MWh, including the ETS price.

According to IEA, current e-methane costs are in the range of 250 -700 EUR/MWh (3-12 x NG prices including ETS) - Costs projected to decrease by 2x by 2030 [EUR/MWh]



Source: IEA, Desk research

#### E-methane is expected to meet renewable fuel regulations globally, but a more cohesive regulatory framework is essential for its scale-up

E-methane is expected to meet the regulatory requirements for renewable fuel in key regions such as the US, EU and Japan. For example, e-methane can be classified as a renewable fuel of non-biological origin (RFNBO) under the EU's Renewable Energy Directive (RED) II.

However, the regulatory framework for e-methane is still in the early stages of development. While existing policies like the EU Green Deal indirectly support the transition to e-methane, they do not explicitly identify e-methane as a primary energy vector for decarbonization.

That being said, the source of CO2 used in methane synthesis is increasingly scrutinized in global legislation. The International Organization for Standardization (ISO) has established international standards for calculating the carbon footprint of e-methane, allowing CO2 from air, biogenic sources, or a company's own operations to be considered eligible. Japan's Clean Gas Certificate scheme allows the use of CO2 for e-methane as long as it does not contribute to an increase in atmospheric CO2 levels upon combustion, though it does not specify the exact eligible CO2 sources. In the EU, the RED II Delegated Act restricts the eligibility of CO₂ captured from industrial activities until 2041 (or 2036 for CO₂ from electricity production), meaning that only CO₂ captured through DAC or from biogenic sources can be used for e-methane production after 2040. In line with these EU regulations, this study considers only CO₂ captured from biogenic sources or via DAC for e-methane production, as well as for methanol production which is produced via renewable hydrogen and captured carbon.

While e-methane is contributing to carbon reduction targets today, the regulatory environment remains fragmented and in development. For large-scale deployment, enhanced and more cohesive regulations will be essential to scale up e-methane production.

### End-use cases key in determining viability of renewable energy vector

By 2040, the Netherlands' projected demand for renewable energy vectors will be 137 TWh. Five key use cases are particularly promising for e-methane adoption based on feasibility and projected demand of e-methane. For each use case, considerations in different parts of value chain have been defined for both e-methane and hydrogen



valuating the feasibility and potential of e-methane in comparison with other renewable energy vectors requires analyzing a number of end-use cases in which demand for renewable gaseous molecules is significant and e-methane is a feasible option to meet that demand.

#### Projected demand in 2040 for renewable gaseous molecules is 137 TWh

E-methane and other renewable energy vectors are expected to be crucial for decarbonizing sectors that are difficult to electrify fully, such as industry, dispatchable electricity production, the built environment and greenhouses. Key sectors like fertilizers and refineries will also rely on these renewable energy vectors as feedstock. The future demand for renewable molecules will depend on factors like industrialization trends, electrification progress and grid capacity. To estimate the projected demand in the Netherlands, the II3050 report has been used as a reference for this study.

This study uses the international trading (INT) scenario as the reference case for projecting energy demand in the Netherlands<sup>18</sup>. The INT scenario assumes an important role for international supply chains and global trading of renewable energy vectors. The choice for this scenario was driven by the belief that coordinated global efforts are essential for achieving climate neutrality, given the shared nature of the climate crisis. The choice of scenario influences the cost of transporting renewable energy vectors in the Netherlands, as the costs directly depend on the total transported volume. The higher the volume the lower the cost per transported MWh. The study will also determine the sensitivity of other scenarios to transportation costs.

The II3050 report does not explicitly mention or forecast future e-methane demand. As e-methane has similar use cases to both hydrogen and biomethane, this study considers the total hydrogen and biomethane demand as the total addressable market for e-methane (and other renewable energy vectors). For the purpose of this study, renewable hydrogen and renewable methane (i.e. biomethane and e-methane) are collectively referred to as renewable gaseous molecules.

The total projected demand for renewable gaseous molecules in the Netherlands in 2040, according to the INT scenario, is 137 TWh<sup>19,20</sup>. The largest share of this demand (72 TWh) is expected from industry, followed by mobility, the built environment, electricity production and greenhouses. ▶ G

 $<sup>18 \</sup>quad \text{The II} 3050 \, \text{report outlines four scenarios for the future energy transition, varying in the degree of government}$  $control\ versus\ market-driven\ developments.\ Moreover,\ the\ scenarios\ differ\ in\ the\ scale\ of\ the\ transition\ -\ whether\ developments\ whether\ developments\ developments\$ national, regional or international - and consider the varying technology and energy carrier choices made by different sectors. The four scenarios are decentral initiatives (DEC), national leadership (NAT), European integration (EUR) and international trading (INT). For further details on the II3050 report, please refer to the appendix

<sup>19</sup> In each use case, demand refers to domestic demand in the Netherlands and does not account for international demand. For example, the demand for renewable gaseous molecules in shipping is based solely on domestic requirements and does not include fuel bunkering for international shipping

<sup>20</sup> Figure A shows the final energy demand for renewable gaseous molecules in 2040, which is 121 TWh. That number does not include renewable gaseous molecule demand for electricity production and district heating, which is included in the 137 TWh given here

#### G Demand for renewable gaseous molecules is expected to be driven primarily by the industrial, mobility and built environment sectors [TWh]

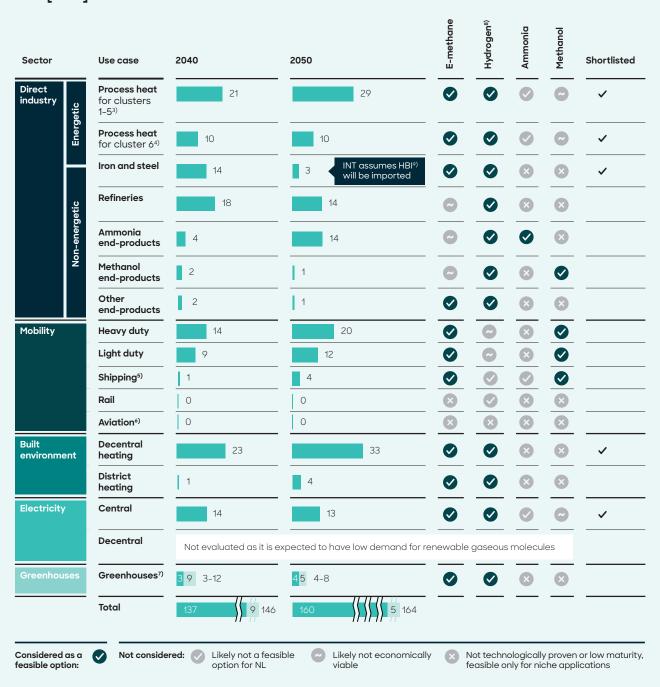


industry	ţi	for clusters 1-5 <sup>1)</sup>		heat for industrial processes across different industries <sup>3)</sup>
	Energetic	<b>Process heat</b> for cluster 6 <sup>2)</sup>	10	
		Iron and steel	14	Methane or hydrogen used for moderate and high-temperature heat and as feedstock for steel production
	<u>.9</u>	Refineries	18	Hydrogen used as feedstock for hydrocracking and desulfurization to produce petroleum products
	Non-energetic	Ammonia end-products	4	Hydrogen or ammonia used as feedstock to produce ammonia end-products in the chemicals industry
	Non-	Methanol end-products	2	Hydrogen or methanol used as feedstock to produce methanol end-products in the chemicals industry
		Other end-products	2	Methane and/or hydrogen used as feedstock to produce several other end- products in the chemicals industry
Mobility		Heavy duty	14	Renewable gaseous molecules used as fuel for trucks and buses
		Light duty	9	Renewable gaseous molecules used as fuel for cars and vans
		Shipping <sup>4)</sup>	1	Renewable gaseous molecules used as fuel for inland shipping
		Rail	0.1	Renewable gaseous molecules used as fuel for freight and passenger trains
		Aviation <sup>5)</sup>	0.04	Renewable gaseous molecules used as fuel for domestic (cargo) flights
Built environment		Decentral heating	23	Renewable gaseous molecules used for decentral heating and other energy use of residential and utility buildings
		District heating	1	Renewable gaseous molecules used for heating water, which is centrally distributed to residential and utility buildings
Electricity		Central	14	Renewable gaseous molecules used for centralized power plants for flexible electricity generation
		Decentral	06)	Renewable gaseous molecules used for decentralized power plants for electricity generation for local use
Greenhouse	s	Greenhouses	3	Renewable gaseous molecules used for decentral heating of greenhouses for agriculture

<sup>1)</sup> Includes refineries and ammonia, methanol and other end-products; 2) Includes the food and beverage industry, paper industry and other industries; 3) Excludes demand for high-temperature heat for iron and steel production; 4) Excludes -60 TWh forecasted demand for international bunkering of synthetic and biofuels in the Netherlands, based on IRENA report on decarbonizing the shipping sector, which estimates 3.5 EJ of 8.5 EJ total global shipping demand in 2040 to be for synthetic and biofuels and 6% of global bunkering to be in the Netherlands; 5) Excludes -20 TWh forecasted demand for synthetic aviation fuel (SAF) for international aviation in the Netherlands in 2050, based on INT scenario in Il3050 report; 6) Not evaluated as it is expected to have little demand for renewable gaseous molecules

Source: II3050

H Iron and steel, process heat, decentral heating and central dispatchable electricity production are shortlisted as main use cases for e-methane to further deepdive [TWh] 1), 2)



1) Figure details the applicability of the renewable energy vectors as a final energy form for the end use case. For example, hydrogen for process heat can be delivered as hydrogen or via ammonia or other liquid hydrogen carriers; 2) For further details on applicability of energy vectors per use case, please refer to the appendix document; 3) Includes refineries and ammonia, methanol and other end-products; 4) Includes the food and beverage industry, paper industry and other industries; 5) Excludes -60 TWh forecasted demand for international bunkering of synthetic and biofuels in the Netherlands, based on IRENA report on decarbonizing the shipping sector, which estimates 3.5 EJ of 8.5 EJ total global shipping demand in 2040 to be for synthetic and biofuels and 6% of global bunkering to be in the Netherlands; 6) Excludes -20 TWh forecasted demand for synthetic aviation fuel (SAF) for international aviation in the Netherlands in 2050, based on INT scenario in Il3050 report; 7) Light green bar represents demand from district heating, potentially to be served by renewable gaseous molecules; 8) Hydrogen as a molecule for end-use, also includes other molecules as hydrogen carriers; 9) Hot briquetted iron

Source: II3050, Desk research

In industry, renewable gaseous molecules can provide moderate to high-temperature process heat, which is difficult to electrify. They are also needed as essential feedstock for chemical processes, enabling the production of key materials and reducing reliance on fossil inputs.

In mobility, demand is primarily driven by heavy-duty transportation, while in the built environment, it is driven by (hybrid) decentral heating for residential and utility buildings. In electricity production, renewable gaseous molecules will play a role in dispatchable power production to balance the intermittency of renewable energy sources like wind and solar, which are forecasted to provide most of the electricity produced.

#### Five key use cases were selected for deeper analysis based on their feasibility for e-methane and projected demand in 2040

The projected renewable gaseous molecule demand could be met by several renewable energy vectors. This study considers e-methane alongside hydrogen, ammonia and methanol. > H It is important to note that this is considering the form in which the molecule is consumed in the end-use conversion step. Therefore, any energy vector used as a hydrogen carrier (e.g. ammonia, LOHC or methanol) that is imported to the Netherlands and then reconverted into hydrogen before use will be represented in this overview as hydrogen, rather than the original energy vector.

E-methane could fulfill up to 80% of the renewable gaseous molecule demand in the Netherlands, but this study narrows its scope to five end-use cases<sup>21</sup>:

- Iron and steel
- Process heat for clusters 1-5
- Process heat for cluster 6
- Decentral heating in the built environment.
- Central dispatchable electricity production

These cases were selected based on two criteria: 1) they must be feasible for e-methane use and 2) they must have significant renewable gaseous molecule demand in 2040. For example, ammonia end-products are excluded as a feasible use case since the sector requires either hydrogen or ammonia directly as an energy vector. Although hydrogen can be produced from e-methane through steam methane reforming, using e-methane to produce hydrogen is energy and cost-inefficient, making it an uneconomic and illogical option. Together, these five use cases are forecasted to represent more than 70% of the total Dutch e-methane demand.

For the five selected use cases, e-methane and hydrogen are the primary energy vectors. Their roles in each value chain step are explored further.

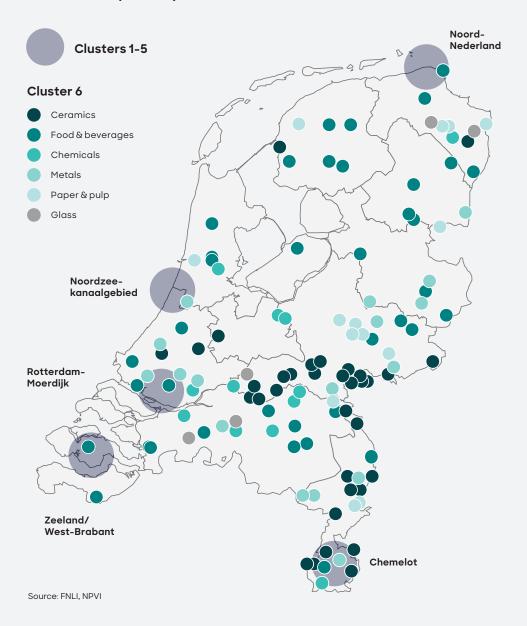
<sup>21</sup> Mobility is a relevant sector for e-methane; however, many use cases within this sector either have a smaller  $share of downstream \ costs in the total value \ chain (e.g. \ shipping) \ or \ would \ require \ similar \ new \ infrastructure \ for \ both$ e-methane and hydrogen (e.g. heavy-duty transport). Since the downstream value chain setup would not significantly differ between the two vectors, mobility use cases were not prioritized for comparison in this study



In the Netherlands, industries are segmented into six clusters based on their geographical distribution. > Clusters 1 to 5 consist of large, geographically concentrated industrial hubs that include sectors like refineries, chemicals and metallurgy. Example companies in these clusters include TATA Steel (iron and steel), OCI (chemicals), Shell (petrochemicals) and

Nobian (chemicals). In contrast, cluster 6 is dispersed across the country and comprises industries such as ceramics, food and beverages, metals, paper and pulp and glass production. Examples of companies in this cluster are Wienerberger (ceramics), FrieslandCampina (dairy) and Ardagh Group (metal and glass packaging).

#### There are primarily six industrial clusters in the Netherlands



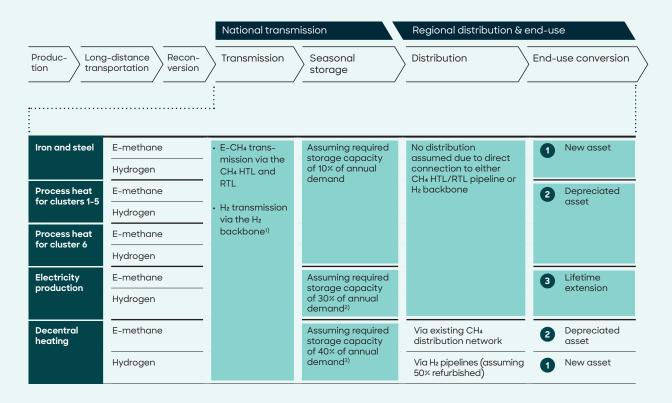
#### Considerations of different value chain steps have been further defined for each use case for both e-methane and hydrogen

The five selected use cases are further detailed for the final value chain steps after reconversion - that is, transmission, seasonal storage, distribution and end-use conversion. > J

In transmission, e-methane can utilize the existing natural gas infrastructure (HTL and RTL), while hydrogen will rely on the planned hydrogen backbone. In addition to the hydrogen backbone, some use cases, such as central dispatchable electricity production and process heat for cluster 6, may require additional pipelines to connect to the hydrogen backbone.

Seasonal storage requirements differ based on demand profiles: 40% of the demand for decentral heating is expected to go into long-term storage, ideally in depleted gas fields. For

#### For the final value chain steps different considerations are relevant per use case



1) Additional dedicated pipelines assumed to connect power plants and cluster 6 to the hydrogen backbone. Other options also exist, such as blending hydrogen and methane in existing pipelines, 2) To accommodate flexible electricity production in times of high electricity demand and low renewable electricity supply; 3) To accommodate storage of additional produced energy in summer for additional energy demand in winter

Source: Interviews with industry experts, Desk research

central dispatchable electricity production, 30% is expected to be stored, with salt caverns being more suitable due to short-term availability needs. Industrial use cases (iron and steel, process heat) require only limited seasonal storage, with 10% expected to be stored in salt caverns<sup>22</sup>.

Of the selected use cases, only decentral heating will require the distribution network, as the other use cases likely will be connected directly to the transmission network<sup>23</sup>.

End-use conversion options include:

- Purchasing new assets
- Using existing assets that are financially depreciated but still functional
- Investing in asset lifetime extensions

For iron and steel, only new assets are feasible as it requires moving from a blast furnace to a direct reduced iron process (option 1), while process heat and central dispatchable electricity production can use both new and existing assets with necessary adaptations for hydrogen use. It is assumed that most industrial boilers will be depreciated, but not yet at the end of their lifetime (option 2) for process heat, whereas for electricity it is assumed that most of the existing natural gas-fired power plants will require lifetime extension by 2040 (option 3). For decentral heating, e-methane can use existing natural gas boilers (option 2), while hydrogen will require new boiler installations (option 1) due to compatibility issues. For both e-methane and hydrogen, it is assumed that existing natural gas boilers are fully depreciated.

<sup>22</sup> Storage percentage for each use case has been calculated based on input from industry experts. Central dispatchable electricity production and industrial applications are expected to require flexible, multi-cycle storage,  $making\ salt\ caverns\ the\ ideal\ choice.\ In\ contrast,\ depleted\ gas\ fields\ are\ better\ suited\ for\ long-term,\ single-cycle$ storage.

<sup>23</sup> Some industries in cluster 6 are also connected via the distribution pipeline; however, for simplicity, this study assumes that cluster 6 is directly connected to either the HTL/RTL pipelines or the  $\rm H_2$  backbone

## Key assumptions and boundary conditions

The study aims to provide a relative comparison of financial and non-financial parameters between energy vectors, rather than forecast absolute numbers. Standardized assumptions across energy vectors have been made to ensure a fair and consistent basis for comparison. The analysis assumes a mature, large-scale system with positive technological advancements and an optimized global supply chain by 2040



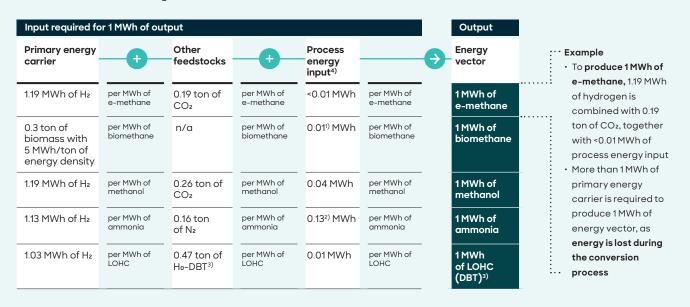
he Netherlands is expected to meet part of its renewable energy vector demand through imports from regions with ample, low-cost renewable energy resources capable of producing a surplus beyond local needs. These include areas like MENA, the US, southern Europe and northern Europe and, to some extent, Australia and South America. To streamline the study, the current analysis focuses on MENA, the US and southern and northern Europe as potential import hubs to meet Dutch renewable energy demands.

For medium to longer distances, transportation of the renewable energy vectors is primarily through pipelines or shipping. The choice of transportation method from these export locations is influenced by the proximity of the production region and its infrastructure. In this study, imports from southern Europe and northern Europe are assumed to utilize pipeline infrastructure. In contrast, imports from the US and MENA rely primarily on shipping. The report further assumes that all Dutch demand for renewable energy vectors will be met via these strategic import routes, ensuring a like-for-like comparison across the entire value chain.

#### For the selected end-use cases, energy delivered via renewable methane or hydrogen is compared

This analysis compares final energy delivered for selected end-use cases, using both methane and hydrogen as vectors. For methane, both e-methane and biomethane (in gaseous and liquid forms) are considered. For hydrogen, gaseous and liquid hydrogen are included, along with three hydrogen vectors: ammonia, methanol and LOHC, all converted back to hydrogen for end-use. Stoichiometric inputs have been assumed for each energy vector in the analysis to ensure consistency across scenarios.

#### Stochiometric inputs vary based on the type of energy vector [per MWh of energy vector produced]



1) Figure comprises electricity and heat used to produce biomethane; 2) Energy consumption includes electricity needed for nitrogen separation from air; 3) LOHC = liquid organic hydrogen carrier, DBT = dibenzyltoluene, a type of LOHC; Ho-DBT = dehydrogenated DBT, Ho-DBT = hydrogenated DBT; 4) Only the energy required to make the energy vector is included. Any energy required to synthesize feedstock is not included here

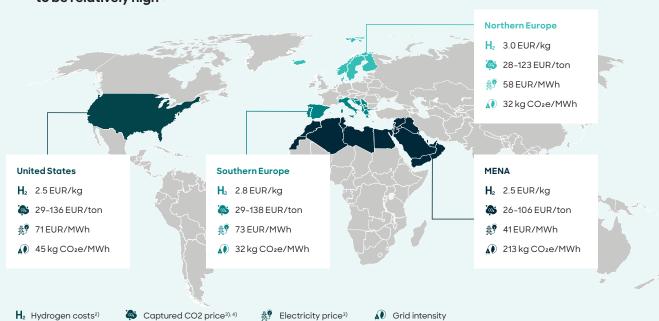
Source: Agora, CE Delft, HyDelta, EU LCA, IEA, IRENA, Desk research

#### For the renewable energy vectors in scope, assumptions across the value chain have been made

This study aims to provide a relative comparison of financial and non-financial parameters between energy vectors, rather than forecast absolute numbers, as these depend on numerous factors outside the scope of the study. Most of the assumptions used throughout the value chain are based on public sources, providing a foundation for the analysis.

The renewable energy vectors evaluated also vary in maturity and are subject to technological and cost uncertainties, as some technologies have not yet been proven at an industrial scale. The analysis assumes a mature, large-scale system with positive technological advancements and an optimized global supply chain featuring centralized conversion/liquefaction and reconversion/gasification infrastructure by 2040. Consequently, assumptions for currently immature technologies are estimates of a future state and inherently carry lower confidence levels compared to those for already mature technologies. Key assumptions - such as the cost of renewable hydrogen, CO2 capture price, electricity prices and grid emission intensity – are standardized across regions to enhance comparability<sup>24</sup>.

MENA is expected to offer competitive costs across regions for renewable hydrogen and lowest price for captured CO2 and electricity in 2040 - Grid intensity of MENA is projected to be relatively high1)



1) Renewable hydrogen costs for 2040 are based on the IEA forecast for 2030, with WACC at 6%, and underlying assumptions that 2030 assumptions are optimistic and forecasted price is expected to be closer to the latter half of the 2030s. CO2 capture price estimates vary, with the lower bound representing capture from high-purity biogenic sources like bioethanol, and the upper bound reflecting DAC with energy consumption of 1 MWh per ton of CO $_2$  captured. In the absence of reliable electricity price data for MENA, the region's electricity price is assumed to be 60% of the US price; 2) Produced via captive renewable power; 3) Prices are based on baseload hours; 4) Study assumed TOTEX cost excl. electricity consumption of 25 EUR/ton for biogenic point-source and of 65 EUR/ton for DAC and an electricity consumption of 0.1 MWh/ton for biogenic point-source and 1 MWh/ton for DAC

Source: IEA, NETL, Natuur & Milieu, Bavarian industry association (VBW), E-bridge

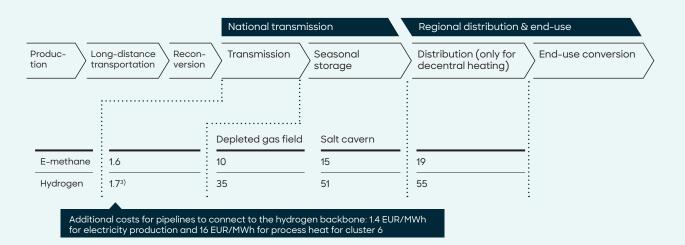
<sup>24</sup> For further details on assumption per energy vector per value chain step per use case, please refer to the appendix

The cost of renewable hydrogen follows IEA projections with a captive renewable setup, while grid electricity, with its associated emissions, is assumed for the rest of the value chain. Most of the upstream value chain - conversion to transportation (excluding pipelines) and reconversion - is modeled purely on operational costs without factoring in the cost of capital or margins. In contrast, pipeline transportation and the downstream segment, encompassing transmission, storage and distribution (regulated assets) incorporate tariffs calculated using the weighted average cost of capital (WACC), accurately reflecting regulatory conditions. WACC is excluded from the upstream segment due to varying regional risk profiles and investor return expectations, making reliable estimates challenging. This approach allows for a focused comparison of cost-competitiveness across energy vectors while respecting downstream regulatory contexts.

For long-distance maritime transportation, vessels carrying methane or liquid hydrogen are assumed to use boil-off gas as their primary fuel source, leveraging the evaporative losses from cryogenic storage to power the engines. In contrast, ships transporting ammonia and methanol will combust a portion of the cargo itself as fuel, balancing efficiency with fuel availability en route. For vessels transporting LOHC, it is assumed that e-methanol is used as fuel.

For downstream costs related to transmission, distribution via pipelines and seasonal storage within the Netherlands, bottom-up cost calculations have been conducted. These calculations are based on extensive literature reviews and stakeholder inputs to ensure that the assumptions are aligned with industry insights and the latest research.

#### Downstream costs have been assumed per value chain step [EUR/MWh]1),2)



1) Power plants and industrial activities in cluster 6 will require dedicated pipelines to connect to the hydrogen network, adding significant costs. Especially for cluster 6, replacing natural gas pipelines with hydrogen-compatible infrastructure introduces complexities, making pipeline costs 2-3 times higher than standard pipelines. Additionally, the limited hydrogen volumes required in this cluster 6 exacerbate the per-unit cost, resulting in a high overall cost for pipeline infrastructure in cluster 6; 2) For the hydrogen backbone, 70% refurbishment of pipelines is assumed; for all other hydrogen pipelines (additional transmission pipelines and distribution pipelines), 50% refurbishment is assumed; 3) The hydrogen tariff was calculated before the new cost estimate for the proposed Dutch hydrogen pipeline network was made public, revealing a 2.5x increase from EUR 1.5 bn to EUR 3.8 bn

Source: Roland Berger comprehensive value chain model

### E-methane van put tot pit: a financially viable renewable energy vector

E-methane's landed costs are competitive with other renewable energy vectors when delivered in their end-use state. For hydrogen-specific applications, ammonia and liquid hydrogen offer the lowest landed cost. E-methane is cost-competitive for specific end-use cases with high downstream costs, such as decentral heating, industrial process heat for cluster 6 and central dispatchable electricity production. Large-scale e-methane production will increasingly rely on DAC to ensure stable CO2 supplies. Consequently, DAC costs will critically determine e-methane's cost-competitiveness relative to hydrogen

he study analyzes renewable energy vector competitiveness through a systematic approach, first identifying optimal transport modes per import region, then evaluating total landed costs of the vectors in their end-use state and when converted to hydrogen, and finally analyzing total value chain costs for selected end-use cases. To account for key uncertainties in the assumptions, a sensitivity analysis was conducted on key parameters affecting total value chain costs. The findings of this study are also more or less relevant to neighboring countries such as Belgium, Germany and others that share a similar reliance on natural gas and are likely to require substantial imports to meet their future renewable energy needs.

Transporting renewable energy vectors via pipelines is expected to be the most cost-competitive method for shorter distances, provided that sufficient volumes are transported. For medium to longer distances, shipping will be more cost-competitive

Long-distance transportation options depend mainly on the distance between export and import locations. Pipelines are more cost-competitive for shorter distances, while maritime shipping is more cost-competitive over medium to longer distances. Pipeline costs rise in line with distance, whereas the high initial costs of shipping (e.g. liquefaction, gasification) are offset over longer routes, with only fuel and operational expenses adding incrementally. According to model-based calculations, the tipping point<sup>25</sup> for methane transportation is around 1,500-2,000 km, while for hydrogen it is around 5,000-6,000 km, reflecting hydrogen's higher upfront costs for liquefaction or conversion (e.g. to ammonia). Liquid hydrogen is expected to have a lower upfront cost compared to other hydrogen derivatives, making it more cost-competitive for delivering hydrogen over short to medium distances. ▶ N

In practice, the tipping point is situation-specific and influenced by various factors. For example, shipping can be viable over shorter distances, as border crossings and intercontinental links can complicate pipelines and increase costs. Additionally, pipelines are typically cost-competitive only for large volumes, making shipping more attractive, particularly in the short term when volumes are lower. Conversely, if existing pipelines are already in place, the tipping point for pipeline transportation could be later than indicated.

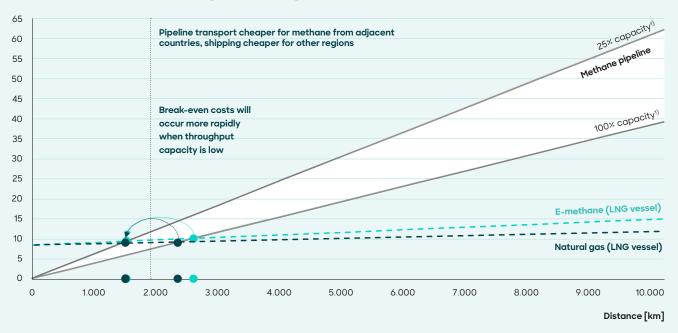
As a result, renewable energy vectors from southern Europe and northern Europe are likely to be shipped initially, with pipelines taking over in the long term, while those from MENA and the US are expected to use shipping in both the short and long term. Factoring in production and transportation, MENA and the US are anticipated to be the most cost-competitive sources of e-methane, while southern Europe likely to be the most cost-competitive for hydrogen. > 0

To mitigate risks like supply chain disruptions, political instability and feedstock limits, diversifying export regions is essential. To ensure consistency across different vectors, the remainder of this analysis will use MENA as the primary export region for renewable energy

<sup>25</sup> Shipping costs include conversion, storage, transportation and reconversion costs. Within conversion, it also accounts for the cost of the additional feedstock required compared to gaseous vector to deliver same amount of landed energy. As explained earlier, shipping costs are modeled purely on an operational cost basis without including WACC, whereas pipeline costs are tariff based and account for WACC as regulated assets. Accounting for WACC in shipping would slightly increase the tipping point

N Transporting renewable energy vectors via pipelines is more cost-competitive for shorter distances, whereas for medium to longer distances shipping becomes more cost-competitive

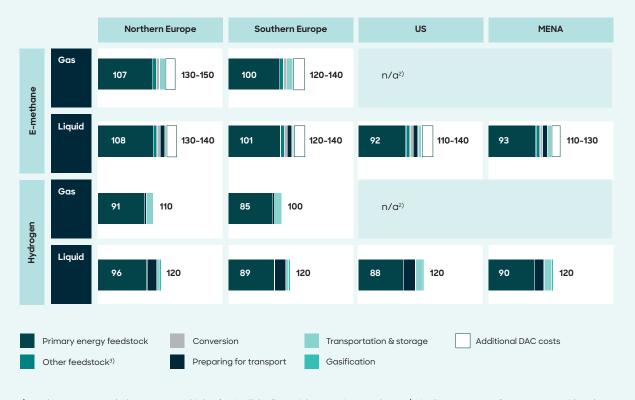
#### Projected transportation cost of methane [EUR/MWh output]



#### Projected transportation cost of hydrogen [EUR/MWh output]<sup>2)</sup>



1) Total pipeline capacity of 163 TWh for methane and 147 TWh for hydrogen; 2) Includes conversion and reconversion Source: Roland Berger comprehensive value chain model Liquid route from MENA and US is expected to be the most costcompetitive for e-methane whereas importing via pipelines from southern Europe seems to be most attractive for hydrogen [EUR/MWh output]<sup>1)</sup>



1) Total costs are rounded to nearest multiple of 10 in all the financial comparison analyses; 2) Pipeline transport of gases not considered for the US and MENA, as the distance for gas pipelines is too long and in that situation pipeline transport becomes significantly more expensive than shipping of liquids; 3) Includes CO₂ for e-methane and methanol, № for ammonia and dehydrogenated DBT for LOHC

Source: Roland Berger comprehensive value chain model

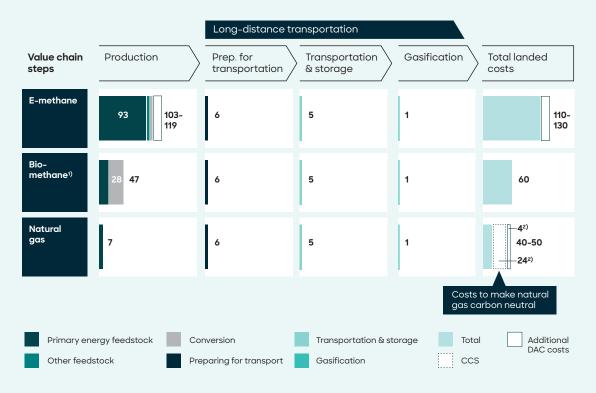
vectors, with shipping as the assumed transportation mode<sup>26</sup>. It is important to note that, for all remaining financial analyses in this chapter, costs are shown per MWh output at the last value chain step in the figure. Due to losses throughout the value chain, numbers might not correspond between figures. The different efficiencies at end-use conversion associated with different use cases also explain the varying costs per use case.

Importing e-methane will come at a premium compared to CO<sub>2</sub> compensated natural gas. Large-scale production of e-methane will increasingly need to rely on DAC to ensure stable CO2 supplies, as biogenic CO2 availability is expected to be limited in long term

Natural gas, with production costs typically well below 10 EUR/MWh, is expected to remain one of the most affordable energy vectors, also when considering the cost of capturing and

<sup>26</sup> Total costs are rounded to nearest multiple of 10 in all the financial comparison analyses. All financial analyses show costs and efficiencies with biogenic CO<sub>2</sub>. Additional DAC feedstock costs are shown separately in the production step. The overall efficiency of e-methane with DAC is about 10% lower than with biogenic CO  $_2$ 

### P Natural gas is expected to remain one of the most affordable energy vectors [EUR/MWh output]



1) Based on anaerobic digestion; 2) The combustion of 1 MWh of natural gas emits - 0.19 ton of CO<sub>2</sub> per MWh. CCS is assumed to occur at the end-use location in the Netherlands, while DAC is expected to take place at the export location in MENA. Costs to capture CO<sub>2</sub> in NL are expected to be -66 EUR/ton for point source with additional transport & storage costs of 60 EUR/ton and DAC in MENA is expected to have a cost of 106 EUR/ton for capture with additional transport & storage costs of 40 EUR/ton

Source: Roland Berger comprehensive value chain model

storing the CO2 created during combustion. P With rising demand for greener alternatives, biomethane and e-methane are emerging as viable options that utilize existing infrastructure. Biomethane is generally more cost-competitive due to lower feedstock costs, though its large-scale production is limited by feedstock availability, which competes with food production, animal feed and agriculture. Feedstock supply is also influenced by geography, seasonality and sustainability factors. In contrast, e-methane can be produced from virtually unlimited renewable sources like sun and wind, making it a scalable supplement to biomethane.

E-methane produced from biogenic  $CO_2$  has lower production costs than  $CO_2$  from DAC, but biogenic  $CO_2$  availability is also limited. By 2040, global biogenic  $CO_2$  supply is projected to be at 400-500 Mt<sup>27</sup>. Just meeting Dutch demand of 25 Mt of  $CO_2$  for e-methane in 2040 would require 6-8% of expected global biogenic  $CO_2$  supply, 12-15% of US and a staggering 150-160% of the expected MENA, illustrating the insufficiency of relying solely on biogenic sources. Therefore, while e-methane with biogenic  $CO_2$  has potential, large-scale production will increasingly need to rely on DAC to ensure stable  $CO_2$  supplies long term - the same applies to methanol.

<sup>27</sup> IEA, Zero Carbon Shipping

# Landed cost of e-methane is in line with other renewable energy vectors. Production and shipping of renewable energy vectors most cost-competitive when already in end-use state

The landed cost<sup>28</sup> of e-methane is comparable to that of other renewable energy vectors. ▶ Q When produced with biogenic CO₂, e-methane costs are comparable to methanol and ammonia. However, sourcing CO₂ from DAC increases the cost of e-methane by 20-25% compared to ammonia. Despite this increase, e-methane remains cost-competitive with other renewable energy vectors as higher production costs are offset by relatively lower long-distance transportation cost.

Shipping renewable energy vectors in their original form is more cost-competitive than synthesizing them in the Netherlands from imported hydrogen, regardless of distance and the shipping method. This advantage arises because transportation costs typically account for only 5-10% of the total landed costs and are more than offset by the higher energy prices in the Netherlands compared to the production location. For instance, synthesizing ammonia or

### Q Landed cost of e-methane is cost-competitive with other renewable energy vectors [EUR/MWh output]



 $<sup>28 \</sup>quad \text{Costs from production up to and including transportation to the import location} \\$ 

methanol in the Netherlands using imported hydrogen is 20–30% more expensive than importing the already synthesized vectors from regions like MENA. As a result, there is a possibility that production of these renewable energy vectors, such as ammonia and methanol, will shift from the Netherlands to regions where energy prices are lower, such as MENA.

### If hydrogen is the required energy vector for end-use, ammonia and liquid hydrogen are expected to offer the lowest cost levels

As some sectors like refineries specifically require hydrogen for their operations, the procurement of renewable hydrogen for end-use will be necessary in the future. Comparing the landed costs of various energy vectors for hydrogen, ammonia and liquid hydrogen are projected to have comparable costs, followed by methanol and LOHC. > R

The landed costs of ammonia and methanol are primarily driven by the production steps of each vector, with ammonia outperforming methanol due to its lower hydrogen feedstock requirements and the absence of the need for GHG-neutral CO<sub>2</sub>. In contrast, the cost of

### R If hydrogen is the end requirement, ammonia and liquid hydrogen are expected to have the lowest costs [EUR/MWh output]



Source: Roland Berger comprehensive value chain model

liquid hydrogen is predominantly influenced by long-distance transportation, including liquefaction and gasification. LOHC is relatively more expensive than ammonia and liquid hydrogen, primarily due to its lower volumetric energy density, which results in higher transportation costs per MWh. Additionally, the dehydrogenation process incurs high conversion losses and energy demands, further increasing its overall cost. Lastly, if used as a hydrogen carrier, e-methane is the least cost-competitive and energy-efficient carrier, primarily due to the costs associated with its synthesis. These high production costs, combined with its lower energy efficiency, make e-methane a less viable option if hydrogen is the required energy vector for end-use in the Netherlands.

Even with CO2 from DAC, which is likely required due to the limited long term availability of biogenic CO2, e-methane is still cost-competitive for certain use cases where downstream costs of storage, distribution, and end-use conversion make up a relatively higher share of total costs in the value chain

The comparison of the total costs includes the downstream value chain steps of transmission, seasonal storage, distribution and end-use conversion. > 5 Comparison depends on the specific end-use case. For the five selected use cases, e-methane sourced as a liquid from MENA via vessels is compared with hydrogen transported from MENA. The analysis assumes hydrogen is delivered as ammonia but acknowledges that it could also be transported as liquid hydrogen, given the comparable landed costs of the two vectors.

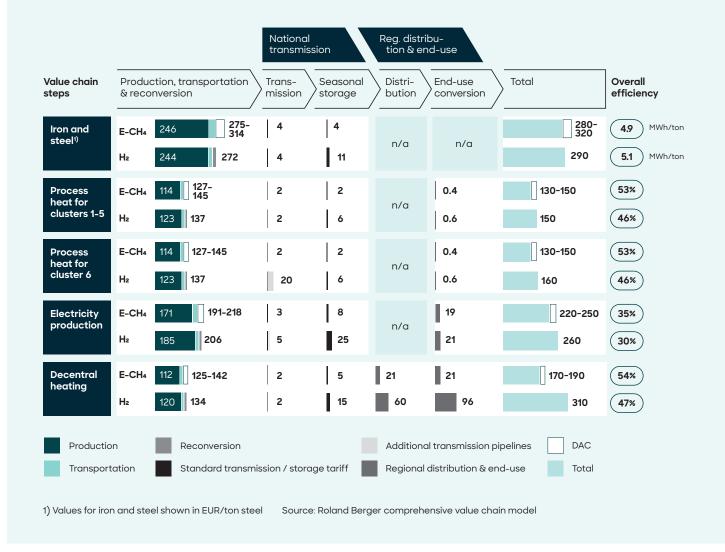
While e-methane with biogenic CO₂ is expected to be more cost-competitive than hydrogen across all shortlisted end-use cases, there are limitations. As mentioned earlier, biogenic CO2 availability is limited due to feedstock constraints. This will likely restrict the scalability of e-methane with biogenic CO₂ for large-scale applications. Although e-methane from DAC incurs higher costs compared to biogenic CO2, it still has a cost advantage over hydrogen for decentral heating, process heat for cluster 6 and central dispatchable electricity production. For process heat in clusters 1-5, e-methane with DAC is cost-comparable to hydrogen, while hydrogen remains more cost-competitive for iron and steel production.

E-methane mainly has a cost advantage over hydrogen in specific use cases with higher downstream value chain costs, as existing infrastructure can be leveraged, reducing associated expenses. For example, decentral heating with hydrogen would require adapting 80% of the existing distribution network (equivalent to 100,000 km<sup>29</sup>) and upgrading 2.5 m boilers<sup>30</sup>, resulting in significant additional costs compared to e-methane, which can use the existing infrastructure. Seasonal storage costs for hydrogen are three times higher than for e-methane, primarily due to e-methane's three times higher volumetric energy density, which reduces storage costs for decentral heating and central dispatchable electricity production. In process heat for cluster 6, the hydrogen route would require an additional

<sup>29</sup> Netbeheer Nederland indicates 136,000 km of gas network in the Netherlands, 11,000 km of which is for transmission, according to Gasunie. The remaining 125,000 km is distribution network and 80% of 125,000 km results in 100 000 km of distribution network remaining

<sup>30</sup> Based on II3050, considering the International Trading (INT) scenario

S E-methane as an end-product with biogenic CO₂ is cost-competitive with hydrogen for all use cases, whereas with DAC it is cost-competitive in cluster 6, electricity production and decentral heating due to the lower infrastructure costs for e-methane [EUR/MWh output]



400 km of dedicated pipeline<sup>31</sup>, adding 18 EUR/MWh in transmission costs. E-methane, however, can utilize the existing transmission network without additional costs for new pipelines to connect to certain end-users.

The current analysis focuses on e-methane synthesized at the export location and transported to the Netherlands. Alternative routes include capturing CO<sub>2</sub> at the combustion site and returning it to the export location or capturing CO<sub>2</sub> at the end-use site and storing it

<sup>31</sup> HyRegions: Approach for the possible roll-out of regional hydrogen infrastructure

in the Netherlands. Both alternatives are cost-comparable, but the latter may offer cost advantages when carbon deposit removal fees exceed 180-200 EUR/ton<sup>32</sup>.

In the broader context of low-carbon energy vectors, fossil vectors with CCS are generally expected to be more cost-competitive than renewable energy vectors if they run at high utilization rates. When comparing different fossil vectors with CCS, natural gas combined with CCS is expected to be more cost-competitive than blue hydrogen, because it is cheaper to transport natural gas and CO2 than to transport hydrogen. Consequently, even when considering low-carbon alternatives, hydrogen pathways remain less cost-competitive than low-carbon/renewable methane-based vectors, solidifying methane's role as a less costly option for selected use cases.

Since e-methane is expected to be more cost-competitive in certain use cases, it could reduce the total future demand for renewable hydrogen in the Netherlands, particularly in applications like decentral heating, process heat and central dispatchable electricity production. This reduction in the Dutch demand for hydrogen would in turn lead to higher transmission and distribution tariffs, as the infrastructure costs would need to be distributed across a smaller user volume. However, in practice, reduced hydrogen demand within the Netherlands could be offset by increased export capacity to neighboring regions like Germany, potentially minimizing the impact on tariffs.

### The costs of DAC play a key role in determining the degree of cost-competitiveness of e-methane with respect to hydrogen

All renewable energy vectors in this study face uncertainties, including the costs for renewable hydrogen, prices for electricity and captured carbon, technology maturity and demand-related tariffs. A sensitivity analysis was conducted on key parameters affecting total value chain costs, such as hydrogen costs, DAC prices, electricity prices and transmission tariffs. Sensitivity on transmission tariffs reflects the uncertainty in the demand of e-methane and hydrogen. If the demand reduces by half, the tariffs will increase by factor of two (assuming pipelines are primarily used for domestic demand). > T

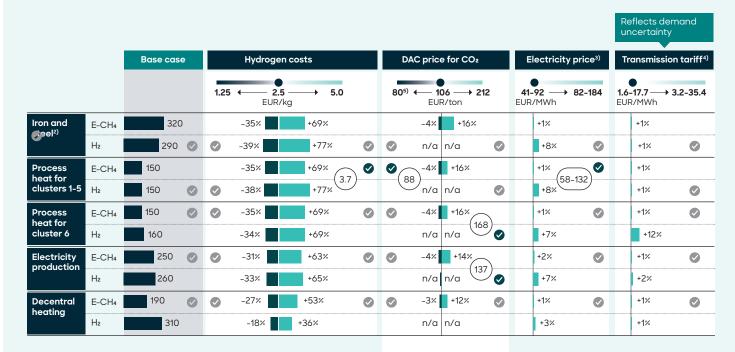
Although uncertainty in renewable hydrogen costs significantly impacts total costs, it does not affect e-methane's cost-competitiveness in most cases, as the hydrogen costs make up over 55% of production costs of all of the renewable energy vectors. Uncertainty in DAC price has the biggest impact on cost-competitiveness; as DAC price doubles, hydrogen becomes more costcompetitive in all cases except decentral heating, where e-methane remains more costcompetitive due to high hydrogen-related costs at later stages of the value chain. Initially, e-methane can use the more cost-competitive biogenic CO2, but as demand grows, the CO2 from DAC will become a crucial feedstock, making DAC pricing a key factor in e-methane's long-term cost-competitiveness. With DAC still at a lower technological maturity level (TRL 6),

<sup>32</sup> Alternative routes for electricity production and process heat in clusters 1-5 have been analyzed. For electricity production, it is assumed that the carbon capture unit increases the CAPEX and OPEX of the electricity plant by 75%. For process heat in clusters 1-5, the CAPEX for the carbon capture facility is assumed to be 250 EUR per ton of CO₂ captured, with an OPEX rate of 4%. Shipping costs are estimated at 40 EUR per ton of CO2, while transportation and storage costs are estimated at 60 EUR per ton

its scalability and cost trajectory remain uncertain, underscoring the importance of investments in its technology to ensure e-methane's future cost-competitiveness.

The current analysis focuses on energy demand based on the INT scenario outlined in the II3050 report. When other scenarios are considered, the total demand for renewable energy vectors changes, which primarily influences transmission tariffs. However, these changes in transmission tariffs do not affect the relative cost-competitiveness of the energy vectors. Even when transmission tariffs are doubled, the conclusions regarding the comparison between e-methane and hydrogen remain unchanged. This suggests that selecting a different II3050 scenario with varying energy demand would not significantly affect the conclusions on the cost-competitiveness of renewable energy vectors.

Cost of hydrogen has the highest impact on the total costs of energy vectors but has less effect on their competitiveness compared to the significant influence of DAC price on cost-competitiveness [EUR/MWh output]<sup>1)</sup>



Most cost-competitive option, both in base case and with changed parameter

1) Considering import of liquid e-methane with DAC and ammonia (to hydrogen) via shipping from MENA, 2040 forecast; 2) Values for iron and steel shown in EUR/ton steel; 3) 41 EUR/MWh in MENA and 92 EUR/MWh in the Netherlands; 4) Depending on energy vector and use case. If multiple tariffs were considered, which is the case for the additional pipelines for cluster 6 and central dispatched electricity production, all tariffs were multiplied by 2 for the sensitivity analysis; 5) Theoretical minimum of DAC costs

Source: Roland Berger comprehensive value chain model

Most cost-competitive option, **not** in base case but only with changed parameter

Break-even price/costs xx

# Comparing e-methane with other energy vectors on criteria beyond cost

Given the capital-intensive nature of the energy transition, the adoption of e-methane allows for the reuse of existing infrastructure, conserving financial and human resources while minimizing delays. With lower upfront costs, e-methane enhances societal value and enables a more resource-efficient energy transition. Its viability is further bolstered by its positive emissions impact, safety advantages and efficiency in land use and logistics



n addition to the landed and total costs of energy vectors discussed in Chapter 5, this study also compares energy vectors across other key parameters, such as infrastructure needs and costs, emissions and safety to evaluate their long-term feasibility. Infrastructure costs and technology readiness levels are key to determine how to meet GHG targets sooner rather than later, influencing timelines and investment needs. Assessing GHG emissions across the value chain and the cost per ton of CO2 saved identifies the most cost-competitive decarbonization pathways. Safety and land-use analyses highlight feasibility, costs and compliance requirements of the energy vectors.

### In the Netherlands, for the selected use cases, the hydrogen route will require an additional EUR 63 billion in CAPEX compared to the e-methane route

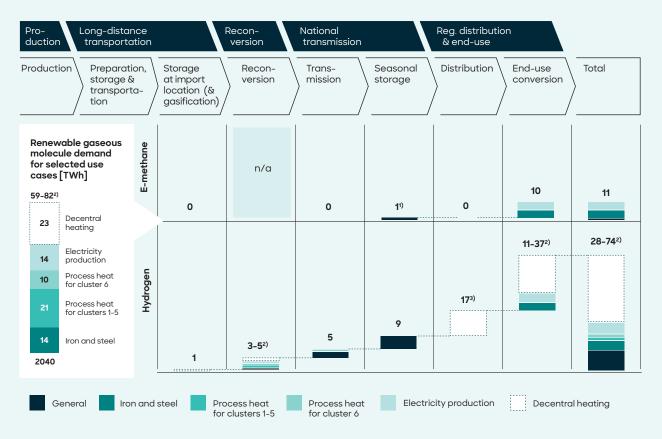
The total CAPEX investment required in the Netherlands to meet renewable energy vector consumption shows that hydrogen consumption costs are estimated at EUR 74 billion across the five selected use cases - significantly higher than the EUR 11 billion needed for e-methane (imported in liquid form). ▶ U This cost disparity largely stems from the Netherlands' existing methane infrastructure, which spans the entire value chain from storage at import terminals to end-use conversion, whereas hydrogen infrastructure would need to be built almost entirely from scratch, except for the share of existing pipelines that can be repurposed for hydrogen. In regions with a less developed methane infrastructure, this cost disparity will likely be less pronounced.

For the use of hydrogen, decentral heating accounts for a substantial portion of CAPEX, totaling EUR 45 billion. Due to e-methane's significant cost advantage and the option to use biomethane and hybrid heat pumps, decentral heating is unlikely to transition to hydrogen. Excluding decentral heating from hydrogen's investment needs reduces total hydrogen CAPEX to EUR 28 billion, still almost triple the EUR 11 billion needed for e-methane.

In the remaining four use cases, most additional costs for hydrogen arise from seasonal storage, transmission and reconversion. For example, in seasonal storage, e-methane would require EUR1 billion to expand flexible storage in salt caverns<sup>33</sup>, increasing the current capacity of 3.6 TWh to 11 TWh. In contrast, hydrogen would require EUR 4 billion to adapt existing salt caverns and develop new hydrogen storage capacity. Also developing new hydrogen storage capacity for longer periods in depleted gas fields would cost EUR 5 billion, leading to a total investment cost of EUR 9 billion. The large difference in required investments is not only due to the fact that much of the methane storage infrastructure is already in place. Also, less TWh of hydrogen can be stored in a salt cavern than methane, as the volumetric energy density of hydrogen is only one-third that of methane. Therefore, relatively more salt caverns are required for hydrogen storage, increasing the hydrogen costs per MWh for seasonal storage.

<sup>33</sup> While there is currently sufficient methane storage capacity in depleted gas fields (136 TWh), this type of storage is mainly suitable for long-term storage. It is expected that in the future, more short-term storage capacity is required, for which salt caverns would be more suitable; there is currently only 3.6 TWh capacity compared to the 11 TWh capacity expected to be required

### U CAPEX intensity of meeting hydrogen demand in the Netherlands is three times higher than that of e-methane, even when excluding decentral heating costs [EUR bn]



<sup>1)</sup> Additional methane storage required specifically for salt caverns for higher flexibility; 2) Low end of the range shows total required CAPEX without decentral heating; 3) Distribution only required for decentral heating

Source: Roland Berger comprehensive value chain model

A recent study by the Dutch Ministry of Economic Affairs indicated that by 2050, up to 60 salt caverns will be required to accommodate the storage needs for hydrogen<sup>34</sup>.

### E-methane adoption enhances societal value, enabling a more resource-efficient energy transition

Given the capital-intensive nature of the energy transition, exploring alternatives that reduce the societal burden with lower upfront costs is crucial. The adoption of e-methane allows us to reuse existing infrastructure, conserving both financial and human resources and minimizing the risk of delay. In addition, e-methane can also serve as a transition energy vector in other use-cases by using it as a drop-in for natural gas. This facilitates the transition

<sup>34</sup> Risk assessment for Underground Hydrogen Storage (UHS) in Salt Caverns and Interaction with other Underground Storage Locations, KEM, 2023

to renewable energy vectors through longer use of the existing natural gas infrastructure throughout the entire value chain. This efficient use of resources and infrastructure amplifies e-methane's societal value, freeing capital and attention for other critical strategic priorities.

### Majority of the renewable energy vectors considered in the study are expected to achieve full commercial readiness by 2040

TRL scores indicate the development stage of a technology, from research and development (TRL 1-3) to full commercial deployment (TRL 11). Understanding these scores is needed for assessing when different energy vectors can be widely adopted. The technological maturity of different energy vectors varies by value chain step. > V Renewable methane vectors are generally more mature than hydrogen vectors as they can leverage fully commercially mature existing gas infrastructure, apart from the production step, which has yet to achieve commercial maturity. For hydrogen, the ammonia vector is the most technologically mature, primarily due to the well-established infrastructure for ammonia synthesis, storage and transportation at scale. However, all renewable energy vectors face technological uncertainties and lower maturity in different parts of their value chains. E-methane, for example, still requires further development in areas like DAC and conversion processes. Similarly, further advances in ammonia cracking technology will be required to mature the ammonia route. Despite these technological uncertainties, all renewable energy carriers currently operate at a TRL level above the prototype stage (TRL 4) and for the purpose of this study are assumed to reach commercial technological readiness by 2040.

### E-methane and renewable hydrogen have comparable GHG emission intensities

E-methane and renewable hydrogen have similar landed GHG emission intensities<sup>35,36</sup>, ranging from 20 to 80 kg CO₂e/MWh, but the sources of these emissions vary. Emissions from methane-based vectors are both scope 1 and scope 2, where scope 1 emissions are due to methane and hydrogen slips, and emissions from hydrogen vectors are largely scope 2, influenced by grid CO2 intensity. As the vectors are net-zero, scope 1 CO2 emissions are not considered. Across both vectors, the production stage is the primary source of emissions, with minimal impact from transportation (except for liquid and gaseous hydrogen, where energy-intensive liquefaction and hydrogen leakage in pipeline transportation, based on current insights, significantly contribute to transportation emissions). > W

Emissions for e-methane and methanol rise when CO2 is sourced from DAC due to the energy intensity of the process. Similarly, ammonia emissions are driven by its energy-intensive synthesis. As a result, all three vectors have higher scope 2 CO2 emissions as the grid

<sup>35</sup> Emissions are converted to CO<sub>2</sub> equivalent using the 100-year Global Warming Potential (GWP<sub>100</sub>); methane is assumed to have a GWP100 of 27, hydrogen of 11.6, N2O of 273 and NOx of 8.5

<sup>36</sup> In all emissions analyses in this chapter emissions are shown per MWh output at the last value chain step shown in the figure. Due to losses throughout the value chain, numbers might therefore not correspond between figures. Some  $value\ chain\ steps\ are\ relatively\ small\ compared\ to\ other\ steps,\ making\ them\ difficult\ to\ visualize\ in\ a\ graph.\ All\ emissions$ analyses show emissions with biogenic CO<sub>2</sub>. Additional DAC feedstock emissions are shown separately in the production step and in the final totals

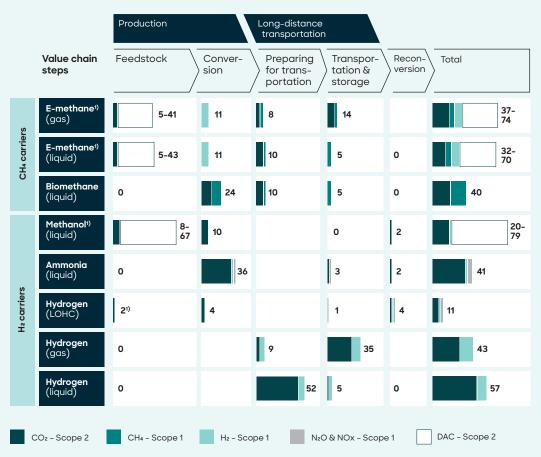
# Renewable methane vectors have relatively higher technology maturity level compared to hydrogen vectors<sup>1)</sup> >

	Production			Long-distance transportation	ansportation				Recon- version	National transmission		Reg. distribution & end-use	
Value chain steps	Production	Other feed-	Conversion	Preparing for transporta-tion	Storage at production location	Transporta-	Storage at import location	Gasification	Reconversion	Transmission	Seasonal	Distribution	End-use conversion
Natural gas (liquid)	Extraction:			Liquefaction: 11	Storage at production:	Shipping:	Storage at import:	Re- gasification:	Conversion to Hz:	National gas grid (HTL & RTL):	Seasonal storage	Local gas grid: <b>11</b>	Iron and steel:
E-methane (gas)	Electrolysis:	Carbon capture:	Methanation: 7	Compression:		Pipeline:							
E-methane (liquid)				Liquefaction:	Storage at production:	Shipping:	Storage at import:	Re- gasification: <b>11</b>					Process heat, electricity
<b>Biomethane</b> (liquid)	Bio feestock		Methanation: 10-11										production, Decentral heating: <b>11</b>
Methanol (liquid)	Electrolysis:	Carbon capture:	Methanol synthesis:		Storage at production:	Shipping:	Storage at import:		Conversion to Hz:	Local H <sub>2</sub> grid: new	Seasonal storage: 4-10	Local H <sub>2</sub> grid: new	Iron and steel:
Ammonia (liquid)		Nitrogen	Haber-Bosch:		Storage at production:	Shipping:	Storage at import:		Conversion to H <sub>2</sub> :	refurbished 8	gas field storage: 4 Salt cavern	refurbished 8	heat, heat, electricity production:
Hydrogen (LOHC)		DBT	Hydrogena- tion:		Storage at production:	Shipping:	Storage at import:		De-hydro- genation: <b>6-7</b>		9-10 We assume NL will		Decentral heating:
Hydrogen (gas)				Compression: 6		Pipeline: new 9, refurbished 8					make use of both storage types		
<b>Hydrogen</b> (liquid)				Liquefaction:	Storage at production:	Shipping: 7	Storage at import:	Re- gasification: <b>8</b> 4)					
TRL unknown	wn TRL 1-6		TRL 7-8	TRL 9-10	TRL 11								

1) The TRL at each value chain step only corresponds to the maturity of the main technology and not to the associated technologies of that value chain step, 2) DAC TRL of 6, point-source capture TRL of 11 (point-source TRL: EU technology report, 2019); 3) According to HydroHub HyChain, 2019; 4) According to RENA; 5) According to Sterner et al, 2019; 6) Shipping TRL refers to tanker transporting relevant renewable energy vector

Source: IEA, IRENA, Desk research

### W Renewable methane and hydrogen vectors have comparable landed emissions [kg CO2e/MWh output]



<sup>1)</sup> CO<sub>2</sub> for e-methane and methanol synthesis is assumed to be captured as biogenic byproduct in the base case 2) LOHC feedstock emissions are scope 1 instead of scope 2

Source: Roland Berger comprehensive value chain model

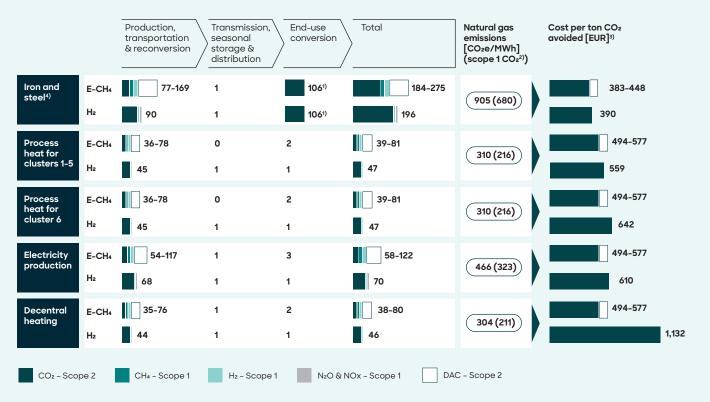
emissions intensity is assumed to be relatively higher in MENA compared to regions such as southern Europe. However, most of these projects are expected to use captive renewable electricity setups in the future, significantly reducing scope 2 emissions and leading to lower overall landed emissions.

## For renewable energy vectors to become economically viable, the EU's Emissions Trading System price must exceed EUR 400 per ton CO<sub>2</sub>

The total emissions of e-methane and hydrogen delivered via ammonia range from approximately 40 to 120 kg CO₂e/MWh across most use cases, except for iron and steel. ➤ X This represents a more than 70% reduction in GHG emissions for most use cases compared to fossil comparators, meeting the RFNBO requirements³7 even when assuming production in

<sup>37</sup> The RED II defines a GHG emission reduction for RFNBOs of 70% below a fossil fuel comparator of 94 gCO $_2$ eq/MJ, i.e. no more than 28.2 gCO $_2$ eq/MJ (equivalent to 102 gCO $_2$ e/kWh H $_2$ )

### The cost per ton CO2 avoided is higher than EUR 400 for both X e-methane and hydrogen [kg CO2e/MWh output]



1) Emissions due to coal component needed for steel production - These emissions are scope 1 instead of scope 2; 2) Refers to scope 1 CO2 emissions at enduse conversion per MWh of output, 3) Only includes scope 1 CO2 emissions at end-use conversion, 4) Values for Iron and steel shown in kg CO2e/ton steel

Source: Roland Berger comprehensive value chain model

MENA and grid electricity use for processes post-hydrogen production. For iron and steel, emissions range from 200 to 300 kg COze/MWh. However, these emissions include coal emissions, which are excluded from RFNBO requirements, ensuring that the iron and steel use case also meets compliance. While future RFNBO thresholds are expected to become stricter, the anticipated adoption of captive renewable electricity setups will significantly reduce scope 2 emissions, ensuring the continued compliance of e-methane and hydrogen vectors.

The emissions are comparable across use cases due to the limited impact of the downstream value chain steps on the GHG emissions. In large part this is because grid intensity is expected to be lower in the Netherlands by 2040, and leakage plays a smaller role in the downstream steps.

The cost per ton of CO<sub>2</sub> avoided<sup>38</sup> is also comparable for e-methane and renewable hydrogen, except in decentral heating, where the avoidance cost for hydrogen is two times that of e-methane due to the higher cost of energy delivered (the higher cost for decentral heating is primarily driven by the higher cost of energy, as discussed in Chapter 5.) The higher

<sup>38</sup> Calculated by dividing the cost difference compared to natural gas by the difference in scope 1 CO₂ emissions during end-use conversion relative to natural gas

avoidance cost implies that the EU's Emissions Trading System (ETS) price would need to be in the EUR 400-600 range to make the business case for renewable vectors competitive.

### Of the renewable energy vectors, e-methane is intrinsically a relatively safer vector

The safety characteristics of an energy vector can be determined based on its chemical properties like flammability, explosiveness and toxicity. (E)-methane scores relatively well on these metrics, with a relatively high auto-ignition temperature, narrow explosive range and low toxicity. > Y

In contrast, hydrogen and methanol both present a significantly larger explosiveness bandwidth, which is measured by the explosive range between the lower explosive limit (LEL) and upper explosive limit (UEL), defining the concentrations at which ignition can occur. The explosive ranges are approximately seven and five times wider than (e)-methane, for hydrogen and methanol respectively, making them highly flammable across various airfuel mixtures. However, it is important to note that hydrogen is much lighter than air, which makes it disperse more rapidly than other molecules. In addition, due to hydrogen's small size, it can escape more easily from indoor environments. Therefore, additional empirical evidence is required to better estimate the risk of hydrogen explosions in practice.

Ammonia has a higher toxicity, as indicated by its low life-threatening limit (Levensbedreigende waarde or LBW) and Acute Exposure Guideline Level (AEGL) scores, meaning

Higher explosiveness risk of hydrogen and methanol, coupled with the greater toxicity of ammonia, makes (e)-methane in terms of measures a comparatively safer renewable energy vector

	General		Flam	mability	Explos	iveness	Toxic	sity		
	Appearance	Odor	Flash point [°C]	Auto- ignition temp. [°C]	LEL [%(V)]	UEL [%(V)]	AEGL 1[mg/ m3]	AEGL 2 [mg/ m3]	AEGL 3 [mg/ m3]	LBW1) [mg/ m3]
(E-) Methane	Colorless gas	Odorless	< -56	670	4.4	17	n/a	n/a	n/a	n/a
Methanol	Colorless liquid	Alcohol-like	9.7	455	5.5	44	690	2,800	9,400	15,000
Ammonia	Colorless	Ammonia- like	n/a	651	16	27	21	112	769	780
Hydrogen	Colorless gas	Odorless	n/a	560	4	77	n/a	n/a	n/a	3,300

1) At exposure of 1 hour

Source: Safety data sheets

even minor leaks can pose serious risks. These properties underscore the importance of stringent safety measures for hydrogen, methanol and ammonia handling.

### Based on current safety guidelines, hydrogen infrastructure will potentially require additional safety measures compared to (e)-methane

The potential need for additional risk mitigation measures for infrastructure varies across the value chain and depends on legal risk thresholds. Risk is determined by the probability of an adverse event and its potential impact. While these factors are well-established for (e)-methane, limited empirical evidence for hydrogen makes them harder to define. Current regulations adopt a cautious approach with conservative assumptions, potentially leading to additional measures for hydrogen to achieve comparable risk levels to (e)-methane. However, as more data becomes available and understanding improves, regulations may evolve, potentially reducing these requirements.

For instance, a risk that is often considered for handling chemical substances is the sitespecific risk (plaatsgebonden risico), defined as the distance from the risk source at which the annual fatality risk is less than one in a million. In case of transportation via pipeline, the site-specific risk is based on the probability of pipeline failure, the probability that after a pipeline failure the released substance will ignite<sup>39</sup> and the impact when the released substance would ignite. While the impact and failure probability are probably comparable for (e)-methane and hydrogen, ignition probabilities differ significantly.

(E)-methane's ignition probability after pipeline failure ranges from 20-80%, depending on pipeline diameter, based on decades of experience. > Z However, with limited data on hydrogen, the RIVM advises assuming a 100% ignition probability for now. This assumption necessitates additional safety measures for hydrogen pipelines if constructed now, to maintain equivalent site-specific risk levels to methane. Measures like increased supervision of digging activities or protective pipeline coverings can mitigate the higher assumed ignition probability. These measures are particularly relevant for smaller pipelines (less than 24-inch diameter) used for last-mile connections, where the ignition probability gap between hydrogen and (e)-methane is more pronounced.

### E-methane offers a more land-efficient and logistically manageable alternative to hydrogen

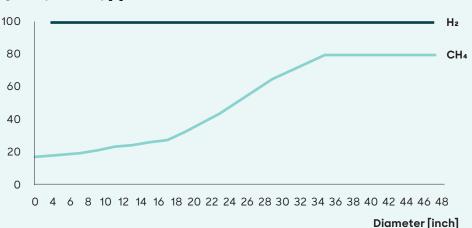
When comparing the land-use requirements of e-methane and hydrogen in the Netherlands,<sup>40</sup> for an equivalent annual energy flow of 100 TWh, e-methane is expected to be notably more land-efficient compared to hydrogen. Within the Netherlands, e-methane

<sup>39</sup> Refers to the probability of ignition over a timeframe of 20 to 140 seconds. An equivalent energy amount escaping from a rupture for both hydrogen and methane is assumed

<sup>40</sup> This analysis only considers land-use requirements inside the Netherlands. When comparing land-use requirements at the location of production, most of the land is required for renewable electricity generation. When assuming all renewable electricity comes from utility-scale solar PV panels, 100 TWh of hydrogen in the Netherlands  $would\,require\,1,400\,km^2\,of\,land\,in\,the\,production\,region,\,compared\,to\,1,600\,km^2\,for\,e-methane\,1,600\,km^2\,for\,e-methan$ 

### Based on current RIVM guidelines, hydrogen has a higher probability Z of ignition after a pipeline rupture than methane, especially for smaller pipelines





Source: RIVM

requires only one-third of the total land use (47 km² vs. 128 km²)41, covering areas needed for storage at import, seasonal storage, reconversion and end-use conversion. The most substantial land-use difference arises from seasonal storage, where e-methane needs 40 km² compared to hydrogen's 120 km² due to hydrogen's lower volumetric density. Although land requirements for storage at import and reconversion are also lower for e-methane (0.3 km² vs. 1.35 km²)<sup>41</sup>, this difference is relatively minor.

In addition, e-methane demands fewer shipping resources. For a 100 TWh annual flow e-methane would require one LNG shipment (transporting an average of 1 TWh per ship) every 3-4 days, while hydrogen (assuming it is shipped via ammonia) would need almost daily shipments, each averaging 0.25 TWh. This increases the logistical intensity for hydrogen. Taken together, these factors make e-methane a more viable option for minimizing land and transportation demands associated with renewable energy use in the Netherlands.

<sup>41</sup> Based on publicly available data from Gate Terminal and Port of Rotterdam, along with additional desk research and interviews with industry experts. Estimates for reconversion of hydrogen are based on land use reported by Port of Rotterdam for ammonia cracking

# Conclusions & recommendations

E-methane is a feasible and promising renewable energy vector for specific use cases with high downstream costs in the future energy mix of the Netherlands, but its full potential can only be realized with advancement and cost reduction of technologies for renewable hydrogen production, e-methane synthesis and direct air capture



s the Netherlands and the broader EU work towards achieving climate neutrality by 2050, e-methane presents itself as a promising and practical energy vector within the renewable energy landscape when also considering the downstream part of the value chain, including transmission, storage, distribution and end-use. The analysis shows that e-methane not only aligns with the Netherlands' climate goals by facilitating the transition from fossil fuels to renewable energy, but also provides several key advantages for specific use cases in terms of cost, emissions, land use and safety. Synthesized from renewable hydrogen and CO<sub>2</sub>, e-methane offers the Netherlands an additional feasible and potential option, next to other renewable energy vectors, to achieve net-zero carbon emissions by 2050 in hard-to-electrify use cases, and it does this while supporting decarbonization targets and minimizing the need for extensive new infrastructure.

One of the key benefits of e-methane is its compatibility with existing natural gas infrastructure. As a drop-in replacement for methane, it can make use of the extensive transport, storage and conversion infrastructure that is already in place. This reduces capital expenditures required to scale renewable energy adoption. This infrastructure advantage makes e-methane a particularly cost-competitive renewable energy vector for sectors with high downstream costs, such as decentral heating, industrial process heat for cluster 6 and central dispatchable electricity production. Additionally, certain industrial processes that will require a non-fossil carbon source can benefit from e-methane, as it contains carbon atoms - an advantage over hydrogen or ammonia. In the Netherlands and other similar regions with well-established natural gas networks, e-methane (combined with biomethane) can be deployed rapidly and at a lower cost for certain sectors, placing a much smaller financial and logistical burden on citizens compared to renewable hydrogen.

E-methane's cost-competitiveness in certain use cases is further bolstered by its emissions profile, safety characteristics and efficiency in land use and logistics. The GHG footprint of e-methane is comparable to that of renewable hydrogen vectors, making it a sustainable option for the energy transition. In terms of safety, e-methane is less hazardous than hydrogen and its derivatives and benefits from established safety protocols, whereas hydrogen infrastructure may require additional measures based on current regulations, which are informed by limited operational experience, to achieve comparable risk levels. Additionally, e-methane is more resource-efficient, with significantly lower land and logistical demands than hydrogen. This advantage could be crucial for large-scale deployment, especially in densely populated areas or areas with limited available land. These attributes collectively highlight the societal value of e-methane by reducing the financial burden on society, supporting sustainability goals and enabling a more inclusive transition to renewable energy.

Initially, e-methane could be produced using biogenic COz; however, due to feedstock limitations, large-scale adoption will rely on DAC for CO2 sourcing. While DAC holds promise, uncertainties around its costs present challenges for e-methane's cost-competitiveness in the long term. Sensitivity analyses show that fluctuations in DAC costs could affect the cost of e-methane, making it essential to address these uncertainties through technological advancements and regulatory support. As DAC technology matures, it will be crucial for unlocking e-methane's potential as a large-scale, cost-competitive additional renewable energy vector.

Ultimately, e-methane is a promising renewable energy vector for specific use cases in the Netherlands and other similar regions, where established natural gas infrastructure can be leveraged for renewable energy distribution. Its efficiency in terms of capital and operational costs, emissions, safety, land use and transportation makes it a viable vector in the renewable energy mix. E-methane can play a role in decarbonizing cluster 6, decentral heating and central dispatchable electricity production - sectors where hydrogen adoption seems to face significant challenges.

However, to realize the full potential of e-methane, several key steps should be focused upon:

### Strategic decarbonization planning

Develop specific end-use case strategies that evaluate the true costs of achieving net-zero emissions across the entire value chain van put tot pit. Recognize e-methane as a feasible and potential energy vector and integrate it into future energy mix evaluation alongside other renewable vectors.

### **Technological maturity**

Invest in R&D and pilot/demonstration projects to validate and commercialize e-methane production processes. Demonstration projects can be initiated globally to provide proof of concept and establish scalability and efficiency.

### Kickstarting e-methane with biogenic CO2

Identify locations (e.g. northern Europe) with high biogenic CO₂ availability to kickstart e-methane production and import.

### Cost reductions for renewable hydrogen

Support initiatives to lower the production costs of renewable hydrogen through innovation in electrolysis technologies, economies of scale and renewable energy price reductions.

### Scaling DAC solutions for e-methane production

Accelerate technological advancements to lower the costs of DAC and ensure economic viability. DAC is critical for scaling up e-methane, especially where biogenic feedstocks are constrained.

### Utilizing CCS solutions to realize negative emissions

Utilizing CCS for high-emission, high-utilization end-use cases powered by e-methane offers the potential to achieve negative emissions. This option should be considered in the overall weighting of the transition paths of end-uses and associated carriers.

### Leveraging existing gas infrastructure

 $\label{lem:continuous} \mbox{Update and align plans for the existing gas infrastructure to ensure readiness to}$ support e-methane, since e-methane can leverage existing gas infrastructure and thus reduce the need for significant downstream infrastructure investments. To enable this transition, adequate pipeline capacity must be ensured for e-methane, alongside sufficient infrastructure for other molecules in the future energy mix.

### Blending-in biomethane and e-methane

Implement blending mandates for biomethane and e-methane into natural gas supplies, especially for fragmented CO₂ emission use cases like decentral heating and transport to drive initial market demand.

### Prioritizing optimal end-use cases

Identify and prioritize the most viable end-use cases for e-methane where it offers the highest cost-competitiveness and impact, such as industrial process heat for cluster 6, dispatchable electricity production and decentral heating.

### Supportive policy and regulatory frameworks

Standardize cross-border CO<sub>2</sub> certification to facilitate trade and align regulatory frameworks. Implement supportive policies to attract investment in e-methane and other renewable energy vectors.

### **Public awareness**

Raise public awareness about the role of renewable gases like e-methane in achieving climate goals to secure societal support for its development and use.

### Definition of key terms and abbreviations

### **Definition of key terms**

GHG-neutral CO2: Refers to CO2 obtained through DAC or from biogenic sources. CO2 sourced from fossil sources is excluded

Hydrogen carriers: Molecules containing hydrogen atoms that can facilitate the transportation of hydrogen. Examples include LOHC, methanol and ammonia

Low-carbon energy vectors: Refers to molecules derived from non-renewable sources that meet a GHG emissions reduction threshold of 70% compared to fossil natural gas across the full lifecycle as defined by the EU

Methane carriers: Methane energy vector produced from different sources. Examples include e-methane, biomethane and natural gas

Renewable electricity: Refers to electricity generated from wind, solar (both solar thermal and solar PV), geothermal energy, ambient energy, tide, wave and other ocean energy, hydropower, biomass, landfill gas, sewage treatment plant gas, biogas and nuclear systems. Although nuclear energy is not classified as renewable in the EU, its carbon emissions are very low. Nuclear can thus be used for production of renewable energy vectors if the average emission intensity of the electricity grid is <18 g CO<sub>2</sub>e/MJ

Renewable energy vectors: Refers to molecules from organic sources, such as biogas and biomethane, or non-biological renewable sources using electricity (which is at least 90% renewable), such as renewable hydrogen and derivatives like e-methane, renewable ammonia and renewable methanol as defined by the EU

Renewable gaseous molecules: Renewable methane and hydrogen, including green hydrogen, e-methane and biomethane

### **Abbreviations**

ACCI. Acuto Evincoura Cuidelina INT computer International Tradici	
AEGL: Acute Exposure Guideline INT scenario: International Trading	_
Level scenario (one of the	113050
AEGL 1: Mild, reversible effects report scenarios)	
(discomfort) ISO: International Organi	zation
AEGL 2: Serious but non-life- for Standardization	
threatening effects <b>kg:</b> Kilogram	
(disability) LBW: Life-Threatening Val	
AEGL 3: Disability potentially causing (Levensbedreigende	Э
death Waarde)	
CAPEX: Capital expenditure LEL: Lower explosive limit	t
CH4: Methane LNG: Liquid natural gas	
CH <sub>3</sub> OH: Methanol LOHC: Liquid organic hydro	gen
CO2: Carbon dioxide carrier	
CO2e: Carbon dioxide equivalent MENA: Middle East and North	th
CCS: Carbon capture and Africa	
storage <b>MW:</b> Megawatt	
DAC: Direct air capture MWh: Megawatt hour	
<b>DEC scenario:</b> Decentral Initiatives N₂: Nitrogen	
scenario (one of the 113050 <b>n/a:</b> Not applicable	
report scenarios) NAT scenario: National Leadership	
ETS: Emissions Trading System scenario (one of the	113050
from the EU report scenarios)	
EU: European Union NH3: Ammonia	
<b>EUR scenario</b> : European Integration <b>NL:</b> The Netherlands	
scenario (one of the 113050 O2: Oxygen	
report scenarios) OPEX: Operational expend	iture
GHG: Greenhouse gas PEM: Proton-exchange	
GW: Gigawatt membrane	
GWh: Gigawatt hour PVs: Photovoltaics	
H2: Hydrogen R&D: Research & develope	ment
H₂O: BU Renewable Energy	ЭY
HTL: Main transmission pipelines Directive	
(hoofdtransportleidingnet) <b>RFNBO</b> : Renewable fuel of no	on-
IA scenario: International Ambition biological origin	
Scenario (one of the EU RTL: Regional transmission	on
scenarios - used for 2030 in pipelines (regionale	
the II3050 in the report, transportleidingnet)	
most similar to the II3050 <b>SOEC:</b> Solid oxide electroly.	zer cell
INT scenario) TRL: Technology readines	ss level
IEA: International Energy Agency TW: Terawatt	
II3050: Integrale TWh: Terawatt hour	
Infrastructuurverkenning <b>UEL:</b> Upper explosive limit	t
2030-2050 (Dutch) or US: United States	
Integrated Infrastructure WACC: Weighted average c	ost of
Outlook 2030-2050 (English) capital	

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We are grateful for the contributions from numerous experts from GasTerra, Gasunie and the broader energy sector.

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# Feasibility and potential of e-methane in the future energy mix

Appendix

April 2025

### **Contents**

This document serves as an appendix to the main report Feasibility and potential of e-methane in the future energy mix. The document details all the assumptions made and additional analysis carried out during the study

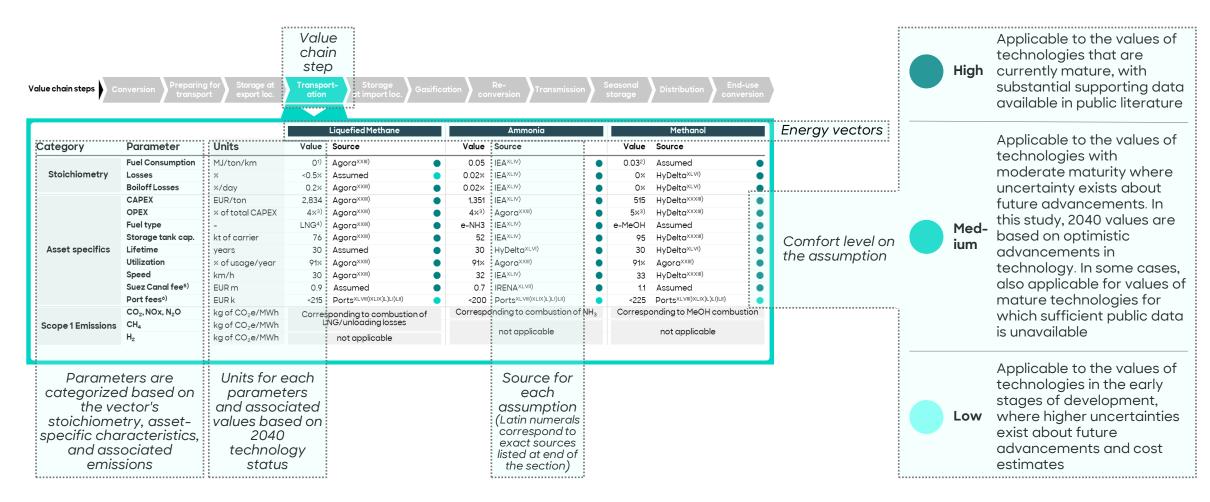
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## A. Assumptions

### In this section, assumptions used in the model have been detailed, including their source and comfort level

Explanation of the layout of the assumption section



Assumptions: General

Parameter	Units	Methane [Natural gas] Value Source	Hydrogen Value Source	Ammonia Value Source	Methanol Value Source	LOHC Value Source
kg to ton	[t/kg]	1,000 -	1,000 -	1,000 -	1,000 -	1,000 -
GJ to kWh	[kWh/GJ]	277.77 -	277.77 -	277.77 -	277.77 -	277.77 -
MJ to kWh	[kWh/MJ]	0.278 -	0.278 -	0.278 -	0.278 -	0.278 -
kWh to MJ	[MJ/kWh]	3.6 -	3.6 -	3.6 -	3.6 -	3.6 -
mmBTU to MWh	[-]	0.29 -	0.29 -	0.29 -	0.29 -	0.29 -
42-gallon barrel to liter	[liter/42- gallon barrel]	159 -	159 -	159 -	159 -	159 -
mcf to MWh	[MWh/mcf]	0.29 NRG <sup>I)</sup>	0.29 NRG <sup>I)</sup>	0.29 NRG <sup>I)</sup>	0.29 NRG <sup>I)</sup>	0.29 NRG <sup>I)</sup>
m³ to ton	[ton/m³]	0.4 Cetiner <sup>II)</sup>				
Lower heating value (LHV)	[MJ/m³]	35.8 Engineering toolbox [] TU Delft <sup>(V)</sup>				
Lower heating value (LHV)	[kWh/kg]	13.9 Engineering toolbox <sup>III</sup> ) [10.6 <sup>1</sup> )] TU Delft <sup>IV</sup> )	33.33 Engineering toolbox <sup>(II)</sup>	5.2 Engineering toolbox <sup>(II)</sup>	5.5 Engineering toolbox <sup>(II)</sup>	2.0 Deutscher Bundestag <sup>v)</sup>

Comfort level of the assumption: High Medium Low

<sup>1)</sup> Based on Groningen/North-sea gas

Assumptions: Emissions

		CO <sub>2</sub>		CH <sub>4</sub>	N <sub>2</sub>	0		NOx	H2	
Parameter	Units	Value Source		Value Source	Vo	alue Source		Value Source	Value :	Source
Global Warming Potential for 100 years	[kg of CO <sub>2e</sub> /kg]	1 -	•	27 IPCC <sup>VI)</sup>		273 IPCC <sup>VI)</sup>	•	8.5 Lammel & Graßl <sup>VII)</sup>	11.6	Sand et al. VIII)
Emissions from natural gas/methane combustion	[kg/kg]	2.69 US NETL <sup>IX)</sup>		<0.1 US NETL <sup>IX)</sup>		<0.1 US NETL <sup>IX)</sup>	•	0 US NETL <sup>IX)</sup>	0 (	JS NETL <sup>IX)</sup>
Emissions from ammonia combustion	[g/kWh]	0 Zero Carbon Shipping <sup>x)</sup>		O Zero Carbon Shipping <sup>X)</sup>		0.1 Zero Carbon Shipping <sup>x)</sup>	•	2.0 Zero Carbon Shipping <sup>x)</sup>	0.0	Zero Carbon Shipping <sup>x)</sup>
Emissions from methanol combustion	[g/MJ]	69.0 DNV <sup>XI</sup> )		0.0 DNV <sup>XI</sup> )		0.0 DNV <sup>XI</sup> )		0.4 DNV <sup>XI</sup> )	0.0	DNV <sup>XI)</sup>
Emissions from hydrogen combustion	[g/kg]	0.0 EU LCAXII)		0.0 EU LCAXII)		0.0 EU LCAXII)	•	6.8 EU LCA <sup>XII)</sup>	0.0	EU LCA <sup>XII)</sup>

Comfort level of the assumption: High Medium Low

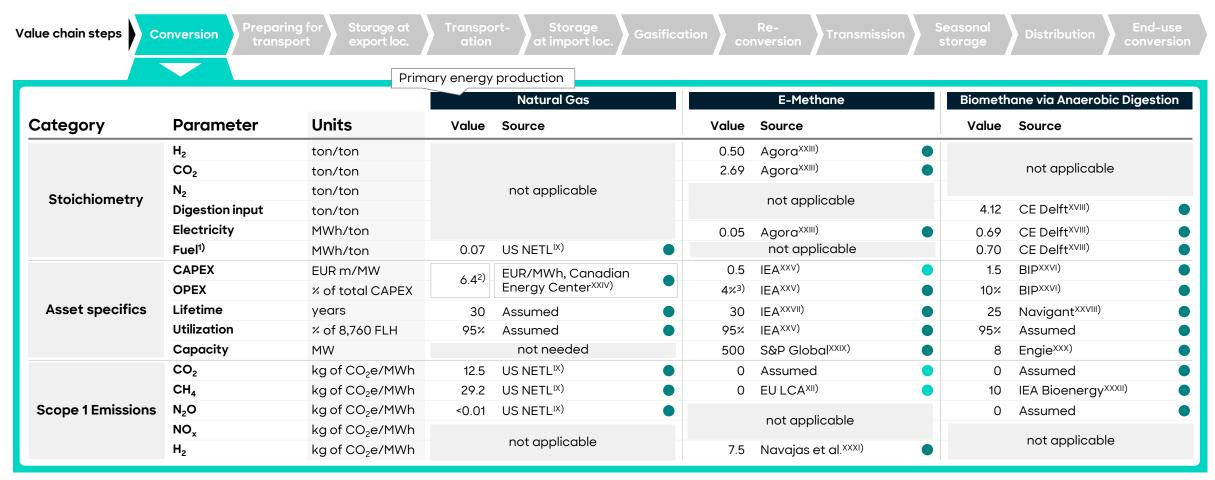
Assumptions: Feedstock

			US		Mic	ddle East		South	ern Europe		North	ern Europe
Parameter	Units	Value	Source		Value	Source		Value	Source		Value	Source
Grid electricity price	[EUR/MWh]	71	EIA <sup>XIII)</sup>	•	41	Assumed	•	73	VBW <sup>XIV)</sup>	•	58 [NL:92]	VBW <sup>XIV)</sup> , E-bridge <sup>XV)</sup>
Grid intensity	[ton of CO <sub>2</sub> /MWh]	0.05	IEA <sup>XVI</sup> )	•	0.21	Enerdata <sup>XVII)</sup>	•	0.03	IEA <sup>XVI)</sup>	•	0.03	IEA <sup>XVI)</sup>
Digestion feedstock price	[EUR/ton]	60	CE Delft <sup>XVIII</sup> )	•	60	CE Delft <sup>XVIII</sup> )	•	60	CE Delft <sup>XVIII</sup> )	•	60	CE Delft <sup>XVIII</sup> )
CO <sub>2</sub> price from DAC	[EUR/ton]	136	Natuur & Milieu <sup>XIX)</sup>	•	106	Natuur & Milieu <sup>XIX)</sup>	•	138	Natuur & Milieu <sup>XIX)</sup>	•	123	Natuur & Milieu <sup>XIX)</sup>
CO₂ price from biogenic byproduct	[EUR/ton]	29	US NETL <sup>XX)</sup>	•	26	US NETLXX)	•	30	US NETLXX)	•	28	US NETL <sup>XX)</sup>
CO <sub>2</sub> price from fossil/ biogenic point source	[EUR/ton]	59	US NETLXX)	•	49	US NETLXX)	•	59	US NETLXX)	•	54	US NETL <sup>XX)</sup>
Green Hydrogen production efficiency	[%]	76%	IEA <sup>XXI)</sup>	•	76%	IEA <sup>XXI)</sup>	•	76%	IEA <sup>XXI)</sup>	•	76%	IEA <sup>XXI)</sup>
Levelized cost of renewable Hydrogen	[EUR/kg]	2.5	IEA <sup>XXI)</sup>	•	2.5	IEA <sup>XXI)</sup>	•	2.8	IEA <sup>XXI)</sup>	•	3	IEA <sup>XXI)</sup>
LOHC (DBT) price	[EUR/kg]	1.6	HySTOC <sup>XXII)</sup>	•	1.6	HySTOC <sup>XXII)</sup>	•	1.6	HySTOC <sup>XXII)</sup>	•	1.6	HySTOC <sup>XXII)</sup>

Comfort level of the assumption: High Medium Low

<sup>1)</sup> We assume the same CO<sub>2</sub> tax for US and Middle East, as CBAM will ensure the carbon price of imports is equivalent to the carbon price of domestic production

Assumptions: Conversion/extraction (1/2)



<sup>1)</sup> Figure depicts combustion of the respective energy vector in the production step; 2) Number incorporate producing, under development and discovery phases of natural gas production; 3) Figure only covers fixed OPEX, excl. feedstock prices;

Assumptions: Conversion/extraction (2/2)

Storage at Value chain steps Conversion

				Ammonia			Methanol		LOHC (DBT)
Category	Parameter	Units	Value	Source		Value	Source	Value	Source
	H <sub>2</sub>	ton/ton	0.18	Agora <sup>XXIII)</sup>	•	0.20	HyDelta <sup>XXXIII)</sup>	0.06	HySTOC <sup>XXII)</sup>
	CO <sub>2</sub>	ton/ton		not applicable		0.07	HyDelta <sup>XXXIII)</sup>		
Stoichiometry	N <sub>2</sub>	ton/ton	0.82	Agora <sup>XXIII)</sup>			not applicable		not applicable
Stoichiometry	DBT-HO	ton/ton		not applicable			not applicable	0.94	EU LCA <sup>XII)</sup>
	Electricity	MWh/ton	0.651)	IRENAXXXIV)		0.20	HyDelta <sup>XXXIII)</sup>	0.02	EU LCA <sup>XII)</sup>
	Fuel <sup>2)</sup>	MWh/ton		not applicable			not applicable		not applicable
	CAPEX	EUR/ton	283	IRENAXXXIV)		158	HyDelta <sup>XXXIII)</sup>	21	IRENA <sup>XXXIV)</sup>
Asset specifics	OPEX <sup>3)</sup>	% of total CAPEX	3%	IRENAXXXIV)		2.7%	HyDelta <sup>XXXIII)</sup>	1.5%	HySTOC <sup>XXII)</sup>
	Lifetime	years	30	Assumed		30	Assumed	30	Assumed
	Utilization	% of 8,760 FLH	95 %	Assumed		95%	Assumed	95%	Assumed
	Capactiy	kt/year	1,825	IRENAXXXIV)		475	Hydelta <sup>XXXIII)</sup>	329	IRENA <sup>XXXIV</sup> )
	CO <sub>2</sub>	kg of CO <sub>2</sub> e/MWh				0	Assumed		
	CH <sub>4</sub>	kg of CO₂e/MWh		not applicable					not applicable
Scope 1 Emissions	N <sub>2</sub> O	kg of CO <sub>2</sub> e/MWh					not applicable		пос аррисаріе
	NO <sub>x</sub>	kg of CO₂e/MWh	1.6	EU LCAXII)					
	H <sub>2</sub>	kg of CO₂e/MWh	1.7	EU LCA <sup>XII)</sup>		0.4	EU LCA <sup>XII)</sup>	0.36	EU LCA <sup>XII)</sup>

<sup>1)</sup> Electricity consumption includes nitrogen separation from air; 2) Figure depicts combustion of the respective energy vector in the production step; 3) Figure only covers fixed OPEX, excl. feedstock prices

Assumptions: Preparing for transport

**Preparing for** Storage at Value chain steps transport

			E-Methane <sup>1)</sup> compression	E-Methane <sup>1)</sup> liquefaction	Hydrogen compression	Hydrogen liquefaction	
Category	Parameter	Units	Value Source	Value Source	Value Source	Value Source	
Stoichiometry	Electricity input	MWh/ton	0.28 Sterner et al. <sup>XXXV)</sup>	0.48 Agora <sup>XXIII)</sup>	0.52 HyDelta <sup>XXXIII)</sup>	6.0 IRENA <sup>XXXIV</sup> )	
Stoichiometry	Losses	%	0.15% US NETL <sup>IX)</sup>	0.1% Agora <sup>XXIII)</sup>	0.5% HyDelta <sup>XXXIII)</sup>	2% EU LCA <sup>XII)</sup>	
	CAPEX	EUR/ton	0.1 EUR/MWh,	750 Zhang et al.XXXVII)	180 HyDelta <sup>XXXIII)</sup>	2,915 IRENA <sup>XXXIV</sup> )	
	OPEX	% of total CAPEX	Oxford Inst. <sup>XXXVI)</sup>	2.5% <sup>2)</sup> Oxford Inst. <sup>XXXVI)</sup>	4% <sup>2)</sup> HyDelta <sup>XXXIII)</sup>	4% <sup>2)</sup> Agora <sup>XXIII)</sup>	
Asset specifics	Lifetime	years	15 Assumed	30 AppeaXXXVIII)	15 HyDelta <sup>XXXIII)</sup>	30 Assumed	
	Utilization	% of 8,760 FLH	85% Assumed	95% Assumed	85% HyDelta <sup>XXXIII)</sup>	95% HyDelta <sup>XXXIII)</sup>	
	Capacity	kt	not needed	32,000 Zhang et al. <sup>XXXVII)</sup>	14 HyDelta <sup>XXXIII)</sup>	73 IRENA <sup>XXXIV)</sup>	
	CO <sub>2</sub>	kg of CO <sub>2</sub> e/MWh	not applicable <sup>3)</sup>	not applicable <sup>3)</sup>			
	CH <sub>4</sub>	kg of CO₂e/MWh	Corresponding to losses	Corresponding to losses	not applicable	not applicable	
Scope 1 Emissions	N <sub>2</sub> O	kg of CO <sub>2</sub> e/MWh			not applicable	not applicable	
·	NO <sub>x</sub>	kg of CO <sub>2</sub> e/MWh	not applicable	not applicable			
	H <sub>2</sub>	kg of CO <sub>2</sub> e/MWh			Corresponding to losses	Corresponding to losses	

<sup>1)</sup> Input also valid for biomethane and fossil natural gas; 2) Value only comprises fixed OPEX, excl. feedstock costs; 3) Conversion process step is electrified and therefore only scope 2 emissions are considered

Assumptions: Local Storage (1/2)

Storage at Storage Value chain steps at import loc. export loc.

				Liquefied Methane <sup>1)</sup>			Ammonia			Methanol	
Category	Parameter	Units	Value	Source		Value	Source		Value	Source	
Stoichiometry	Electricity input	MWh/ton	1.21	MWh/kg of boiloff, Li & Wen <sup>XXXIX)</sup>	•	0.03	Llyod' s Register <sup>XL)</sup>	•	0	EU LCA <sup>XII)</sup>	
,	Losses	%	0%2)	EU LCAXII)		0.02%	EU LCAXII)	•	0%	EU LCAXII)	
	CAPEX			0.05 EUR/MWh/day,		909	HyDelta <sup>XXXIII)</sup>	•	473	HyDelta <sup>XXXIII)</sup>	
	OPEX	% of total CAPEX	0.05	Fluxys <sup>XLI)</sup>		2.0%3)	HyDelta <sup>XXXIII)</sup>		0.7%3)	HyDelta <sup>XXXIII)</sup>	
Asset specifies	Lifetime	years	40	40 Fluxys <sup>XLII)</sup>		30	Assumed		30	HyDelta <sup>XXXIII)</sup>	
Asset specifics	Utilization	% of 8,760 FLH	98%	Assumed		98%	Assumed		98%	Assumed	
	Capacity	kt	265	Fluxys <sup>XLIII)</sup>		55	HyDelta <sup>XXXIII)</sup>	•	32	HyDelta <sup>XXXIII)</sup>	
	Storage Length	days	Duration (	of sea transport one-way		Duration	of sea transport one-way		Duration o	of sea transport one-way	
	CO <sub>2</sub>	kg of CO₂e/MWh		not appliable							
	CH <sub>4</sub>	kg of CO₂e/MWh	0	EU LCAXII)							
Scope 1 Emissions	N <sub>2</sub> O	kg of CO₂e/MWh					not applicable		not applicable		
	NO <sub>x</sub>	kg of CO₂e/MWh									
	<b>H₂</b> kg of CO₂e/MWh	''									

1) Input also valid for biomethane and fossil natural gas; 2) Boiloff losses (-0.07 %/day) are assumed to be reliquefied; 3) Figures only comprises fixed OPEX excl. feedstock costs

Assumptions: Local Storage (2/2)

Value chain steps

Conversion

Preparing for transport

Storage at export loc.

Storage at export loc.

Storage at import loc.

Storage at import loc.

Gasification

Re-conversion

Transmission

Seasonal storage

Distribution

End-use conversion

Stoichiometry   Electricity input   Losses					LOHC			Liquid H <sub>2</sub>
Losses	Category	Parameter	Units	Value	Source		Value	Source
Capex	Stoichiomatry	Electricity input	MWh/ton	0	EU LCA <sup>XII)</sup>	•	0.15	HyDelta <sup>XXXIII)</sup> , IEA <sup>XLIV)</sup>
Plant specifics    Comparison	Stoichionletry	Losses	%/day	0%	EU LCAXII)	0%1)		IRENA <sup>XXXIV</sup> )
Plant specifics  Lifetime years 30 HyDeltaXXXIII) 30 HyDeltaXXXIII)  Utilization % of 8,760 FLH 98% HyDeltaXXXIII) 98% Assumed  Capacity kt 30 Ortiz Cebolla et al.XLV) 7 HyDeltaXXXIII)  Storage Length days Duration of sea transport one-way Duration of sea transport one-way  CO2 kg of CO2e/MWh CH4 kg of CO2e/MWh N2O kg of CO2e/MWh NOx kg of CO2e/MWh NOx kg of CO2e/MWh		CAPEX	EUR/ton	322	Ortiz Cebolla et al.XLV)		13,650	IRENA <sup>XXXIV</sup> )
Plant specifics  Utilization % of 8,760 FLH 98% HyDelta*XXXIII) 98% Assumed  Capacity kt 30 Ortiz Cebolla et al.*XLV) 7 HyDelta*XXXIII)  Storage Length days Duration of sea transport one-way Duration of sea transport one-way  CO2 kg of CO2e/MWh  CH4 kg of CO2e/MWh  N2O kg of CO2e/MWh NOx kg of CO2e/MWh  NOx kg of CO2e/MWh		OPEX	% of total CAPEX	1.0% <sup>2)</sup>	Ortiz Cebolla et al.XLV)		2.0%2)	HyDelta <sup>XXXIII)</sup>
Capacity kt 30 Ortiz Cebolla et al.XLV) 98% Assumed 7 HyDeltaXXXIII)  Storage Length days Duration of sea transport one-way Duration of sea transport one-way  CO <sub>2</sub> kg of CO <sub>2</sub> e/MWh  CH <sub>4</sub> kg of CO <sub>2</sub> e/MWh  N <sub>2</sub> O kg of CO <sub>2</sub> e/MWh  NO <sub>x</sub> kg of CO <sub>2</sub> e/MWh  NO <sub>x</sub> kg of CO <sub>2</sub> e/MWh	Dignt enseifies	Lifetime	years	30	HyDelta <sup>XXXIII)</sup>		30	HyDelta <sup>XXXIII)</sup>
Storage Length days Duration of sea transport one-way Duration of sea transport one-way  CO2 kg of CO2e/MWh  CH4 kg of CO2e/MWh  N2O kg of CO2e/MWh  NOx kg of CO2e/MWh  NOx kg of CO2e/MWh	Plant specifics	Utilization	% of 8,760 FLH	98%	HyDelta <sup>XXXIII)</sup>		98%	Assumed
CO2         kg of CO2e/MWh           CH4         kg of CO2e/MWh           N2O         kg of CO2e/MWh         not applicable           NOx         kg of CO2e/MWh		Capacity	kt	30	Ortiz Cebolla et al.XLV)		7	HyDelta <sup>XXXIII)</sup>
CH4         kg of CO2e/MWh         not applicable           Scope 1 Emissions         N2O         kg of CO2e/MWh         not applicable           NOx         kg of CO2e/MWh		Storage Length	days	Duration o	of sea transport one-way		Duration	of sea transport one-way
Scope 1 Emissions N <sub>2</sub> O kg of CO <sub>2</sub> e/MWh not applicable NO <sub>x</sub> kg of CO <sub>2</sub> e/MWh		CO <sub>2</sub>	kg of CO <sub>2</sub> e/MWh					
Scope 1 Emissions N₂O kg of CO₂e/MWh not applicable NO₂ kg of CO₂e/MWh		CH <sub>4</sub>	kg of CO₂e/MWh					not applicable
	Scope 1 Emissions	N <sub>2</sub> O	kg of CO₂e/MWh		not applicable			not applicable
H₂ kg of CO₂e/MWh Corresponding to losses in storage		NO <sub>x</sub>	kg of CO₂e/MWh					
- 5 2		H <sub>2</sub>	kg of CO₂e/MWh				Corresp	oonding to losses in storage

1) Boiloff losses (-0.1%/day) is assumed to be reliquefied, requiring 0.15 kWh per kg of boiloff gas; 2) Value only comprises fixed OPEX, excl. feedstock costs

Assumptions: Maritime transport (1/2)

 Value chain steps
 Conversion
 Preparing for transport
 Storage at export loc.
 Storage at import loc.
 Gasification
 Re-conversion
 Transmission
 Seasonal storage
 Distribution
 End-use conversion

				Liquefied Methane			Ammonia		Methanol	
Category	Parameter	Units	Value	Source		Value	Source	Value	Source	
	Fuel Consumption	MJ/ton/km	O <sup>1)</sup>	Agora <sup>XXIII)</sup>	•	0.05	IEA <sup>XLIV</sup> )	0.032)	Assumed	
Stoichiometry	Losses	%	<0.5%	Assumed	•	0.02%	IEA <sup>XLIV)</sup>	0%	HyDelta <sup>XLVI)</sup>	
	<b>Boiloff Losses</b>	%/day	0.2%	Agora <sup>XXIII)</sup>		0.02%	IEA <sup>XLIV</sup> )	0%	HyDelta <sup>XLVI)</sup>	
	CAPEX	EUR/ton	2,834	Agora <sup>XXIII)</sup>		1,351	IEA <sup>XLIV</sup> )	515	HyDelta <sup>XXXIII)</sup>	
	OPEX	% of total CAPEX	4% <sup>3)</sup>	Agora <sup>XXIII)</sup>		4% <sup>3)</sup>	Agora <sup>XXIII)</sup>	5% <sup>3)</sup>	HyDelta <sup>XXXIII)</sup>	
	Fuel type	-	LNG <sup>4)</sup>	Agora <sup>XXIII)</sup>		e-NH3	IEA <sup>XLIV)</sup>	e-MeOH	Assumed	
	Storage tank cap.	kt of vector	76	Agora <sup>XXIII)</sup>		52	IEA <sup>XLIV</sup> )	95	HyDelta <sup>XXXIII)</sup>	
Asset specifics	Lifetime	years	30	Assumed		30	HyDelta <sup>XLVI)</sup>	30	HyDelta <sup>XLVI)</sup>	
	Utilization	% of usage/year	91%	Agora <sup>XXIII)</sup>		91%	Agora <sup>XXIII)</sup>	91%	Agora <sup>XXIII)</sup>	
	Speed	km/h	30	Agora <sup>XXIII)</sup>		32	IEA <sup>XLIV)</sup>	33	HyDelta <sup>XXXIII)</sup>	
	Suez Canal fee <sup>5)</sup>	EUR m	0.9	Assumed		0.7	IRENA <sup>XLVII)</sup>	1.1	Assumed	
	Port fees <sup>6)</sup>	EUR k	<215	Ports <sup>XLVIII</sup> )XLIX)L)LI)LII)		<200	Ports <sup>XLVIII</sup> ) <sup>XLIX</sup> )L)LI)LII)	<225	Ports <sup>XLVIII</sup> )XLIX)L)LI)LII)	
	CO <sub>2</sub> , NOx, N <sub>2</sub> O	kg of CO₂e/MWh	Corres	ponding to combustion of		Correspo	onding to combustion of NH <sub>3</sub>	Corresp	onding to MeOH combustion	
Scope 1 Emissions	CH <sub>4</sub>	kg of CO₂e/MWh			n at annul a alala		n at amulia alala			
	H <sub>2</sub>	kg of CO₂e/MWh		not applicable			not applicable		not applicable	

<sup>1)</sup> LNG carrier runs on boiloff losses; 2) Methanol vessels assumed to have identical fuel consumption in MJ/ton as ammonia vessels; 3) Value only comprises fixed OPEX, excl. feedstock costs; 4) CO<sub>2</sub> emissions only accounted for natural gas, as emissions from e-methane are net zero; 5) Tariff for roundtrip through Suez canal on MENA route scales by weight of cargo; 6) Port fees of import (Rotterdam) and export port (US: Corpus Christi, MENA: Abu Dhabi, ESP: Huelva, NOR: Greenland)
Source: Oxford Institute for Energy Studies, HyDelta, EU LCA, DNV, ZeroCarbon Shipping

Comfort level of the assumption:

Medium

Low

Assumptions: Maritime transport (2/2)

Transport-Storage at Value chain steps ation

				LOHC		Liquid H <sub>2</sub>	
Category	Parameter	Units	Value	Source	Value	Source	
	Fuel Consumption	MJ/ton/km	0.031)	Assumed	02)	IEA <sup>XLIV</sup> )	•
Stoichiometry	Losses	%	0%	HyDelta <sup>XLVI)</sup>	1%	IEA <sup>XLIV)</sup>	
	<b>Boiloff Losses</b>	%/day	0%	HyDelta <sup>XLVI)</sup>	0.6%	IEA <sup>XLIV</sup> )	
	CAPEX	EUR/ton	471	HyDelta <sup>XXXIII)</sup>	40,196	IEA <sup>XLIV</sup> )	
	OPEX	% of total CAPEX	6% <sup>3)</sup>	HyDelta <sup>XXXIII)</sup>	4% <sup>3)</sup>	Agora <sup>XXIII)</sup>	
	Fuel type	-	e-MeOH	Assumed	Liquid H <sub>2</sub>	IEA <sup>XLIV)</sup>	
	Storage tank cap.	kt of vector	104	HyDelta <sup>XXXIII)</sup>	10	IEA <sup>XLIV)</sup>	
Asset specifics	Lifetime	years	30	HyDelta <sup>XLVI)</sup>	30	HyDelta <sup>XLVI)</sup>	
	Utilization	% of usage/year	91%	Agora <sup>XXIII)</sup>	91%	Agora <sup>XXIII)</sup>	
	Speed	km/h	33	HyDelta <sup>XXXIII)</sup>	30	IEA <sup>XLIV)</sup>	
	Suez Canal fee <sup>4)</sup>	EUR m	1.2	Assumed	0.1	Assumed	
	Port fees <sup>5)</sup>	EUR k	<230	Ports <sup>XLVIII)XLIX</sup> )L)LI)LII)	<190	Ports <sup>XLVIII)XLIX</sup> )L)LI)LII)	
	CO <sub>2</sub> , NOx, N <sub>2</sub> O	kg of CO <sub>2</sub> e/MWh	Correspo	nding to MeOH combustion <sup>1)</sup>	Corresp	onding to combustion of LH	$H_2$
Scope 1 Emissions	CH <sub>4</sub>	kg of CO <sub>2</sub> e/MWh		not applicable		not applicable	
	H <sub>2</sub>	kg of CO <sub>2</sub> e/MWh		пот аррисаріе	Corresp	oonding to losses of loading	3

Assumptions: Pipeline Transportation

Value chain steps Conversion Preparing for transport Storage at export loc. Storage at export loc. Storage at import loc. Gasification Re-conversion Transmission Seasonal storage Distribution Conversion

			C	Compressed methane	C	ompressed hydrogen
Category	Parameter	Units	Value	Source	Value	Source
Stoichiometry	Electricity input	kWh/ton/km	0.08	EU LCA <sup>XII)</sup>	0.6	Agora <sup>XXIII)</sup>
Stoichiometry	Losses	%/1,000 km	0.02%	EU LCA <sup>XII)</sup>	0.40%1)	EU LCA <sup>XII)</sup>
	Existing tariff [NOR]	EUR/MWh	10 <sup>2)</sup>	Bottom-up calculation		not applicable
	Existing tariff [ESP]	EUR/MWh	10 <sup>3)</sup>	Bottom-up calculation		
	New tariff	EUR/MWh/1000 km	3.94)	Assumed	6.0	IEA <sup>LIII)</sup>
Dl	Lifetime	years	55	Assumed	55	Assumed
Plant specifics	Plant specifics Utilization	%	70% <sup>5)</sup>	Calculated	90%5)	Calculated
	Pipeline length [NOR]	km	~2,300	Assumed	~ 2,300	Assumed
	Pipeline length [ESP]	km	~2,300	Assumed	~ 2,300	Assumed
	Max. capacity	GW	18.8	Assumed	16.9	IEA <sup>LIII)</sup>
	CO <sub>2</sub>	kg of CO₂e/MWh		not applicable		
	CH <sub>4</sub>	kg of CO₂e/MWh	Corresp	oonding to losses in pipeline		not applicable
Scope 1 Emissions	N <sub>2</sub> O	kg of CO₂e/MWh				not applicable
•	NO <sub>x</sub>	kg of CO₂e/MWh		not applicable		
	H <sub>2</sub>	kg of CO <sub>2</sub> e/MWh			Corresp	oonding to losses in pipeline

<sup>1)</sup> Considering total loss of 1% and then dividing by 2.5 to get the loss in %/1,000 km; 2) Pipeline length form NOR and ESP is similar; 3) Tariff assumes transmission from Spain via France and Belgium; 4) NG pipeline cost are assumed by scaling hydrogen pipeline LCOH by 65% to account for fact that CAPEX of NG pipeline is 30-40% cheaper and can carry 10% more volume; 5) Utilization is scaled for the total expected demand by 2040 Source: HyDelta, EU LCA, Fluxys, IEA

Comfort level of the assumption: High Medium Low

Assumptions: Gasification

Storage at Value chain steps Gasification

			Lic	quified Methane to Gas	Lic	uified Hydrogen to Gas
Category	Parameter	Units	Value	Source	Value	Source
	Electricity	MWh/ton	0.06	EU LCA <sup>XII)</sup>	0.2	IRENA <sup>XXXIV)</sup>
Stoichiometry	Electricity price	EUR/MWh	92	E-bridge <sup>XV)</sup>	92	E-bridge <sup>XV)</sup>
	Losses	%	0.01%	EU LCA <sup>XII)</sup>	0.01%	Assumed
	CAPEX	EUR/ton	200	Frontier <sup>LIV)</sup>	441	IRENAXXXIV)
	OPEX	% of total CAPEX.	2.5%	Assumed	4%1)	Brändle et al. <sup>LV)</sup>
Asset specifics	Lifetime	years	30	Assumed	30	Assumed
	Utilization	% of 8,760 FLH	95%	Assumed	95%	Assumed
	Capacity	kt/year	174	TWh, Fluxys <sup>XLIII)</sup>	912	IRENAXXXIV)
	CO <sub>2</sub>	kg of CO₂e/MWh		not applicable		
	CH <sub>4</sub>	kg of CO <sub>2</sub> e/MWh	Corresp	oonding to losses in pipeline	not applicable	
Scope 1 Emissions	$N_2O$	kg of CO <sub>2</sub> e/MWh				not applicable
	NO <sub>x</sub>	kg of CO₂e/MWh		not applicable		
	H <sub>2</sub>	kg of CO₂e/MWh			Corres	oonding to losses in pipeline

<sup>1)</sup> Value only comprises fixed OPEX, excl. feedstock costs

Assumptions: Reconversion

Value chain steps

ring for Storage at Transport-Storage sport export loc. Gasifica

Reconversion Seasonal storage istribution

conversion

			Methane to H2 (SMR)		Ammonia to	Hydrogen	Metl	nanol to Hydrogen		LOHC (DBT to H <sub>2</sub> )
Category	Parameter	Units	Value Source		Value Source		Value	Source	Valu	ie Source
	Energy vector	ton/ton	1.32 IEA <sup>XLIV</sup> )	•	7.2 HyDelto	XLVI)	7.1	EU LCA <sup>XII)</sup>	22.4	<sup>11)</sup> Assumed
Stoichiometry	Electricity	MWh/ton	O <sup>2)</sup> EU LCA <sup>XII)</sup>		0.99 <sup>3)</sup> HyDelto	XLVI)	1.32,3)	EU LCAXII)	1.9	<sup>3)</sup> EU LCA <sup>XII)</sup>
	Electricity price	EUR/MWh	95 E-bridge <sup>XV)</sup>		95 E-bridg	e <sup>XV)</sup>	95	E-bridge <sup>XV)</sup>		75 E-bridge <sup>XV)</sup>
	CAPEX	EUR/ton	655 EUR/kW, IEAXLIV)		1,041 HyDelto	XLVI)	455	Agora <sup>XXIII)</sup>	• 7d	9 IRENAXXXIV)
	OPEX	% of total CAPEX.	5%4) IEAXLIV)		3% <sup>4)</sup> IEA <sup>XLIV)</sup>	(XLIV)		HyDelta <sup>XXXIII)</sup>	2.5%	(4) HySTOC <sup>XXII)</sup>
Asset specifics	Lifetime	years	25 Assumed		25 IEAXXVII)	•	25	Assumed	• 2	25 Assumed
	Utilization	% of 8,760 FLH	90% Assumed		90% Assume	ed 🔵	90%	HyDelta <sup>XXXIII)</sup>	90	% Assumed
	Capacity	kt/year	75 HyDelta <sup>XLVI)</sup>		270 HyDelto	XLVI)	183	Agora <sup>XXII)</sup>	2:	25 IRENA <sup>XXXIV</sup> )
	CO <sub>2</sub>	kg of CO₂e/MWh	270 <sup>5)</sup> EU LCA <sup>XII)</sup>		not anal	iaabla	06)	EU LCA <sup>XII)</sup>		
	CH <sub>4</sub>	kg of CO₂e/MWh			not applicable					not applicable
Scope 1 Emissions	N <sub>2</sub> O	kg of CO₂e/MWh	not applicable		<0.01 EU LCA	<0.01 EU LCA <sup>XII)</sup>		not applicable		
-	NO <sub>x</sub>	kg of CO₂e/MWh	not applicable		0.5 EU LCA <sup>XII)</sup>					1.1 EU LCA <sup>XII)</sup>
	H <sub>2</sub>	kg of CO <sub>2</sub> e/MWh		0 EU LCAXII)		KII)	0.04	EU LCAXII)	<0.	01 EU LCA <sup>XII)</sup>

Assumptions: Transmission

Value chain steps

Conversion

Preparing for Storage at export loc.

Storage at import loc.

Gasification

Reconversion

Seasonal storage

Distribution

End-use conversion

			e-	Methane/Biomethane			Hydrogen		
Category	Parameter	Units	Value	Source		Value	Source		
Stoichiometry	Electricity input	kWh/ton/km	0.08	EU LCA <sup>XII)</sup>	•	0.6	Agora <sup>XXIII)</sup>		
3 tolchiometry	Losses	%/1,000 km	0.02%	EU LCA <sup>XII)</sup>		0.04%1)	EU LCAXII)		As cluster 6 and power plants will
	Tariff	EUR/MWh	1.6 <sup>2)</sup>	Bottom-up calculation		1.7			require a dedicated pipeline they will
	Lifetime	years	55	Assumed		55	Assumed		pay an additional cost to this tariff:
Plant specifics	Utilization	% of 8760 FLH	90%	Assumed		90%	Assumed		• Process heat cluster 6: EUR/MWh 16
	Capacity input	TWh	359 <sup>4)</sup>	Assumed, II3050 <sup>LVI)</sup>		137	113050 <sup>LVI)</sup>		• Electricity production: EUR/MWh 1.4
	Average distance per end-user	km	250	Assumed	•	250	Assumed		
	CO <sub>2</sub>	kg of CO <sub>2</sub> e/MWh		not applicable					
	CH <sub>4</sub>	kg of CO <sub>2</sub> e/MWh	Corresp	oonding to losses in pipelir	ne				
Scope 1 Emissions	N <sub>2</sub> O	kg of CO <sub>2</sub> e/MWh					not applicable		
-	NO <sub>x</sub>	kg of CO <sub>2</sub> e/MWh		not applicable					
	H <sub>2</sub>	kg of CO <sub>2</sub> e/MWh				Corresp	onding to losses in pipeline	е	
					1				

<sup>1)</sup> Considering total loss of 1% and then dividing by 2.5 to get the loss in %/1,000 km; 2) Tariff is the mean of the past five years of annual revenues of Gasunie Transport Services divided by the annual gas supply in the respective year and scaled by a factor of 2.5 to account for reduction in demand; 3) Combination of HTL and RTL pipelines; 4) Includes demand from e-methane and natural gas and demand for export Source: HyDelta, EU LCA, Fluxys

Comfort level of the assumption: High Medium Low Roland Berger | 18

## Backup on the assumptions for transmission pipeline tariffs in 2040

Transmission tariff calculation - 2024, 2030 and 2040

Source: HyWay27, GTS annual reports, IRENA, Liander, HyRegions, Netbeheer Nederland, II3050

Gas network - 2024	Gas network - 204	0 H2-backbone - 20	)30 H2-backbone - 2040	)
Not	Not	3.7	3.7	_
applicable	applicable	0.99	0.99	_
		70%	70%	
11,256	11,256	1100	1600	_
4584	3670 <sup>1)</sup>	1,997	3,865	
55	55	55	55	
4%	4%	4% 1% of new	4% 1% of new	
10%	10%	2.1% value of pipelines	1.5% value of pipelines	
796	581	160	286	_
Not applicable	Not applicable	Not applicable	Not applicable	
700	359 <sup>2)</sup>	78	136	
1.1	1.6	2.0	1.7	
	Not applicable  11,256  4584  55  4%  10%  796  Not applicable  700	Not applicable       Not applicable         11,256       11,256         4584       3670¹)         55       55         4%       4%         10%       10%         796       581         Not applicable       Not applicable         700       359²)	Not applicable       Not applicable       3.7         11,256       11,256       1100         4584       3670¹)       1,997         55       55       55         4%       4%       4%       1x of new value of pipelines         10%       10%       2.1%       pipelines         796       581       160         Not applicable       Not applicable       Not applicable         700       359²)       78	Not applicable         Not applicable         3.7         3.7           11,256         11,256         1100         1600           4584         3670¹)         1,997         3,865           55         55         55         55           4%         4%         4%         1% of new value of pipelines         1.5% pipelines           10%         10%         2.1% pipelines         1.5% pipelines           796         581         160         286           Not applicable         Not applicable         Not applicable         Not applicable           700         359²)         78         136

#### **Key assumptions**

- CAPEX for hydrogen pipelines is based on HyWay27 and adjusted with inflation percentage of 5.3% year on year between 2021-2024<sup>3</sup>)
- Assuming 30% of the backbone will be new pipelines and 70% will be refurbished pipelines in 2030
- The hydrogen backbone is assumed to be 1100 km in 2030 and 500 km is added to backbone in 2040 to account for additional volume needed
- OPEX for hydrogen backbone is assumed to be 1% of the new value of the backbone

<sup>1)</sup> Estimated by adding the expected investments to the current book value and subtracting the expected depreciation costs; 2) Includes methane demand for export; 3) HyWay27 estimated the capex per km for the hydrogen backbone in a report published in 2021, we account for the value increase since

## Backup on the assumptions for transmission pipeline tariffs in 2040

Additional pipeline CAPEX for electricity production & process heat cluster 6 - 2040

	Electricity pro	duction	Process heat f	or cluster 6
Parameters	Hydrogen	Methane	Hydrogen	Methane
Capex new [EUR m/km]	1.9			n pipeline with n diameter
Capex refurbished [EUR m/km]	0.5		1.25 multiplie factor o	ed by scaling f 2.5
New pipeline [%]	50%		50%	
Pipeline length [km]	150	Assumed to be	400	Assumed to be
Total CAPEX [EUR m]	177	directly connected to the	750	directly connected to the
Lifetime [years]	55	main transmission grid	55	main transmission grid
WACC[%]	8%		8%	
OPEX [% of CAPEX]	1.6%		1.3%	
TOTEX [EUR m/year]	13		54	
Volume [TWh]	14		5	
Tariff for H <sub>2</sub> [EUR/MWh]	1.4		16	

#### **Key assumptions**

- Power plants and industrial facilities in cluster 6 will require dedicated pipelines to connect to the hydrogen backbone
- The additional CAPEX is accounted via an added tariff
- WACC of 8% is assumed as cost of capital will be higher for private players compared to GTS
- In electricity production, pipeline diameter is assumed to be 50% of the diameter of the H<sub>2</sub> backbone pipeline resulting in 50% of the H<sub>2</sub> backbone CAPEX
- In cluster 6 industry, a factor of 2-3 to the original Capex numbers is applied to account for additional complexities and safety adherences in the placing of the pipelines
- Length of additional pipeline required is based on the HyRegions report
- In electricity production 9 power plants are not directly connected to the backbone, also based on the HvRegions report

Assumptions: Seasonal storage

 Value chain steps
 Conversion
 Preparing for transport
 Storage at export loc.
 Storage at import loc.
 Gasification
 Reconversion
 Transmission
 Seasonal storage
 Distribution
 End-use conversion

			e-	Methane/Biomethane			Hydrogen			
Category	Parameter	Units	Value	Source		Value	Source			
Stoichiometry	Electricity input	MWh/MWh	0.02	Assumed		0.03	HyDelta <sup>XXXIII)</sup>	•		
Stolchionieu y	Losses	%/day	0.02%	Assumed		0.04%	IEA <sup>LVII)</sup>		Different share of gas sent to	o storage
	Depleted gas field tariff	EUR/MWh	10	Bottom-up calculation	•	36	Bottom-up calculation	•	assumed per use case:  Iron & steel	5-15%
Plant specifics	Salt cavern tariff	EUR/MWh	15	Bottom-up calculation		51	Bottom-up calculation		• Process heat cluster 1-5	5-15%
	Share of gas sent to storage	% of total gas						•	Process heat cluster 6	5-15%
	CH <sub>4</sub>	kg of CO <sub>2e</sub> /MWh	Co	orresponding to losses			not applicable		Electricity production      December 1 beating.	25-35%
Scope 1 Emissions	H <sub>2</sub>	$kg of CO_{2e}/MWh$		not applicable		Сс	orresponding to losses		Decentral heating	35-45%

1) Number only covers fixed OPEX, excl. feedstock costs

## Backup on the assumptions for seasonal storage tariffs in 2040

Seasonal storage tariff calculation for hydrogen and e-methane<sup>1)</sup>

		Depleted gas field		Salt cavern
	H <sub>2</sub>	E-CH <sub>4</sub>	H <sub>2</sub>	E-CH₄
Working gas volume [bcm]	0.78	0.78	0.08	0.08
Cushion gas volume [bcm]	2.00	2.00	0.06	0.06
Lease rate [EUR m/year]	10	10		not applicable
Storage CAPEX [EUR m]	no	additional investment needed	60	60
Cushion gas CAPEX [EUR m]	540	693	17	22
Compression CAPEX [EUR m]	11.9	4.0	10.0	3.3
Wells/piping CAPEX [EUR m]	4.4	4.4	3.2	3.2
Gas cleaning CAPEX [EUR m]	30.7		Assuming no gas cle	eaning required
OPEX [EUR m / year]	16.3	12.5	1.6	2.0
Lifetime [years]	30	30	30	30
WACC[%]	8%	8%	8%	8%
LCOS [EUR/MWh]	35	10	51	15

#### **Key assumptions**

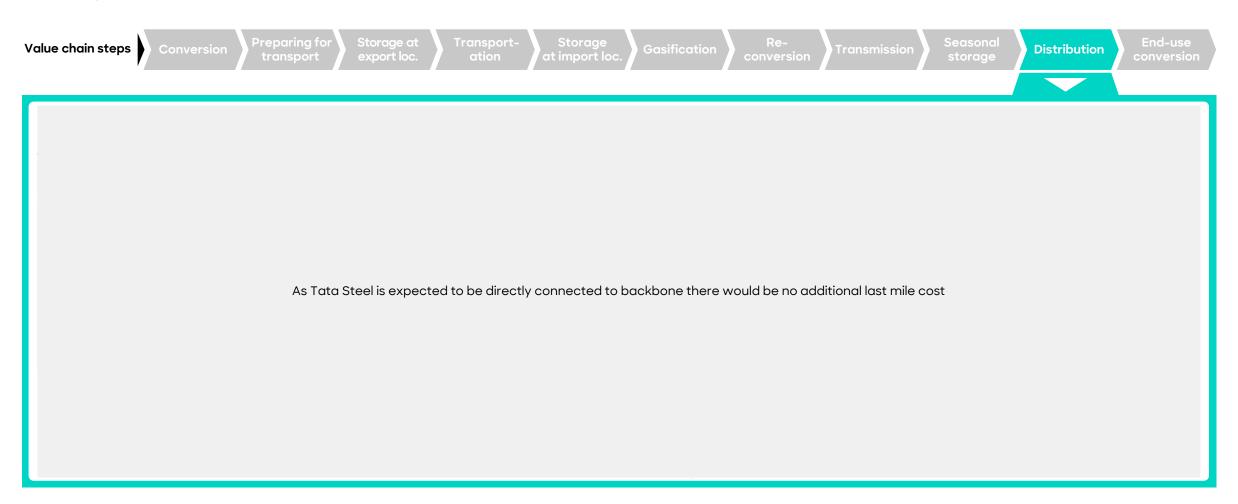
- Assuming H<sub>2</sub> price of 3 EUR/kg and CH<sub>4</sub> price of 30 EUR/MWh
- A mix of green and blue hydrogen is used as cushion gas for hydrogen storage and natural gas is used as cushion gas for emethane storage
- CAPEX for methane compressors assumed to be one third of CAPEX for hydrogen compressors
- No cleaning assumed for e-methane in depleted gas fields or for e-methane or hydrogen in salt caverns
- Salt caverns assumed to have 2 cycles/year

Source: TNO, HyDelta, EWI, Desk research

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<sup>1)</sup> Taking half the  $H_2$  and  $CH_4$  price would lead to tariffs of 22.3 and 6.1 EUR/MWh for  $H_2$  and  $e-CH_4$  storage resp. in depleted gas fields & 41.6 and 11.4 EUR/MWh for  $H_2$  and  $e-CH_4$  storage resp. in salt caverns

Assumptions: Distribution - Iron & steel



Assumptions: End-use conversion - Iron & steel

 Value chain steps
 Conversion
 Preparing for transport
 Storage at export loc.
 Transport- ation
 Storage at import loc.
 Gasification
 Re- conversion
 Transmission
 Seasonal storage
 Distribution
 End-use conversion

				e-	Methane/Biomethane			Hydrogen
Stoichiometry  Hydrogen MWh/ton steel not applicable 2.2 TSNLVIII), AgoraXXIII)  Electricity MWh/ton steel 0.8 TSNLVIII), AgoraXXIII) 0.8 TSNLVIII), AgoraXXIII)  Coal ton/ton steel 0.03 TSNLVIII), AgoraXXIII) 0.03 TSNLVIII), AgoraXXIII)  CAPEX EUR/ton steel 750¹) DIWLIX 750¹) DIWLIX)  Demand TWh/year 14 II3050LVI) 14 II3050LVI) 14 II3050LVI)  Other plant specific financials not considered²)  CO2 kg of CO2e/ton steel 80²) Climate accountabilityLXI 80 Climate accountabilityLXI 100 CH4 kg of CO2e/ton steel No2 kg of CO2e/ton steel No2 kg of CO2e/ton steel No2 kg of CO2e/ton steel No3 kg of CO	Category	Parameter	Units	Value	Source	Vo	alue	Source
Stoichiometry   Electricity   MWh/ton steel   0.8   TSNLVIII), Agora		Methane	MWh/ton steel	2.4	TSN <sup>LVIII)</sup> , Agora <sup>XXIII)</sup>			not applicable
Coal   ton/ton steel   0.8   TSNLVIII), Agora   0.8   TSNLVIII), Agora   0.8   TSNLVIII), Agora   (2.5   TSNLVIII), Agor	Stoichiomotry	Hydrogen	MWh/ton steel		not applicable		2.2	TSN <sup>LVIII)</sup> , Agora <sup>XXIII)</sup>
Plant specifics  CAPEX  EUR/ton steel 750¹) DIW <sup>LIX</sup> Demand TWh/year 14 II3050 <sup>LVI</sup> ) 14 II3050 <sup>LVI</sup> )  Other plant specific financials not considered²)  CO <sub>2</sub> kg of CO <sub>2</sub> e/ton steel 80²) Climate accountability <sup>LX</sup> 80 Climate accountability <sup>LX</sup> CH <sub>4</sub> kg of CO <sub>2</sub> e/ton steel N <sub>2</sub> O kg of CO <sub>2</sub> e/ton steel N <sub>2</sub> O kg of CO <sub>2</sub> e/ton steel N <sub>2</sub> O kg of CO <sub>2</sub> e/ton steel NO <sub>x</sub> kg of CO <sub>2</sub> e/ton steel NO <sub></sub>	Stoichiometry	Electricity	MWh/ton steel	0.8	TSN <sup>LVIII)</sup> , Agora <sup>XXIII)</sup>		8.0	TSN <sup>LVIII)</sup> , Agora <sup>XXIII)</sup>
Plant specifics  Other plant specific financials not considered <sup>2</sup> )  CO <sub>2</sub> kg of CO <sub>2</sub> e/ton steel 80 <sup>2</sup> ) Climate accountability <sup>LX</sup> ) 80 Climate accountability <sup>LX</sup> )  CH <sub>4</sub> kg of CO <sub>2</sub> e/ton steel  N <sub>2</sub> O kg of CO <sub>2</sub> e/ton steel  NO <sub>x</sub> kg of CO <sub>2</sub> e/ton steel  not applicable		Coal	ton/ton steel	0.03	TSN <sup>LVIII)</sup> , Agora <sup>XXIII)</sup>	(	0.03	TSN <sup>LVIII)</sup> , Agora <sup>XXIII)</sup>
Plant specifics  Other plant specific financials not considered <sup>2)</sup> CO <sub>2</sub> kg of CO <sub>2</sub> e/ton steel 80 <sup>2)</sup> Climate accountability <sup>LX)</sup> 80 Climate accountability <sup>LX)</sup> CH <sub>4</sub> kg of CO <sub>2</sub> e/ton steel N <sub>2</sub> O kg of CO <sub>2</sub> e/ton steel not applicable  NO <sub>x</sub> kg of CO <sub>2</sub> e/ton steel		CAPEX	EUR/ton steel	750 <sup>1)</sup>	DIW <sup>LIX</sup> )	7	′50¹)	DIW <sup>LIX</sup> )
		Demand	TWh/year	14	II3050 <sup>LVI)</sup>		14	II3050 <sup>LVI)</sup>
	Plant specifics		Ot	her plant s	pecific financials not considere	ed <sup>2)</sup>		
Scope 1 Emissions  N <sub>2</sub> O kg of CO <sub>2</sub> e/ton steel  NO <sub>x</sub> kg of CO <sub>2</sub> e/ton steel  not applicable  not applicable		CO <sub>2</sub>	kg of CO <sub>2</sub> e/ton steel	80 <sup>2)</sup>	Climate accountability <sup>LX)</sup>		80	Climate accountability <sup>LX)</sup>
NO <sub>x</sub> kg of CO <sub>2</sub> e/ton steel not applicable not applicable		CH <sub>4</sub>	kg of CO <sub>2</sub> e/ton steel					
kg of CO <sub>2</sub> e/ton steel	Scope 1 Emissions	N <sub>2</sub> O	kg of CO <sub>2</sub> e/ton steel		n at amalia alala			not emplionale
U long of OO a few stand		NO <sub>x</sub>	kg of CO <sub>2</sub> e/ton steel		not applicable			not applicable
$\mathbf{n_2}$ kg of $\mathbf{CO_2}$ e/ton steel		H <sub>2</sub>	kg of CO <sub>2</sub> e/ton steel					

<sup>1)</sup> The financial analysis is focused on cost of energy required per ton of steel and as the costs for an e-methane and hydrogen DRI system are the same, plant specific financials are not considered. Only for the total investment cost analysis for the Netherlands, CAPEX for a DRI system is considered; 2) Emissions for natural gas assumed to be 600 kg of CO<sub>2</sub>/ton steel

Source: TSN IJmuiden, Agora, DIW, II3050

Roland Ber

Source: DIW

## For low-emission iron & steel production, a new direct reduced iron (DRI) system is required, either for e-methane or for hydrogen at the same costs

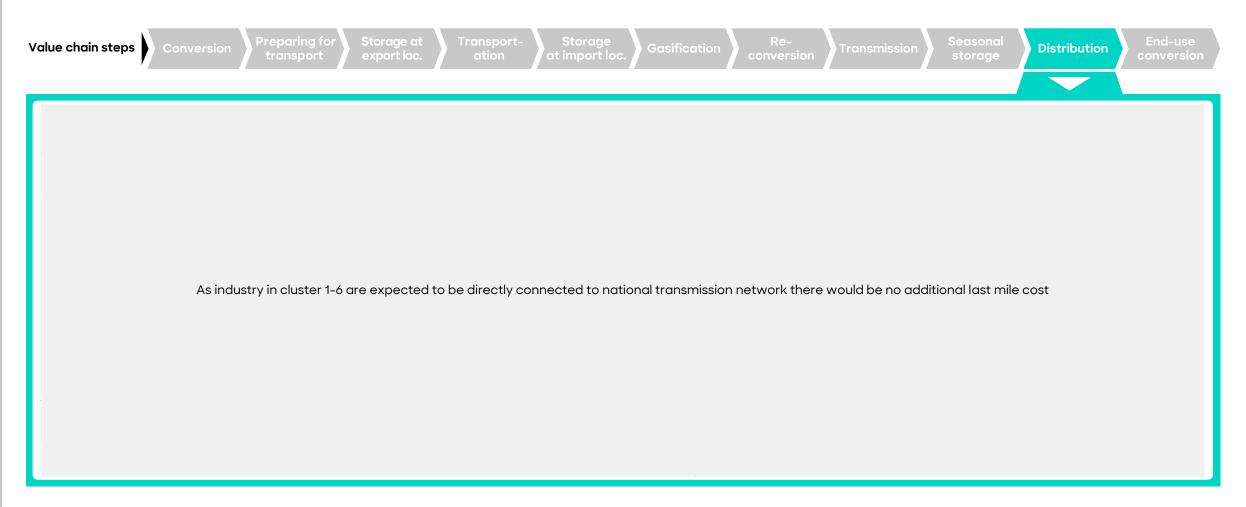
Options considered for end-use conversion of e-methane and hydrogen - Iron & steel

	fe	hnological easibility	Considerations	CAPEX [EUR/ton]	OPEX [EUR/ton/yr]
New asset	E-methane	<b>✓</b>	Same costs assumed for a new DRI system on	750 <sup>1)</sup>	Not considered <sup>1)</sup>
	Hydrogen 🗸		e-methane as for a new DRI system on hydrogen	750 <sup>1)</sup>	Not considered <sup>1)</sup>
Depreciated CH <sub>4</sub> asset	E-methane 🗶			n.a.	n.a.
within lifetime (with adaptations if required)	of  Hydrogen  E-methane	×	Currently used technology not compatible with	n.a.	n.a.
Lifetime extension of		×	e-methane or hydrogen	n.a.	n.a.
CH <sub>4</sub> asset (with adaptations if required)	Hydrogen	X		n.a.	n.a.

<sup>✓</sup> Technologically feasible X Not technologically feasible Selected option for comparison - Based on age of current assets & technological feasibility

<sup>1)</sup> The financial analysis is focused on cost of energy required per ton of steel and as the costs for an e-methane and hydrogen DRI system are the same, plant specific financials are not considered. Only for the total investment cost analysis for the Netherlands, CAPEX for a DRI system is considered

Assumptions: Distribution - Process heat



Assumptions: End-use conversion - Process heat

**End-use** Storage at Value chain steps conversion

			e-	Methane/Biomethane			Hydrogen	
Category	Parameter	Units	Value	Source		Value	Source	
Stoichiometry	Heat efficiency	%	90%	TNO <sup>LXI)</sup> , IRENA <sup>XLVII)</sup>		90%	Assumed	
	CAPEX	EUR/kW	0	Assumed	•	14	CE Delft <sup>LXII)</sup>	
	OPEX	EUR/kW/year	2.8	Assumed, IRENAXLVII)	•	4.0	TNO <sup>LXIII)</sup>	
Dignet on a sifica	Retrofitted	%	100%	Assumed		100%	Assumed	
Plant specifics	Lifetime	years	30	Assumed		30	Assumed	
	Utilization	%	90%1)	Assumed		90%1)	Assumed	
	Total demand	TWh/year	31	II3050 <sup>LVI)</sup>		31	II3050 <sup>LVI)</sup>	
	CO <sub>2</sub>	kg of CO₂e/MWh		not applicable <sup>2)</sup>				
	CH <sub>4</sub>	%	0.05%	Assumed			not applicable	
Scope 1 Emissions	N <sub>2</sub> O	kg of CO₂e/MWh	0.61	US NETL <sup>IX)</sup>				
	NO <sub>x</sub>	g NO <sub>x</sub> /MWh <sup>3)</sup>	50	TNO <sup>LXIV</sup> )		16.5	TNO <sup>LXIV</sup> )	
	H <sub>2</sub>	%		not applicable		0.25%	IEA <sup>LXV)</sup>	

<sup>1)</sup> Figure assumes full load hours of 8,760 per year; 2) Emissions for natural gas assumed to be 0.22 ton CO<sub>2</sub>/MWh from stochiometric calculation of combustion; 3) At 3% O<sub>2</sub>

## Most industrial plants in the Netherlands have methane boilers in place which can likely be retrofitted to hydrogen boilers if needed at relatively low costs

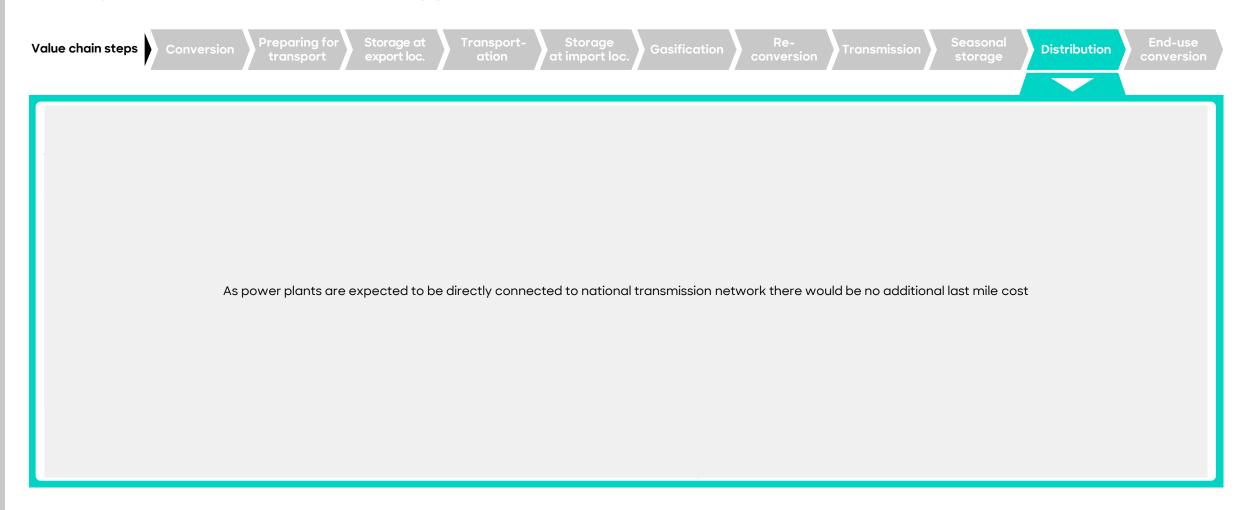
Options considered for end-use conversion of e-methane and hydrogen - Process heat

	Technologi feasibility		CAPEX [EUR/kW]	OPEX [EUR/kW/yr]
New good	E-methane 🗸	Some especially older industrial methane boilers can be replaced by new industrial methane boilers or for new industrial plants a new methane boiler can be bought	70	2.5
New asset	Hydrogen 🗸	Some especially older industrial methane boilers can be replaced by new industrial hydrogen boilers or for new industrial plants a new hydrogen boiler can be bought	100	3.6
Depreciated CH <sub>4</sub> asset	E-methane 🗸	Most current industrial methane boilers can likely be used without extra costs	0	2.8 <sup>1)</sup>
within lifetime (with adaptations if required)	Hydrogen 🗸	Most current industrial methane boilers can likely be retrofitted to hydrogen with relatively low extra costs	14	4.01)
Lifetime extension of CH <sub>4</sub> asset (with adaptations if required)		Not considered as an option due to relatively low C	CAPEX costs	

<sup>1)</sup> Assuming 10% higher OPEX for older assets

Source: TNO, IRENA, CE Delft Roland Berger | 28

Assumptions: Distribution - Electricity production



Assumptions: End-use conversion - Electricity production

**End-use** Storage at Value chain steps conversion

			e-Methane/Biomethane				Hydrogen	
Category	Parameter	Units	Value	Source		Value	Source	
Stoichiometry	Electricity efficiency	%	60%	TNO <sup>LXVI)</sup>	•	60%	TNO <sup>LXVI)</sup>	•
Stoichiometry	Heat efficiency	%	30%	EPA <sup>LXVII</sup> )		30%	Assumed	•
	CAPEX	EUR/kW	350 <sup>1)</sup>	TNO <sup>LXVI)</sup>	•	409 <sup>1)</sup>	TNO <sup>LXVI)</sup>	•
	OPEX	EUR/kW/year	11	Assumed, TNO <sup>LXVI</sup> )	•	12	Assumed, TNO <sup>LXVI)</sup>	
Plant specifics	Lifetime	years	30	Assumed		30	Assumed	
	Utilization	Full load hours	1,194	II3050 <sup>LXVIII</sup> )		1,194	II3050 <sup>LXVIII)</sup>	
	Total demand	TWh	14	II3050 <sup>LVI)</sup>		14	II3050 <sup>LVI)</sup>	
	CO <sub>2</sub>	kg of CO₂e/MWh		not applicable <sup>3)</sup>				
	CH <sub>4</sub>	%	0.05%	Assumed	•		not applicable	
Scope 1 Emissions	N <sub>2</sub> O	kg of CO₂e/MWh	0.91	US NETL <sup>IX)</sup>	•			
	NO <sub>x</sub>	g NO <sub>x</sub> /MWh <sup>2)</sup>	35	TNO <sup>LXIV)</sup>		17	TNO <sup>LXIV</sup> )	
	H <sub>2</sub>	%		not applicable		0.2%	IEA <sup>LXV)</sup>	•

1) Including costs for increasing lifetime - 350 EUR/kW for both methane and hydrogen; 2) At 15% O<sub>2</sub>; 3) Emissions for natural gas assumed to be 0.42 ton CO<sub>2</sub>/MWh, source US NETL

Comfort level of the assumption: High Medium Low Source: TNO, EPA, II3050, SCI Roland Berger | 30

# Power plants in the Netherlands are in general relatively old, but lifetime can likely be extended (possibly in combination with hydrogen retrofitting)

Options considered for end-use conversion of e-methane and hydrogen - Electricity production

Likely option in Germ to limited current co	rany due Technolo feasib	•	CAPEX [EUR/kW]	OPEX [EUR/kW/yr]
Nowagoot	E-methane	Some especially older methane power plants can be replaced by new methane power plants or buying n methane power plants can increase total capacity	e iew 700	10
New asset	Hydrogen 🗸	Some especially older methane power plants can be replaced by new hydrogen power plants or buying new hydrogen power plants can increase total capacity	e new 770	11
Depreciated CH <sub>4</sub> asset within lifetime	E-methane	Some current methane power plants can likely be us without extra costs	sed 0	(11 <sup>1)</sup>
(with adaptations if required)	Hydrogen 🗸	Some current methane power plants can likely be retrofitted to hydrogen without lifetime extension	59	121)
Lifetime extension of	E-methane 🗸	Most current methane power plants in the Netherlar likely require lifetime extension	nds 350	111)
<b>CH</b> ₄ <b>asset</b> (with adaptations if required)	Hydrogen 🗸	Most current methane power plants in the Netherlar likely require lifetime extension and potential retrofit to hydrogen	nds ting 409	121)

<sup>✓</sup> Technologically feasible X Not technologically feasible Selected option for comparison - Based on age of current assets & technological feasibility

Source: TNO Roland Berger | 31

<sup>1)</sup> Assuming 10% higher OPEX for older assets

Source: EU LCA, HyWay 27, IRENA, II3050

## Overview of the assumptions for all selected renewable energy vectors in 2040

Assumptions: Distribution - Decentral heating

Storage at Value chain steps **Distribution** 

				e-	Methane/Biomethane			Hydrogen
Category		Parameter	Units	Value	Source		Value	Source
Stoichiome	. <b>+</b>	Electricity input	kWh/ton/km	0.08	EU LCA <sup>XII)</sup>		0.6	Agora <sup>XXIII)</sup>
Stoichionie	ru y	Losses	%/1,000 km	0.02%	EU LCAXII)		0.40%1)	EU LCAXII)
		Tariff	EUR/MWh	19 <sup>2)</sup>	Assumed		55	Calculated
	}	CAPEX	EUR m/km				0.3	IRENAXXXIV)
	New	OPEX	% of CAPEX				1%	Assumed
	6 d	CAPEX	EUR m/km				0.1	IRENAXXXIV)
	Retro- fitted	OPEX	% of CAPEX		not applicable		1%3)	Assumed
Pipeline specifics		Retrofitted	%		not applicable		50%	Assumed
оросшос		Lifetime	years				55	Assumed
		WACC	%				4%	Dutch Climate Ministry <sup>LXIX)</sup>
		Pipeline length	km				82,718	Calculated
		Total demand	TWh/year	47 <sup>4)</sup>	II3050 <sup>LVI)</sup>		23	II3050 <sup>LVI)</sup>
		Av. distance per end user	km	60	Assumed	•	60	Assumed
Scope 1 Emis	cions	CO <sub>2</sub>	kg of CO <sub>2</sub> e/MWh	Corross	Corresponding to losses in pipeline		Corrosp	anding to losses in ningling
Scope remis	310113	H <sub>2</sub>	kg of CO <sub>2</sub> e/MWh	Corresp	oriding to losses in pipe	III IE	Corresp	onding to losses in pipeline

<sup>1)</sup> Considering total loss of 1% and then dividing by 2.5 to get the loss in %/1,000 km; 2) Dividing the sum of the 2040 depreciation costs, cost of capital and OPEX by the demand; 3) OPEX as percentage of new values of pipelines, 4) Demand including fossil methane

Assumptions: End-use conversion - Decentral heating

**End-use** Storage at Value chain steps conversion

				e-	-Methane/Biomethane			Hydrogen	
Category		Parameter	Units	Value	Source		Value	Source	
Stoichion	netry	Heat efficiency	%	92% <sup>1)</sup>	TNO <sup>LXX)</sup>	•	92% <sup>1)</sup>	TNO <sup>LXX)</sup>	
		CAPEX	EUR per boiler	0	Assumed	•	5,000	Nefit Bosch <sup>LXXI)</sup>	
	S	OPEX	EUR/year	100	Feenstra <sup>LXXII)</sup>		100	Assumed	
		Number of boilers	# m	0.252)	II3050 <sup>LXVIII)</sup>		0.242)	II3050 <sup>LXVIII)</sup>	
Boiler	סדט	CAPEX	EUR per boiler	0	Assumed		11,000 <sup>3)</sup>	Assumed, Milieu Centraal <sup>LXXII</sup>	II) <b>(</b>
specifics	Hybrid heat pump	OPEX	EUR/year	200	Feenstra <sup>LXXIV)</sup>		200	Assumed	
	± – σ	Number of boilers	# m	1.7 <sup>2)</sup>	II3050 <sup>LXVIII)</sup>		1.4 <sup>2)</sup>	II3050 <sup>LXVIII)</sup>	
		Lifetime	years	15	Feenstra <sup>LXXV)</sup>		15	Assumed	
		Total demand	TWh/year	23	II3050 <sup>LVI)</sup>		23	II3050 <sup>LVI)</sup>	
		CO <sub>2</sub>	kg of CO <sub>2</sub> e/MWh		not applicable4)				
		CH <sub>4</sub>	%	0.05%	Assumed			not applicable	
Scope 1 Em	issions	N <sub>2</sub> O	kg of CO <sub>2</sub> e/MWh	0.60	US NETL <sup>IX)</sup>				
		NO <sub>x</sub>	g NO <sub>x</sub> /MWh <sup>5)</sup>	50	TNO <sup>LXIV)</sup>		10.5 TNO <sup>LXIV</sup> )  0.25% Oxford Energy Institute <sup>LXXVI</sup> )		
		H <sub>2</sub>	%		not applicable				

<sup>1)</sup> Based on HHV; 2) 2050 values for residential boilers scaled based on 2040 demand - Utilities relatively small compared to residential, so not considered here; 3) Hybrid heat pumps include both a CV and pump, price is the sum of both elements; 4) Emissions for natural gas assumed to be 0.22 ton CO<sub>2</sub>/MWh from stochiometric calculation of combustion; 5) at 3% O<sub>2</sub>

## In the Netherlands, boilers for decentral heating currently almost all run on methane - Retrofitting those to hydrogen is likely not technologically feasible

Options considered for end-use conversion of e-methane and hydrogen - Decentral heating

	Technol	logical		CA	PEX	OP	EX
	feasik	bility	Considerations	[EUR/CV]	[EUR/HHP]	[EUR/CV /year]	[EUR/HHP /year]
New asset	E-methane		Some especially older decentral methane boilers can be replaced by new decentral methane boilers - Likely limited use case for new methane boilers for newbuild	2,000	8,000	100	200
New usset	Hydrogen 🗸		Some especially older decentral methane boilers can be replaced by new decentral hydrogen boilers - Likely limited use case for new hydrogen boilers for newbuild	5,000	(11,000)	100	200
Depreciated CH <sub>4</sub> asset within lifetime	E-methane 🗸	/	Most current decentral methane boilers can likely be used without extra costs	0	0	1001)	(200 <sup>1)</sup>
(with adaptations if required)	Hydrogen	ζ		n.a.	n.a.	n.a.	n.a.
Lifetime extension of CH <sub>4</sub> asset	E-methane	Lifetime extension of decentral methane boilers and retrofitting existing decentral methane boilers to hydrogen likely not technologically feasible		n.a.	n.a.	n.a.	n.a.
(with adaptations if required)	Hydrogen X			n.a.	n.a.	n.a.	n.a.

<sup>✓</sup> Technologically feasible X Not technologically feasible Selected option for comparison - Based on age of current assets & technological feasibility CV ("Centrale Verwarmina") HHP (Hybrid Heat Pump)

<sup>1)</sup> Assuming the same OPEX also for older assets due to fixed maintenance contracts

XIX.

XX.

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LXXI. "Koop een ketel die op waterstof kan", Nefit Bosch, 2021

LXXII. Service & onderhoud cv-ketel, Feenstra

LXXIII. Nieuwe cv-ketel of combiketel kopen, Milieu Centraal

LXXIV. Onderhoud hybride warmtepomp, Feenstra

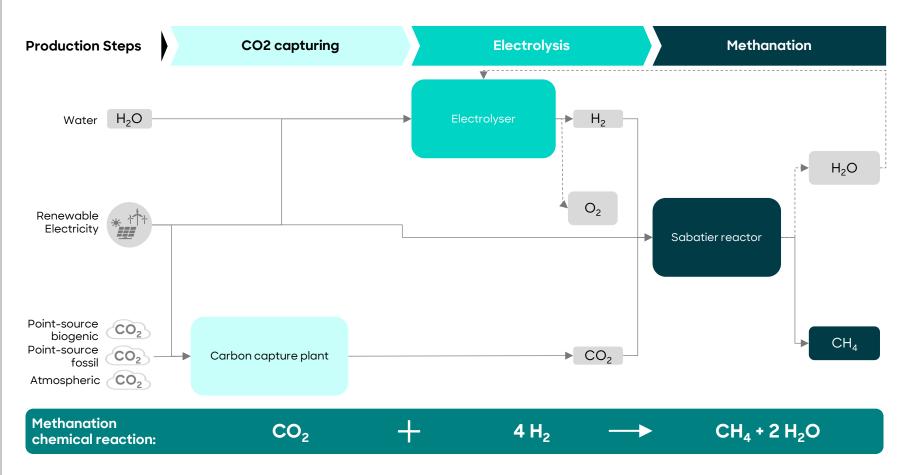
LXXV. Cv-ketel vervangen, Feenstra

LXXVI. Review of Hydrogen Leakage along the Supply Chain, Oxford Institute for Energy Studies, 2024

## B. E-methane production technology deepdives

## Sabatier methanation is the only commercialized synthesis method, employing a two-stage process, although it has a relatively low efficiency of 55-60%

Technology deepdive: Sabatier methanation



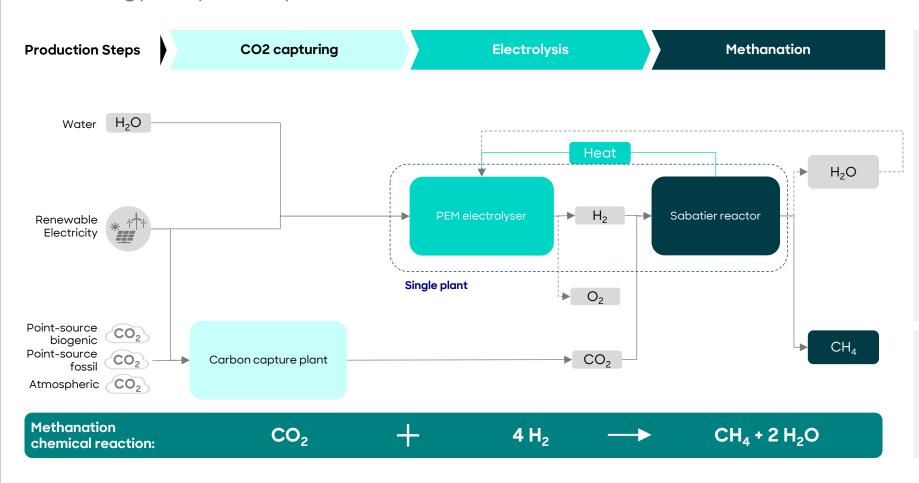
- · Sabatier methanation is a two-stage process that produces methane (CH<sub>4</sub>) by reacting hydrogen (H2) with carbon dioxide (CO<sub>2</sub>) over a nickél catalyst at 200-500°C and 1-10 bar.
- In the first stage, hydrogen is generated via water electrolysis, followed by reaction with CO2 in the methanation staae
- The Audi e-gas plant in Germany, with a 6 MW electric capacity, is the world's largest green methanation plant
- · In China, Sabatier methanation on gas field coal is operated at GW scale

Key parameter: Category	Value
Technology maturity	High
Methanation temperature [°C]	200-500
Overall process efficiency <sup>1)</sup> [%]	65%

<sup>1)</sup> Process efficiency describes the combined efficiency of the electrolysis and methanation step. The efficiency of electrolysis is expected to be 76% by 2040.

## Hybrid Sabatier methanation combines electrolysis and methane synthesis within a single plant, utilizing the heat generated during methanation

Technology deepdive: Hybrid conventional Sabatier methanation



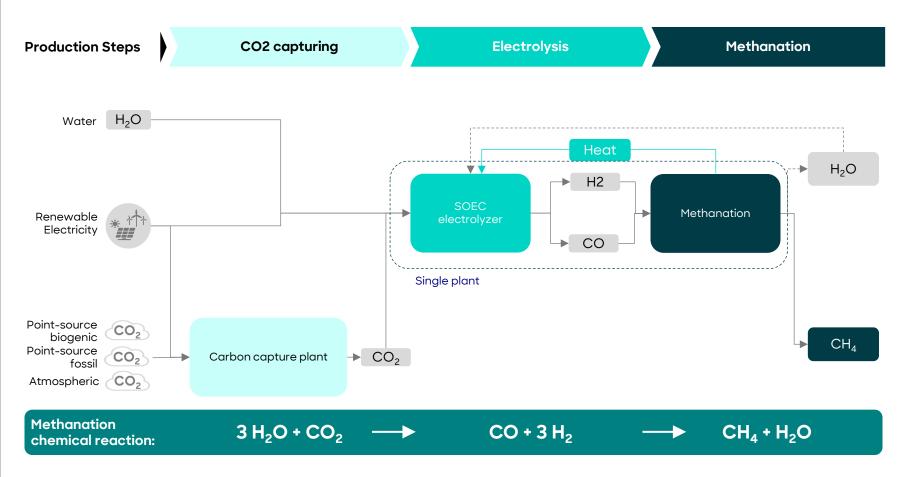
- Hybrid Sabatier methanation combines electrolysis and methane formation within a single plant, utilizing the heat generated during methanation to drive the endothermic water electrolysis step
- This technology eliminates the need for separate hydrogen procurement and achieves higher efficiency than traditional Sabatier methanation through effective waste heat utilization
- A pilot project has been launched by Tokyo Gas and JAXA, with commercialization expected after 2040

Key parameter: Category	Value
Technology maturity	Medium
Methanation temperature [°C]	220
Overall process efficiency <sup>1)</sup> [%]	80%

<sup>1)</sup> Process efficiency describes the combined efficiency of the electrolysis and methanation step

## SOEC methanation integrates high temperature co-electrolysis of H<sub>2</sub>O and CO<sub>2</sub> and methane synthesis within a single plant, achieving high efficiencies

Technology deepdive: Hybrid SOEC methanation



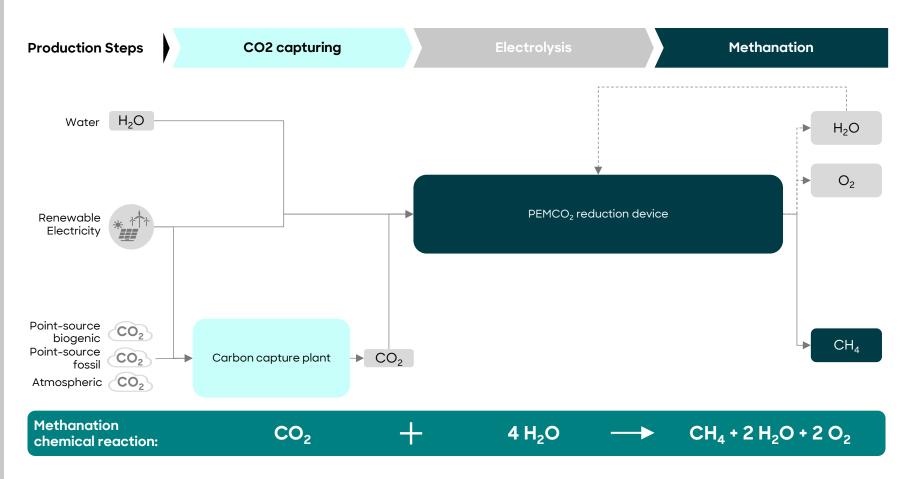
- SOEC methanation combines the coelectrolysis of H2O and CO2 with methane synthesis in a single plant
- This technology eliminates the need for separate hydrogen procurement and achieves higher efficiency than traditional Sabatier methanation through effective waste heat utilization
- Osaka Gas is currently conducting **pilot** testing, demonstrating efficiencies of 85% to 90%
- Commercialization is anticipated in the 2040s

Key parameter: Category	Value
Technology maturity	Low
Methanation temperature [°C]	800
Overall process efficiency <sup>1)</sup> [%]	75-90%

<sup>1)</sup> Process efficiency describes the combined efficiency of the electrolysis and methanation step

## PEMCO<sub>2</sub> methanation uses a Polymer Electrolyte Membrane (PEM) to synthesize e-methane directly from water and CO<sub>2</sub> in one step

Technology deepdive: PEMCO<sub>2</sub> methanation



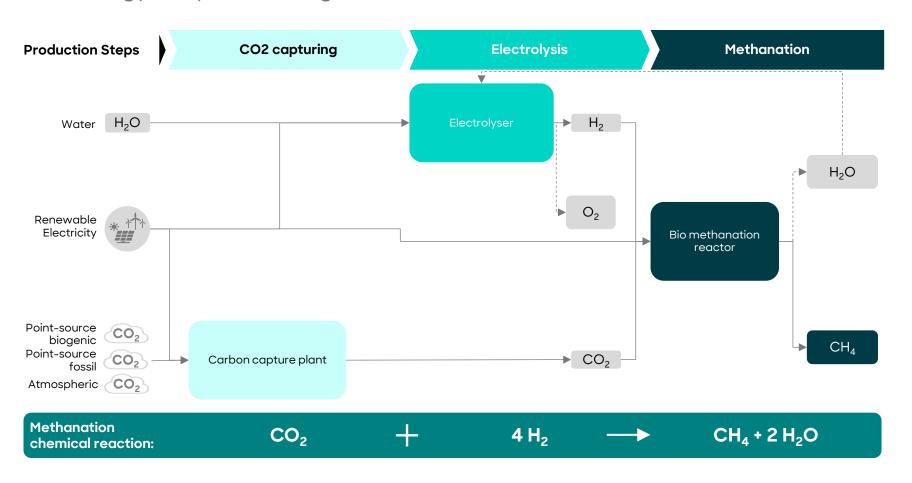
- PEMCO<sub>2</sub> methanation utilizes a Polymer Electrolyte Membrane (PEM) to directly synthesize e-methane from water and CO<sub>2</sub>
- The technology lowers equipment costs and operates at moderate temperatures (60-80°C). It also eliminates the need for precious metal cathodes and hydrogen procurement
- A pilot project has been launched by Tokyo Gas, with commercialization expected after 2040

Key parameter: Category	Value
Technology maturity	Low
Methanation temperature [°C]	60-80
Overall process efficiency <sup>1)</sup> [%]	70-80%

<sup>1)</sup> Process efficiency describes the combined efficiency of the electrolysis and methanation step

## Biological methanation utilizes a two-step biochemical process where archaea act as biological catalysts to produce methane

Technology deepdive: Biological methanation



- · Biological methanation employs a twostep biochemical process in which hydrogen is generated via electrolysis before archaea serve as biological catalysts to produce methane
- · This method operates under mild temperature and pressure conditions
- · However, projected investment costs are **higher** than those for Sabatier
- The world's first demonstration plant combining electrolysis and biological methanation was established in Germany in 2015

Key parameter: Category	Value
Technology maturity	Medium
Methanation temperature [°C]	35-65
Overall process efficiency <sup>1)</sup> [%]	60-65%

<sup>1)</sup> Process efficiency describes the combined efficiency of the electrolysis and methanation step. The efficiency of electrolysis is expected to be 76% by 2040.

## C. Forecasted renewable energy vector demand in NL

## Energy demand estimates are based on II3050 report, developed by NL network companies to outline pathways to a climate-neutral energy system by 2050

Introduction to the II3050 report



## Objective of the report

#### II3050 aims to identify the key choices required to achieve a climate-neutral energy system by 2050

- It provides insight into the energy infrastructure and flexibility measures required in the long term
- It addresses uncertainties in predicting future developments by using scenarios that represent realistic extremes of possible energy system outcomes



## Approach of the report

#### II3050 uses scenarios to guide decisive policymaking

- The energy transition is a major societal challenge, demanding rapid fossil fuel reduction, renewable energy growth, and systemic changes across key sectors
- Energy infrastructure (gas, electricity, and heat networks) must undergo significant transformation to meet future demands
- Scenarios help capture uncertainties and support informed decision-making for policymakers and stakeholders



#### Contributors

#### II3050 was developed by several Dutch network companies and other relevant stakeholders

- · Network companies include: Alliander, Coteg, Enexis, Gasunie, Rendo, Stedin, TenneT, and Westlandinfra
- External experts, relevant industry associations, and government agencies provided input and consultation during the study

Source: II3050 Roland Berger | 46

# In this study the international trading scenario (INT) is the reference scenario

Scenarios used in II3050 report

Scenarios aligned with RepowerEU plan

#### IP2024 (December 2022) **II3050** (October 2023) National Leadership (NAT) **European Integration (EUR)** Collective 2040 technology High level of government involvement and national • High level of government involvement and European choices **Decentral** level of organization - Electrification, energy efficiency level of organization - Members of EU coordinate and 2030 **Initiatives** and renewable integration sharing energy and alian policies on resources management by High renewable energy generation from large scale · High adoption of CCS, limited renewable energy government national projects (e.g., offshore wind), flexible nuclear generation mainly from solar, wind and base load ND energy generation and nuclear hydrogen production **National** European · Limited decline of industry - Incentivized to Limited decline of industry - Existing electrify and use European biomass and **National National** Lead Integration NAT industry incentivized to electrify and hydrogen drivers Leadership new green industry is stimulated (e.g., synthetic fuel production) 2019 KA Nationally oriented, as much self-Internationally oriented, room for sufficient as possible import Climate European **EUR** Low level of government involvement Low level of government involvement and ambition Integration and regional level of organization international level of organization -Decentral climate neutral projects Development of economy driven by optimizing usage of global (hydrogen) supported by the government as a IA International Decentralized trading and leveraging international supply main tool for reaching climate targets **Initiatives Trading** High renewable energy generation from solar and onshore wind energy, limited High import of hydrogen and other renewable energy adoption of CCS vectors in combination with limited green hydrogen Tradina Market-Energy-intensive industry partially leaves the production from offshore wind driven Netherlands due to lack of governmental steering on individual Energy-intensive industry partially leaves the energy transition solutions. Netherlands due to strong global supply chain aovernment

The international tradina (INT) scenario which is the reference for this study as it is expected that coordinated alobal efforts will be required due to the shared nature of the climate crisis

**Decentralized Initiatives (DEC)** 

International Trading (INT)

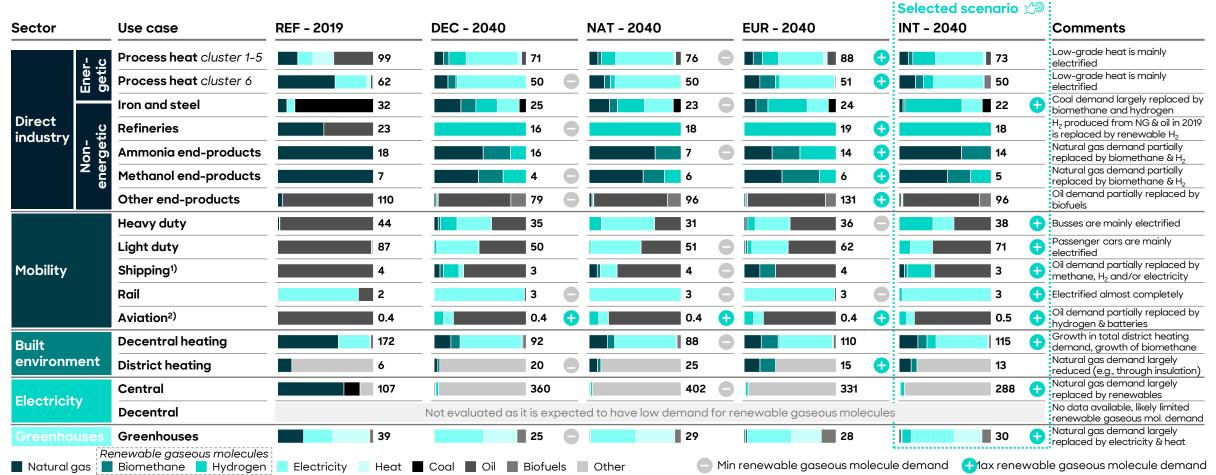
Source: II3050 Roland Beraer | 47

sets

frameworks

# The energy mix per use case is expected to change in the future – Each scenario from the II3050 report assumes a slightly different energy mix in 2040

Energy demand per use case - 2019 and 2040 [TWh]



<sup>1)</sup> Excl. ~140 TWh forecasted demand for international bunkering of synthetic and biofuels in NL, based on IRENA report on decarbonizing the shipping sector, which estimates 8.5 EJ total global shipping demand in 2040 and 6% of global bunkering to be in the Netherlands; 2) Excl. ~45 TWh forecasted demand for synthetic aviation fuel (SAF) for international aviation in NL in 2050, based on INT scenario in II3050 report

Source: II3050, Desk research Roland Beraer 1 48

# Different renewable energy vectors can be considered per use case to meet the demand for renewable gaseous molecules

Back-up - Rationale behind feasibility of renewable energy vectors per use case

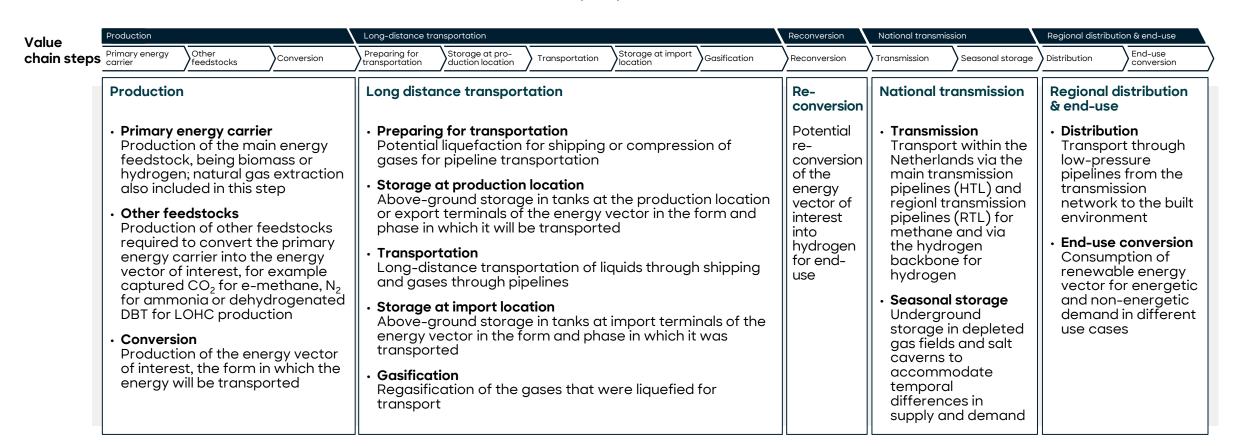
Sector	Use case	E- Methane	Hydrogen	Ammonia	Methanol
Non-energetic getic	Process heat cluster 1-5 Process heat cluster 6	E-methane is used for mid to high grade heat processes	Hydrogen is used for mid to high grade heat processes	High NOx emissions make ammonia less feasible for NL, also challenges due to slow combustion	Lower energy density makes methanol less economically viable
	Iron and steel	E-methane can be used as input for DRI systems to reduce iron ore	Hydrogen can be used as input for DRI systems to reduce iron ore	Low maturity of ammonia for steel production, challenges due to NOx	Low maturity of methanol for steel production
	Refineries	Reconverting e-methane back into hydrogen (for potential further processing) is likely economically unviable	Hydrogen is used for hydrocracking and desulfurization	No direct use for ammonia as feedstock	No direct use for methanol as feedstock
	Ammonia end-products		Hydrogen is used for conversion into ammonia	Ammonia can be directly imported rather converted on site from hydrogen	No direct use for methanol in ammonia end-products
	Methanol end-products		Hydrogen is used for conversion into methanol	No direct use for ammonia in methanol end-products	Methanol can be directly imported rathe converted on site from hydrogen
	Other end-products	E-methane for producing other chemicals (oxo-chemicals, acetylene,)	Hydrogen for producing other chemicals (bromine, hydrogen peroxide,)	Limited / no use for ammonia in other chemicals	Limited / no use for methanol in other chemicals
Mobility	Heavy duty Light duty	E-methane can be used in the form of CNG <sup>1)</sup> as fuel, niche use case for light duty as it is mostly electrified	Likely economically unviable compared to other sustainable options	High toxicity, poor flame stability and high NOx emissions make ammonia likely challenging	<ul> <li>Methanol can directly be used as fuel, niche use case for light duty as it is mostly electrified</li> </ul>
	Shipping	E-methane in the form of e-LNG can be used as direct fuel alternative	Not a likely option for domestic shipping in the Netherlands	Not a likely option for domestic shipping in the Netherlands	Methanol can be used as fuel alternative in specialized engines
	Rail	Not a likely options for trains in the Netherlands, almost all electrified	Not a likely option for trains in the Netherlands, almost all electrified	High toxicity, poor flame stability and high NOx emissions likely challenging	No methanol powered trains operate, unlikely alternative
	Aviation	Use case e-methane in the form of CNG <sup>1)</sup> as fuel alternative too limited	Hydrogen as a fuel alternative likely only suitable for niche applications	Use case ammonia as fuel alternative too limited	Use case methanol as fuel alternative to limited
Built environment	Decentral heating  District heating	E-methane can (directly) be used as input for methane / hybrid heat boilers	Hydrogen can be used as input for hydrogen / hybrid heat boilers	High toxicity and poor flame stability require specially designed / modified boilers, therefore likely challenging, also NOx challenges	Toxicity and potential formaldehyde emissions require specially designed / modified boilers, therefore likely challenging
Electricity	Central	E-methane can be used as input for methane power plants	Hydrogen can be used as input for hydrogen power plants	Potential in co-firing with coal & high NOx emissions, limited use case in the Netherlands	Low energy density makes methanol les economically feasible
	Decentral		Not evaluated as it is expected to have low	w demand for renewable gaseous molecules	
Greenhouses	Greenhouses	Methane can be used as input for boilers - Potential for CO <sub>2</sub> enrichment	Hydrogen can be used as input for boilers	Challenges as high toxicity and poor flame stability demand specialized boilers, and NOx emissions	Challenges as high toxicity and poor flame stability demand specialized boile

Source: II3050, Desk research Roland Berger | 49

D. Value chain quantification of renewable energy vectors

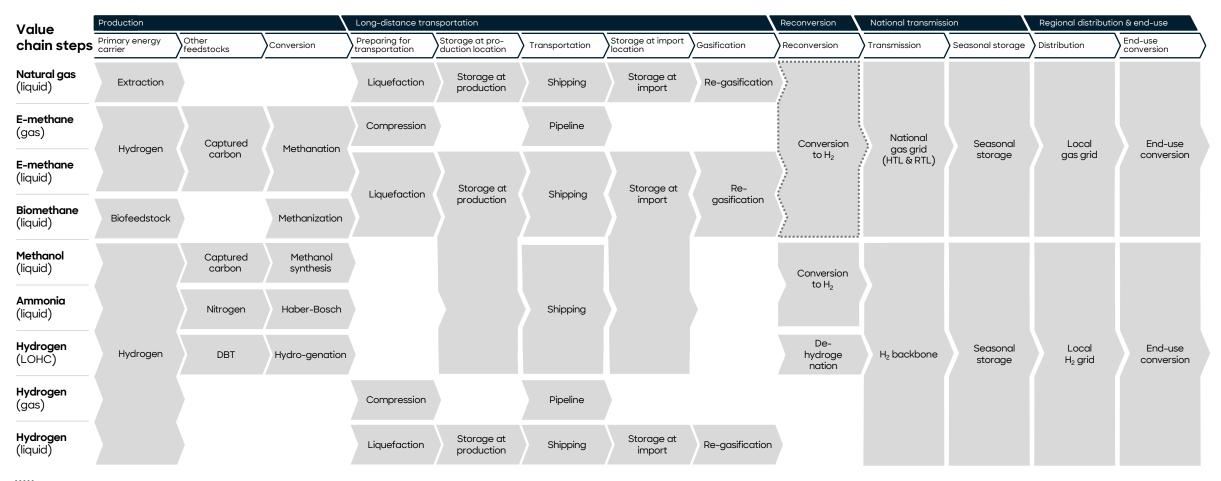
### Study focuses on the entire value chain from production to transportation to distribution and end-use

Renewable energy vector value chain descriptions (1/2)



## For the shortlisted end-use cases, different energy vectors have been mapped across the entire value chain

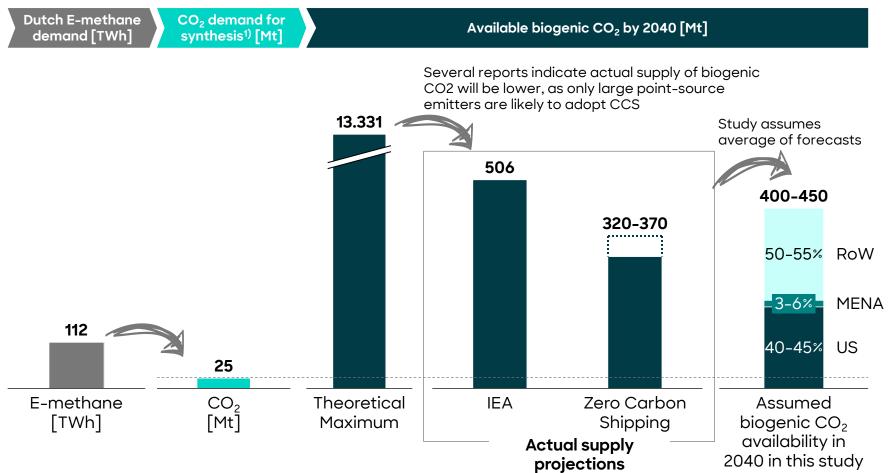
Renewable energy vector value chain descriptions (2/2)



# E. Biogenic CO<sub>2</sub> availability

# Supply of biogenic $CO_2$ will be limited as just the Dutch demand for e-methane would require ~13% of total available biogenic $CO_2$ of the US or ~150% of MENA

Availability of biogenic CO<sub>2</sub> in 2040 [Mt]



### Key takeaways

- Synthesizing the projected Dutch E-methane demand for 2040 requires approximately 25 Mt of CO<sub>2</sub>
- By 2040, 400–450 Mt of biogenic CO<sub>2</sub> is expected to captured and available for use
- Meeting Dutch E-methane needs would claim ~6% of global biogenic CO<sub>2</sub> –disproportionate for its energy demand under 1% of the global total. Moreover, other sectors might outcompete the demand for e-methane production
- Meeting the entire Dutch Emethane demand through imports from specific regions would require ~13% of the available biogenic CO<sub>2</sub> of the US or ~150% of MENA

1) Assuming a 90% capture rate efficiency

# F. Challenges

## Challenges

1/3

The transition to a low-carbon energy system presents an array of challenges. In this chapter, we focus on the most critical challenges related to emethane. Our aim here is to provide a more nuanced understanding of e-methane's potential and its limitations as an emerging technology to decarbonize future energy usage. First, we will focus on challenges that are solely related to e-methane, after which we will end with challenges that are also related to all new emerging energy carriers.

#### **Technical and Productional**

E-methane has a number of technical and productional challenges. Two are related to the Technical Readiness Levels (TRL) of this energy carrier. First of all, DAC technology is at the moment not fully mature (see also Chapter 5). Secondly, the production of e-methane is currently still at pilotlevel quantities, while upscaling to large production quantities will probably be complex.

Other challenges relate to the production efficiency of e-methane. Like most physical and chemical conversions from one product into another the combination of electrolyser, DAC and methanation is energy intensive. This challenge is described in Chapter 4 (Figure 11) of the report.

Furthermore, when producing e-methane losses can occur. These losses might lead to the preference of direct use of hydrogen instead of adding another conversion step for producing e-methane.

#### **Economics and Financial**

The question whether e-methane will succeed in terms of being adopted by end-users will for an important part be a matter of its economics. In the end, the economics decide on e-methane's competitiveness in relation to competing energy carriers.

This study shows on the one hand that e-methane may turn out to be twice as expensive to produce in 2040 compared to biomethane. At the same time natural gas (including CCS) will be even less expensive than biomethane. So, when comparing low carbon gases, e-methane is the least competitive. However, biomethane will not be abundantly available in the future and natural gas including CCS does not contribute to the aim of reaching the 2050 climate goals.

Chapter 6 indicates that for the selected use cases, the CAPEX intensity of meeting hydrogen demand in NL is, at least, three times higher than that of e-methane. One could therefore argue that economically e-methane must become the energy carrier of choice for certain cases. However, policy makers and end-users have to make decisions today for the energy landscape of tomorrow. As long as industrial companies have no feasibility of e-methane being abundantly available ten or twenty years from now, these companies may choose a different path. This path may be, with equivalent uncertainties about availability, hydrogen. Uncertainty regarding the ultimate costs of DAC is another uncertain factor companies have to deal with. If the costs of DAC would turn out twice as high, the electricity sector and cluster 6 would perhaps be better off using hydrogen instead of e-methane.

## Challenges

2/3

The transition to a low-carbon energy system presents an array of challenges. In this chapter, we focus on the most critical challenges related to emethane. Our aim here is to provide a more nuanced understanding of e-methane's potential and its limitations as an emerging technology to decarbonize future energy usage. First, we will focus on challenges that are solely related to e-methane, after which we will end with challenges that are also related to all new emerging energy carriers.

#### Societal acceptance and sustainability

Accepting the idea that e-methane could in the future be a sustainable energy carrier, by policy makers as well as the public in general, is crucial for e-methane to be adopted. For biomethane and e-methane, like with natural gas, methane leakage is the biggest challenge. We are only at the beginning of understanding the current scale of methane leakage but, specifically during natural gas production, scope 1 emissions appear to be substantial. Potential e-methane emissions in the supply chain; during production, transportation or as a result of an asset being dismantled would hurt the image of e-methane as a zero-footprint energy carrier. In this respect it is important to note that in this study the production of e-methane results in scope 2 emissions via the CO<sub>2</sub> grid intensity for the electricity that is used for DAC. A potential lack of confidence by policy makers and/or end-users that e-methane will be a zero-footprint energy carrier in the future might hinder its adoption. It will take substantial efforts in terms of adopting global standards and convincing interest groups to tackle this issue.

Another element that could affect public perception negatively is the supposed lock-in for natural gas. This means that the public sees synthetic renewable fuels as a reason for the continuation of the fossil fuel-based infrastructure. Policy makers and end-users aim for the transition to sustainable energy carriers. Interest groups will argue that in a situation where energy carriers are still being dependent on the fossil fuel-based infrastructure the transition to sustainable energy carriers is delayed or even thwarted. One can argue however that no lock-in risk exists because phasing out fossil fuels is the only direction to go in order to tackle climate change. Continued and reuse of current fossil infrastructure for renewable energy sources like e-methane is evidently an opportunity and not a risk.

The transition to a low-carbon energy system presents an array of challenges. In this chapter, we focus on the most critical challenges related to emethane. Our aim here is to provide a more nuanced understanding of e-methane's potential and its limitations as an emerging technology to decarbonize future energy usage. First, we will focus on challenges that are solely related to e-methane, after which we will end with challenges that are also related to all new emerging energy carriers.

#### Challenges related to all new emerging energy carriers

The study contains many assumptions on the speed of development of technologies and the future costs associated with the production and transportation of e-methane. This is especially true for the costs and the grid intensity related to DAC. This makes the outcome of the future costs of e-methane for end-users uncertain as well as e-methane's competitiveness (relative costs) against other energy carriers. Whatever the future costs of e-methane, in general it is clear that electrification of all end-users and industries is not a viable alternative.

A major hurdle for all new emerging energy carries such as hydrogen and e-methane is the establishment of robust carbon accounting and certification systems which is a requirement under the Renewable Energy Directive (REDII and the forthcoming REDIII revisions). Ensuring the carbon neutrality of e-methane requires reliable methods for measuring, reporting, and verifying (MRV) emissions throughout its life cycle. Although progress has been made, these systems remain underdeveloped. This also applies to countries outside Europe, for example in the case that emethane is sourced from MENA.

Another critical issue is the inconsistency of policy incentives. While government interventions through mechanisms like carbon pricing, taxes, and subsidies are vital to make e-methane competitive with fossil fuels, such incentives vary widely across the European Union and its member states. This disparity creates market imbalances, discourages private investment, and complicates the development of a unified European approach to emethane adoption.

The lack of global standardization is an uncertainty for all energy carriers. Without internationally agreed-upon standards for production, quality, and sustainability criteria, cross-border trade in e-methane may be hindered. This lack of alignment affects not only the feasibility of international market integration but also the harmonization of decarbonization goals and the realization of large-scale ambitions.

Permitting and environmental regulations present a significant challenge. Securing permits for the construction of e-methane production facilities, green hydrogen and DAC is often a lengthy and complex process, influenced by strict environmental regulations. These delays can increase project costs and slow the pace of scaling up production, undermining the role of e-methane in the energy transition.

